

# Rheology of Dense Suspensions

## From micro to MACRO

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Francisco Rocha

IUSTI, Aix Marseille University

60<sup>th</sup> Anniversary Groupe Français de Rhéologie

October 2024





Lecture day GFR 2024 at IUSTI Laboratory

Tuesday 22th

11:00

**Jean Comtet** (CNRS, ESPCI Paris)

**Microscopic characterization and formulation of solid interfaces**

2:00

*We are now here!*

**Francisco Melo da Rocha** (IUSTI, Marseille)

**Macroscopic rheological behavior of dense granular suspensions from microscopic considerations**

4:00

**François Peters** (InPhyNi, Nice)

**Numerical simulations of dense granular suspensions**

# Outline

## *Initial (but not mandatory) Plan:*

1. *General Introduction*

2. *Granular Suspensions: The Newtonian behaviour*

i) *Suspension as an effective fluid — Suspension Viscosity*

ii) *Characterising the Viscosity: Volume— vs Pressure—imposed Rheology*

iii) *Link to microstructure?*

3. *Non—Newtonian Behaviours: e.g. Shear—thickening in non-Brownian suspensions*

i) *Experimental observations*

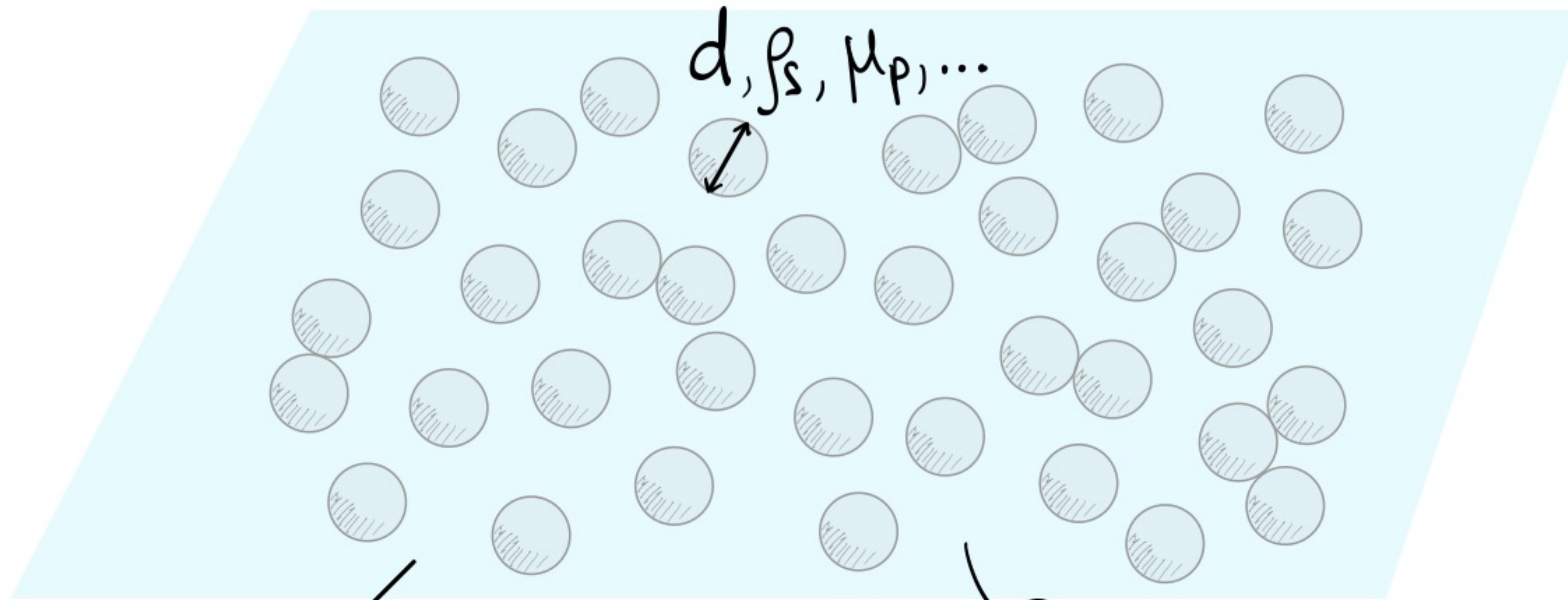
ii) *The frictional transition model*

ii) *Hydrodynamics of shear—thickening suspensions*

# What is a Suspension?

## Definition:

Generally speaking, it's a mixture of solid particles and a fluid (e.g. water, oil ...)



Volume fraction,  $\Phi = \frac{\text{Vol. Grains}}{\text{Total Vol.}}$

$\eta_f, \rho_f$

# Suspensions in Nature:

e.g. Phytoplankton blooms in Gulf of Finland



# Suspensions in Nature:

e.g. Geophysical Flows

Debris flows, pyroclastic flows, snow avalanches, among others...

“Civilization exists by  
geological consent,  
subject to change  
without notice.”

Will Durant

# Suspensions in Nature:

e.g. Geophysical Flows

Debris flows, pyroclastic flows, snow avalanches, lahars, among others...



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e.g. Geophysical Flows

Debris flows, pyroclastic flows, snow avalanches, lahars, among others...



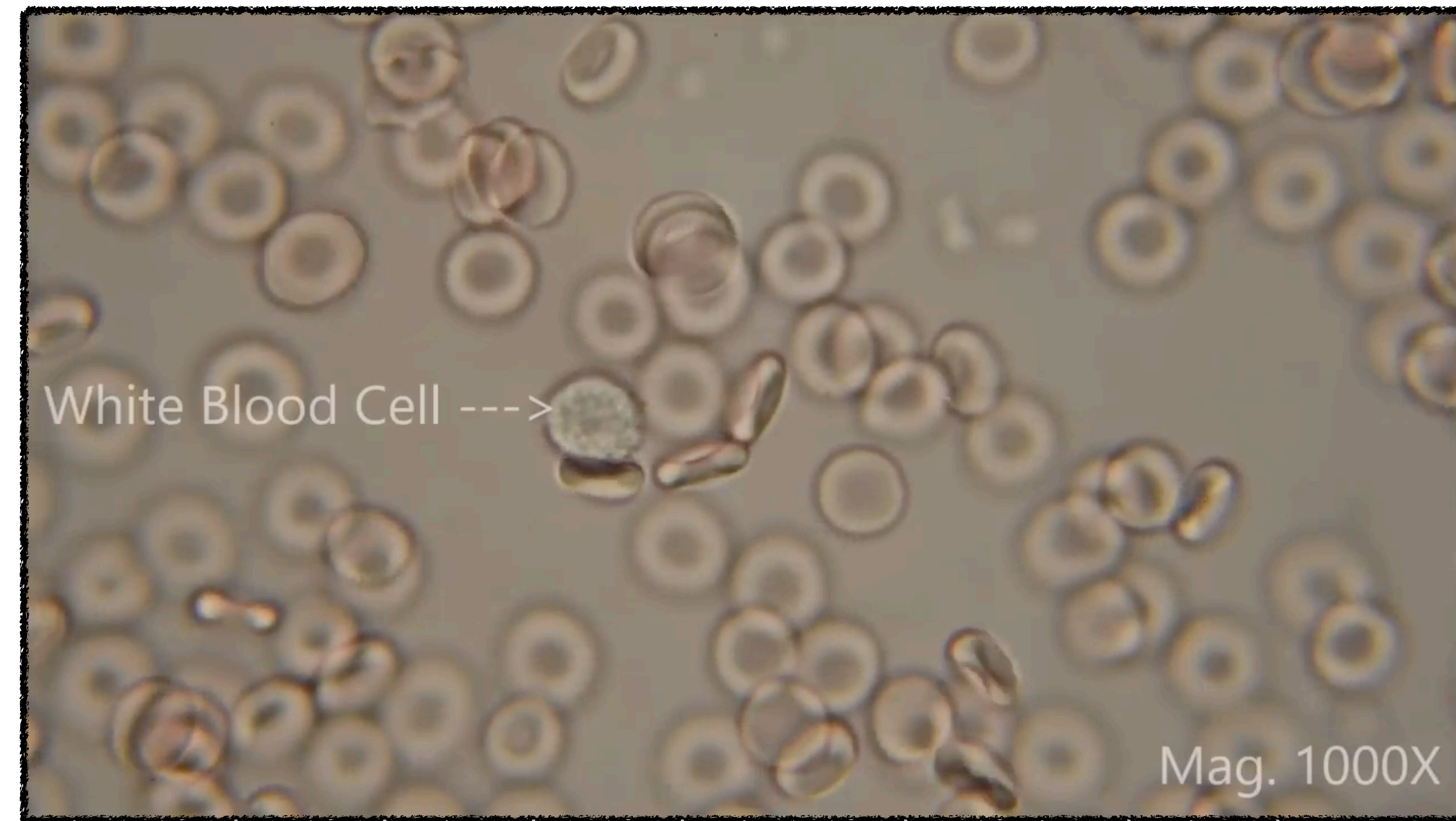
Between 2004 and 2016, almost **5000** debris flows were registered globally killing more than **50.000 people**

(Froude & Petley *Nat. Hazards Earth Syst. Sci.* 2018)

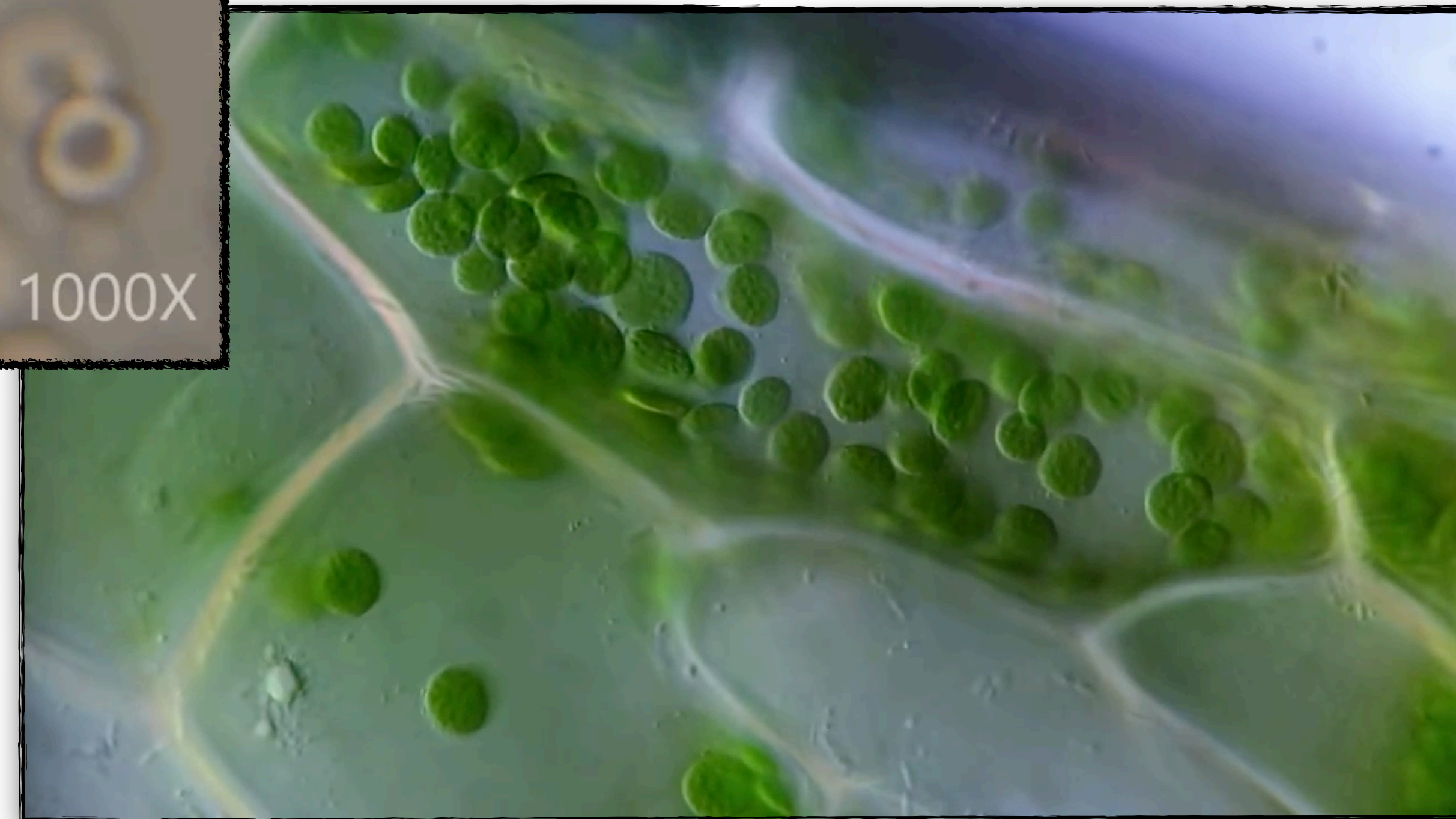


# Suspensions in Nature:

e.g. biological flows



Cytoplasmic streams



Red blood cells

*credits: Sci-Insp Youtube Channel*

# Suspensions in Industry



Civil engineering



Mucem  
(Marseille)

Food processing



Paints, bulk chemicals...

Only in the USA,  $10^{12}$  kg of granular materials are used per year.  
→ *2<sup>nd</sup> most—used product!*

*(Shinbrot & Muzzio PRL 1998)*

# Not Trivial to Understand Scientifically...

## Multidisciplinary Interest:

*statistical physics, fluid / solid mechanics, soil mechanics*

## Not trivial to apply “classical” techniques:

*In many situations thermal agitation does not play a role  
Extremely dissipative system*

*Real situations involves HUGE amount of particles*



*Classical statistical mechanics*



*Tracking individual grains*

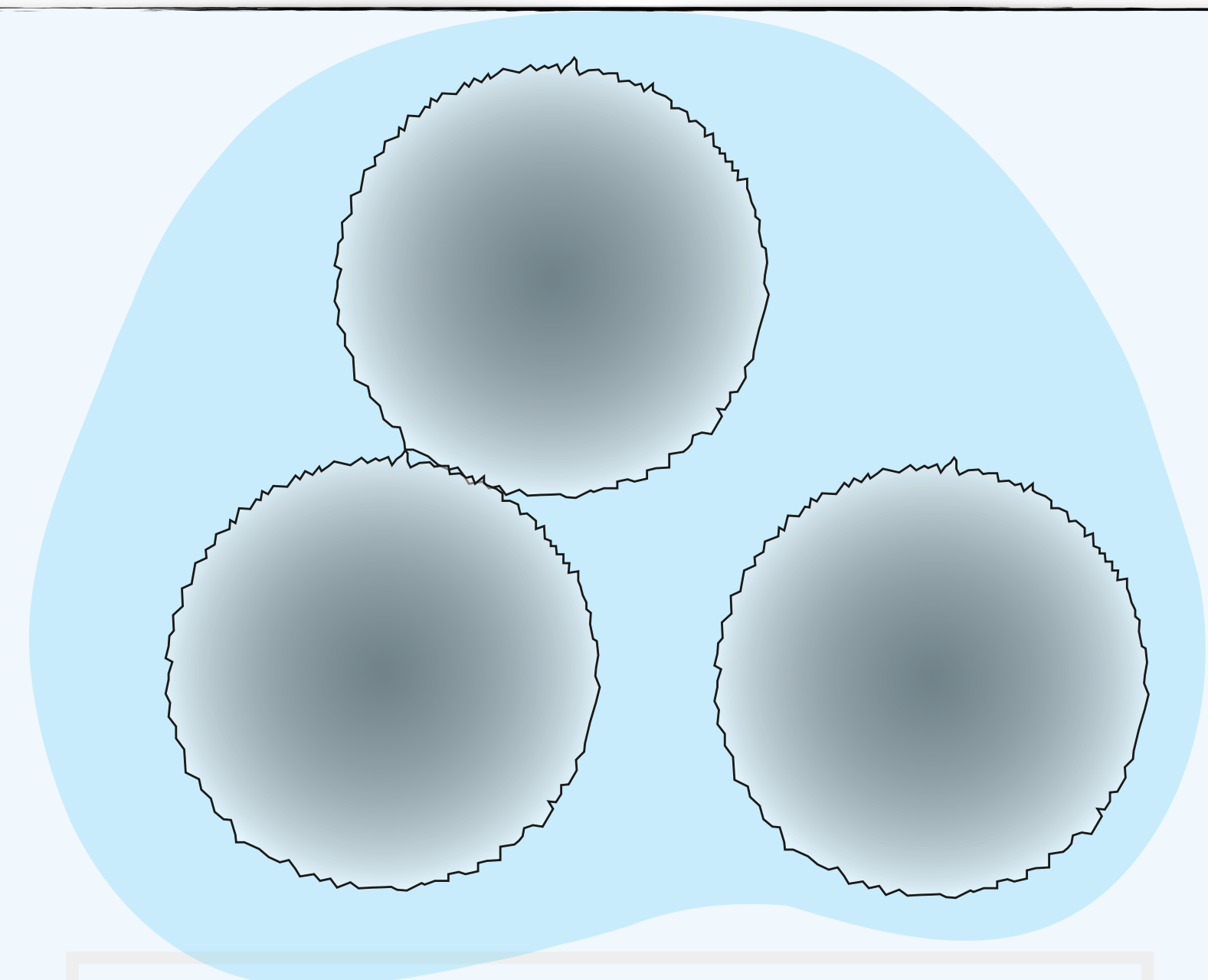
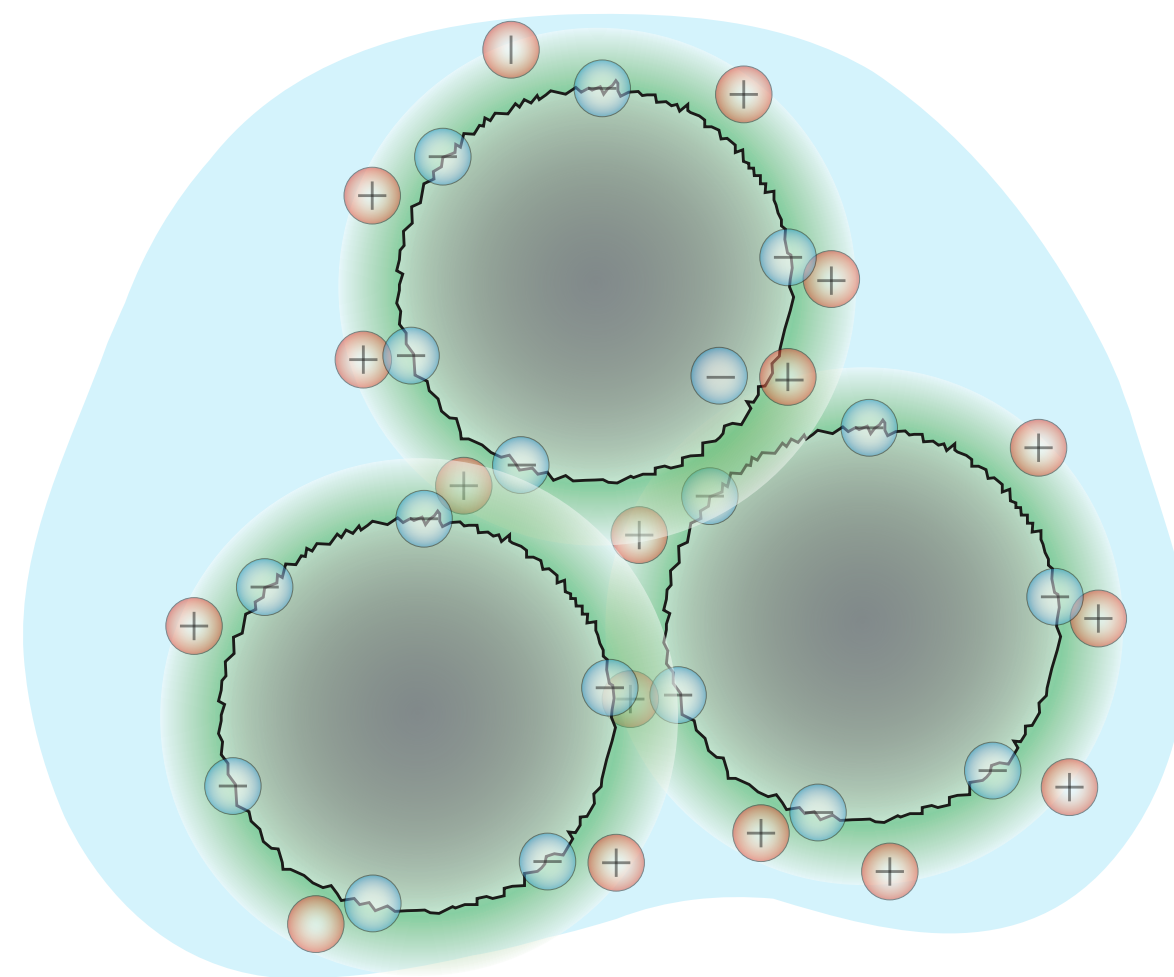
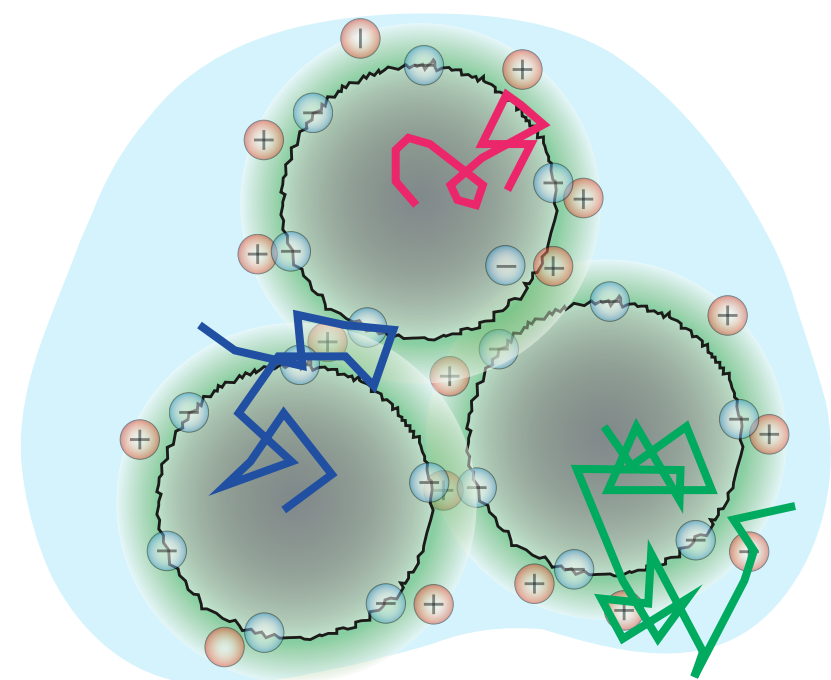


*Suspensions as  
an effective Complex Fluid*



*Suspension Rheology???*

# Different Physics Depending on Particle Size



Brownian/colloidal suspensions

Granular suspensions

$1 \mu m$

$100 \mu m$

Grain size  $d$

Thermal agitation

Repulsive forces (Electrostatics, polymer brushes...)

Adhesion forces (Van der Waals,...)

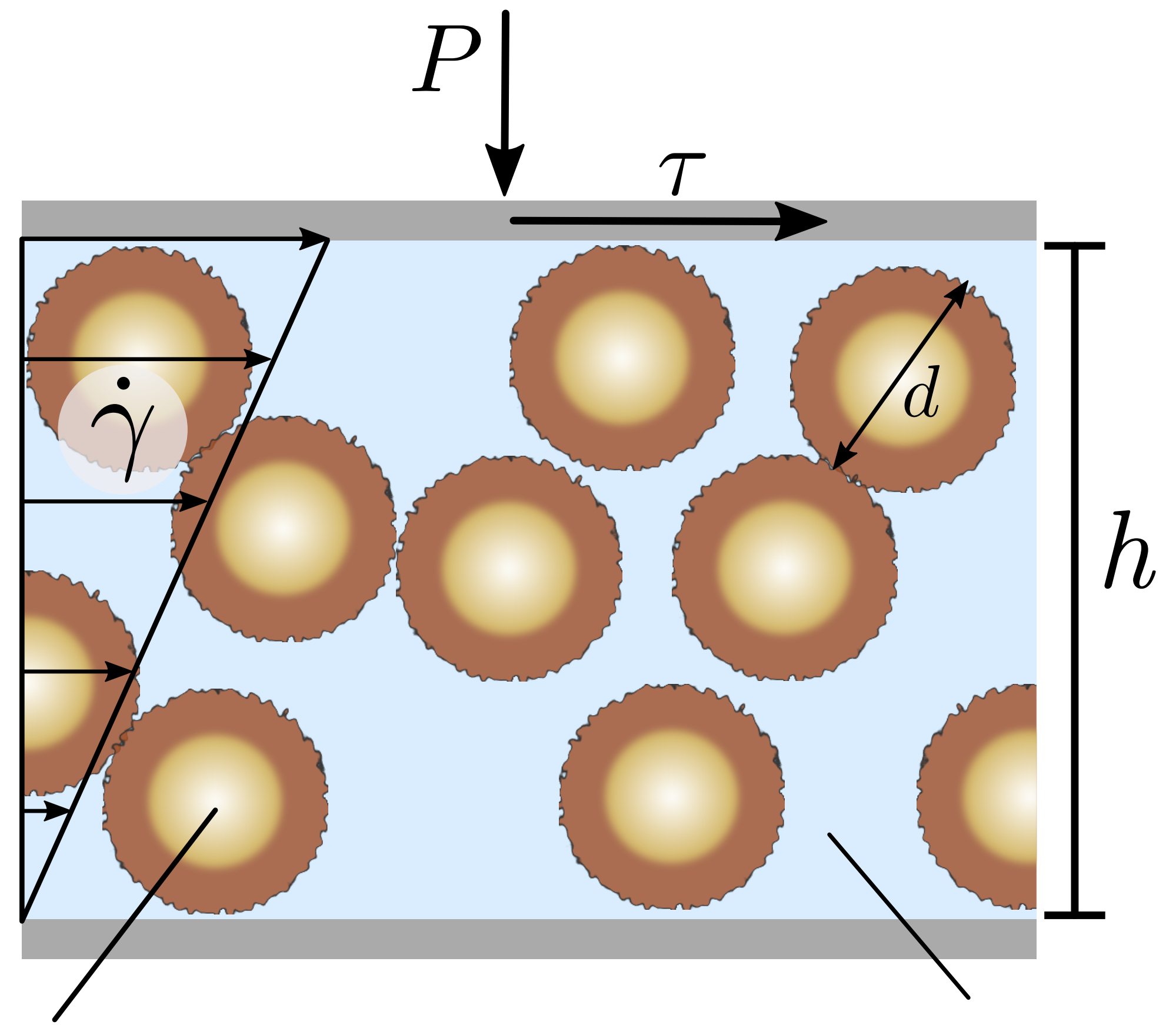
Hydrodynamics

Solid contacts

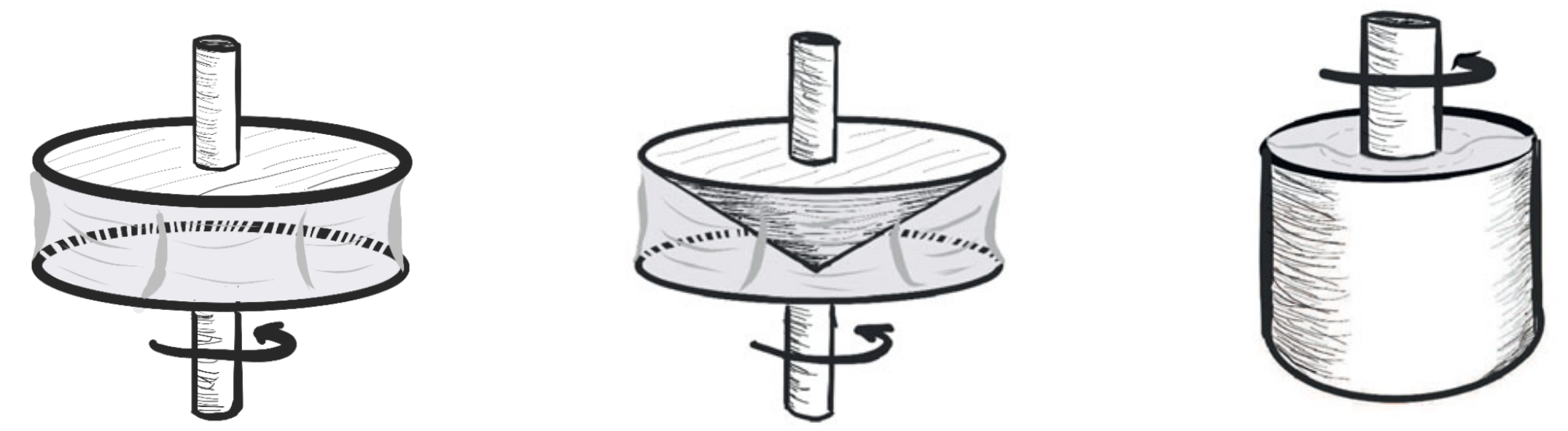
Friction

# Rheology of Granular Suspensions

$$\left\{ \begin{array}{l} \rho_p = \rho_f \quad Re = \frac{\rho_f \dot{\gamma} h^2}{\eta_f} \ll 1 \quad St = \frac{\rho_p \dot{\gamma} d^2}{\eta_f} \ll 1 \end{array} \right.$$



## “Classical” Rheology (volume—imposed)



Volume Fraction,  $\phi$   
Shear Rate,  $\dot{\gamma}$



**Imposed**

Shear Stress,  $\tau$



**Measured**

??

$$\tau = \boxed{\eta_s(\phi)} \eta_f \dot{\gamma}$$

Non-Brownian, rigid & frictional particles

viscous fluid  
 $\eta_f, \rho_f$

$$\phi = \frac{\text{Vol of Grains}}{\text{Total Volume}}$$

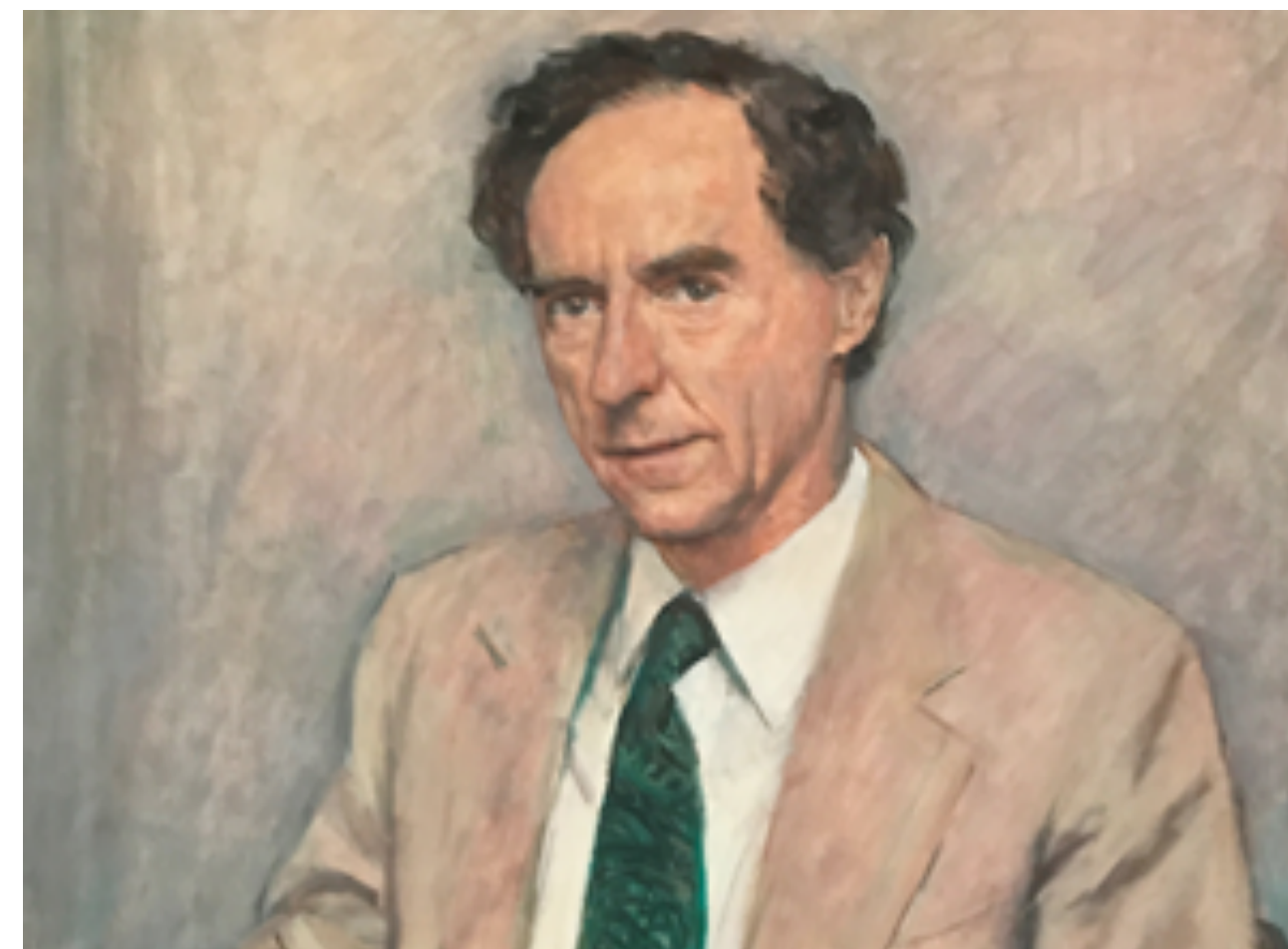
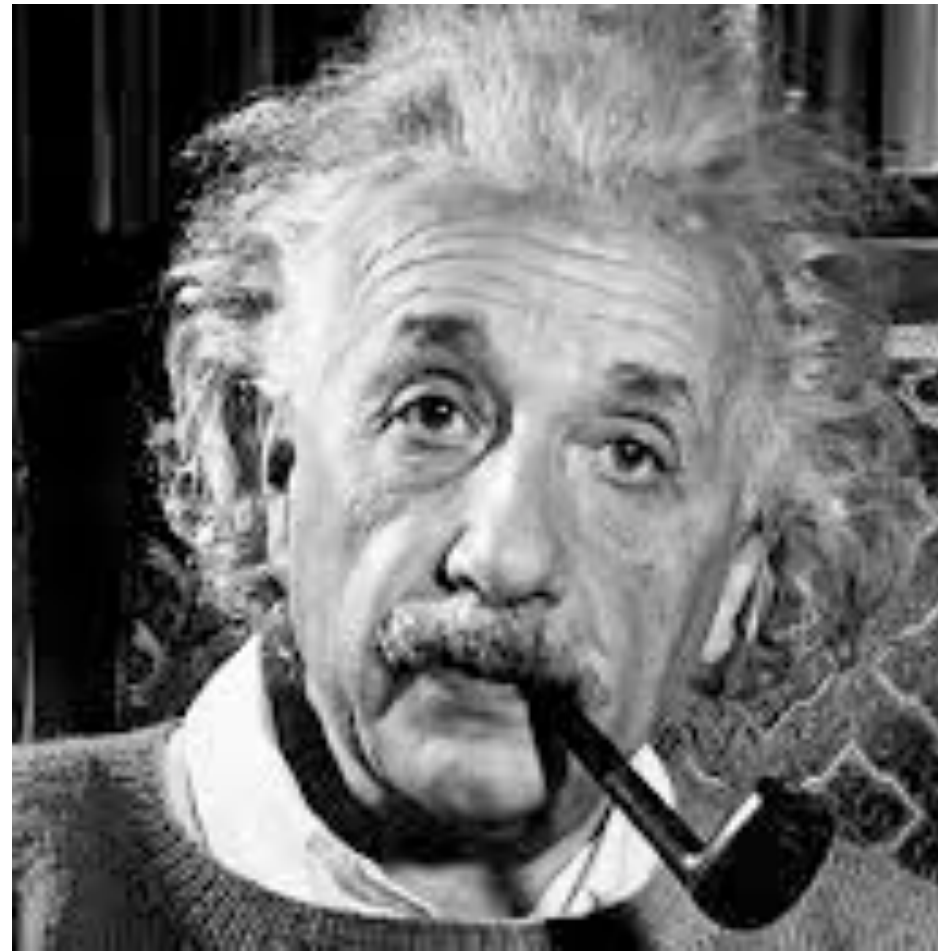
# Suspension Effective Viscosity

1906

1972

2000

Chronology &  $\phi$



*What about dense regime?*



(A. Einstein PhD Thesis 1906)

(Batchelor & Green JFM 1970)

$$\eta_s(\phi) = 1 + 5\phi/2$$

$$\eta_s(\phi) = 1 + 5\phi/2 + \lambda\phi^2$$

*Multibody interactions:*  
*no exact analytical solution!*

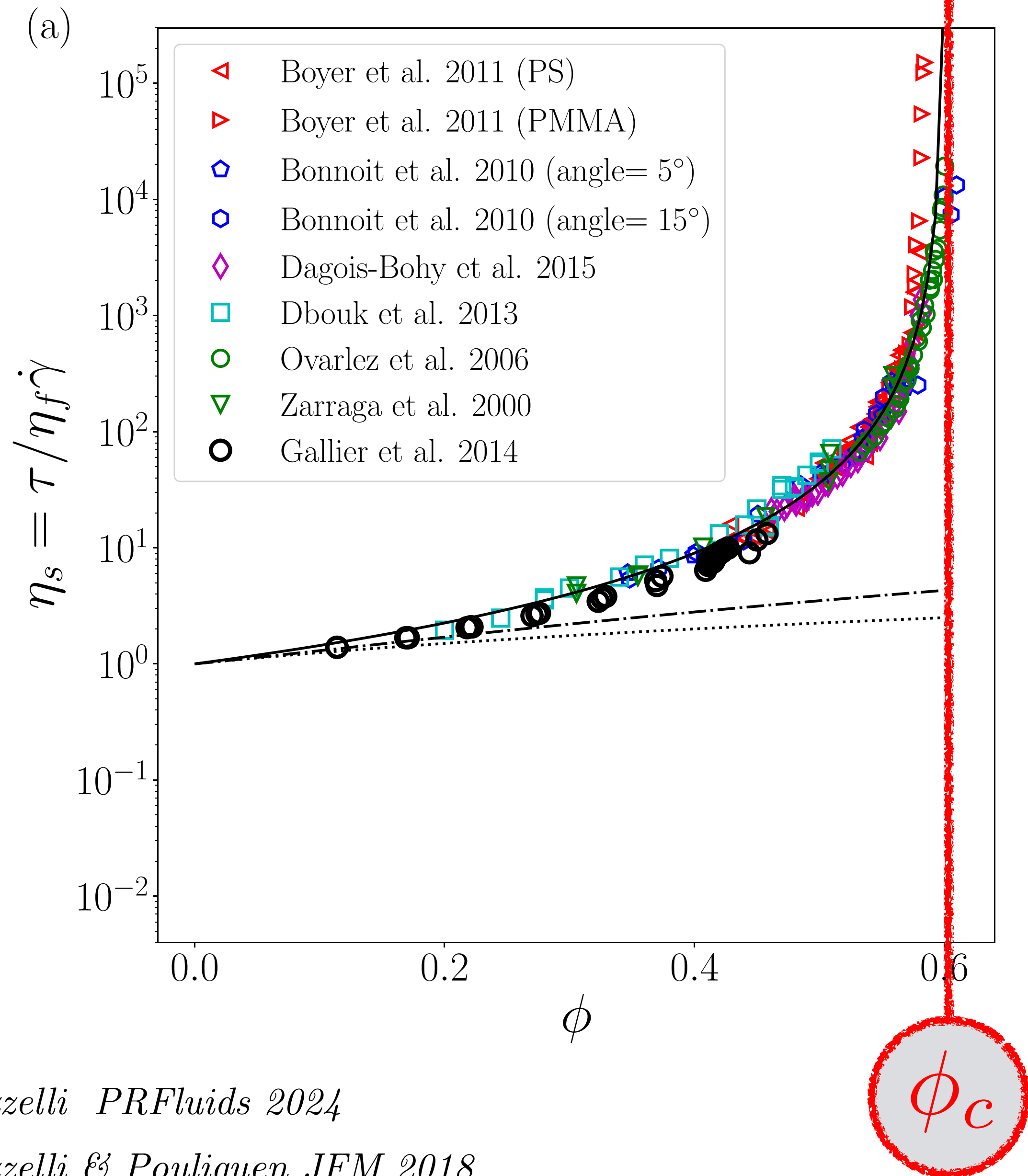
*Stresslet dissipation*

— *Dilute regime* —

*Pair interactions*

— *Semi-dilute regime* —

# Suspension Effective Viscosity: Empirical Observations



$$\tau = \eta_f \eta_s(\phi) \dot{\gamma}$$

$$\eta_s(\phi) \sim (\phi_c - \phi)^{-2}$$

*Viscosity is set by  
the distance to Jamming!*



Even the simplest case introduces strange behaviours...

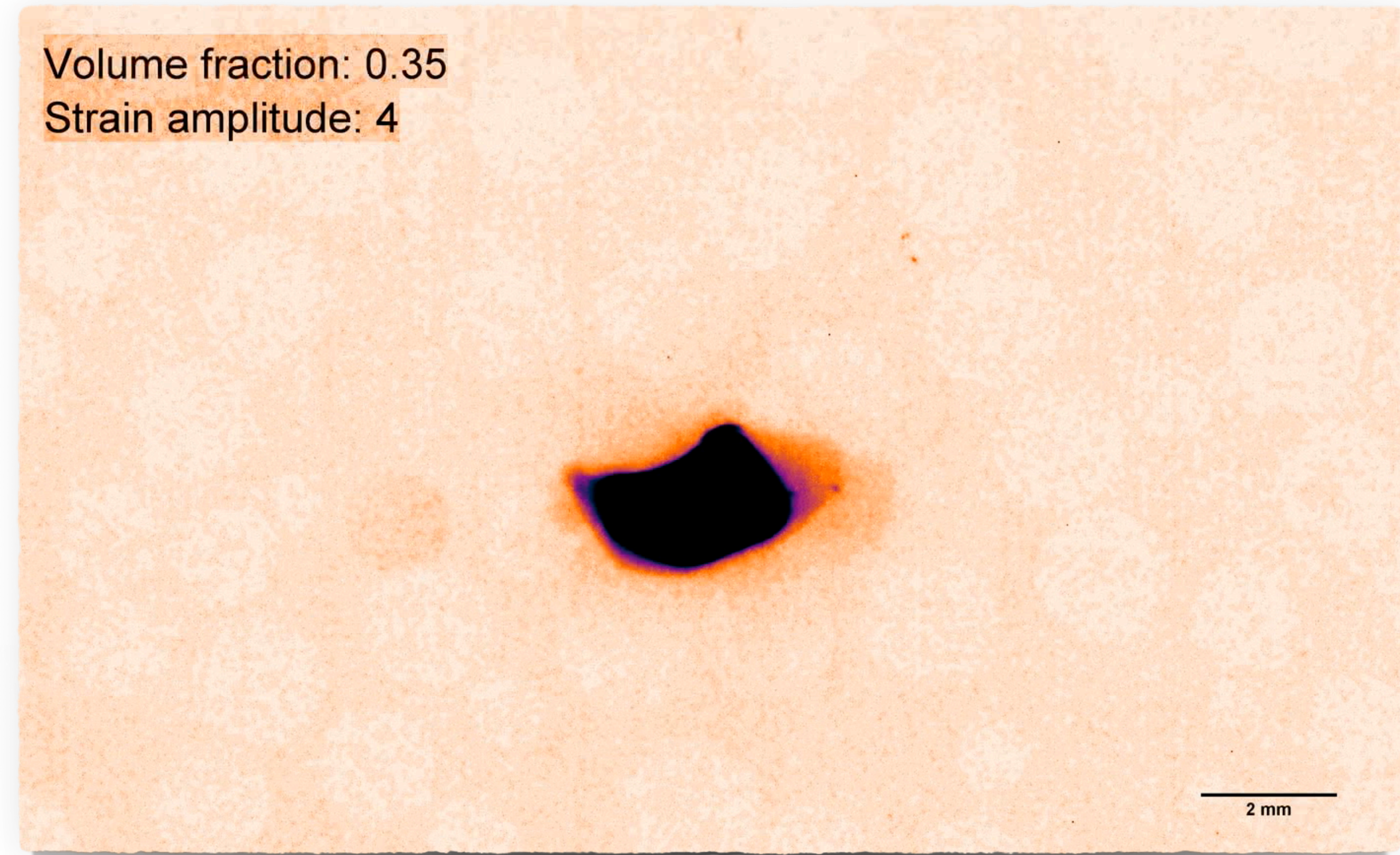
*e.g. loss of reversibility*

*Taylor's experiment with pure viscous fluid*



*G.I. Taylor (1967)*

*Taylor's experiment in a granular suspension*

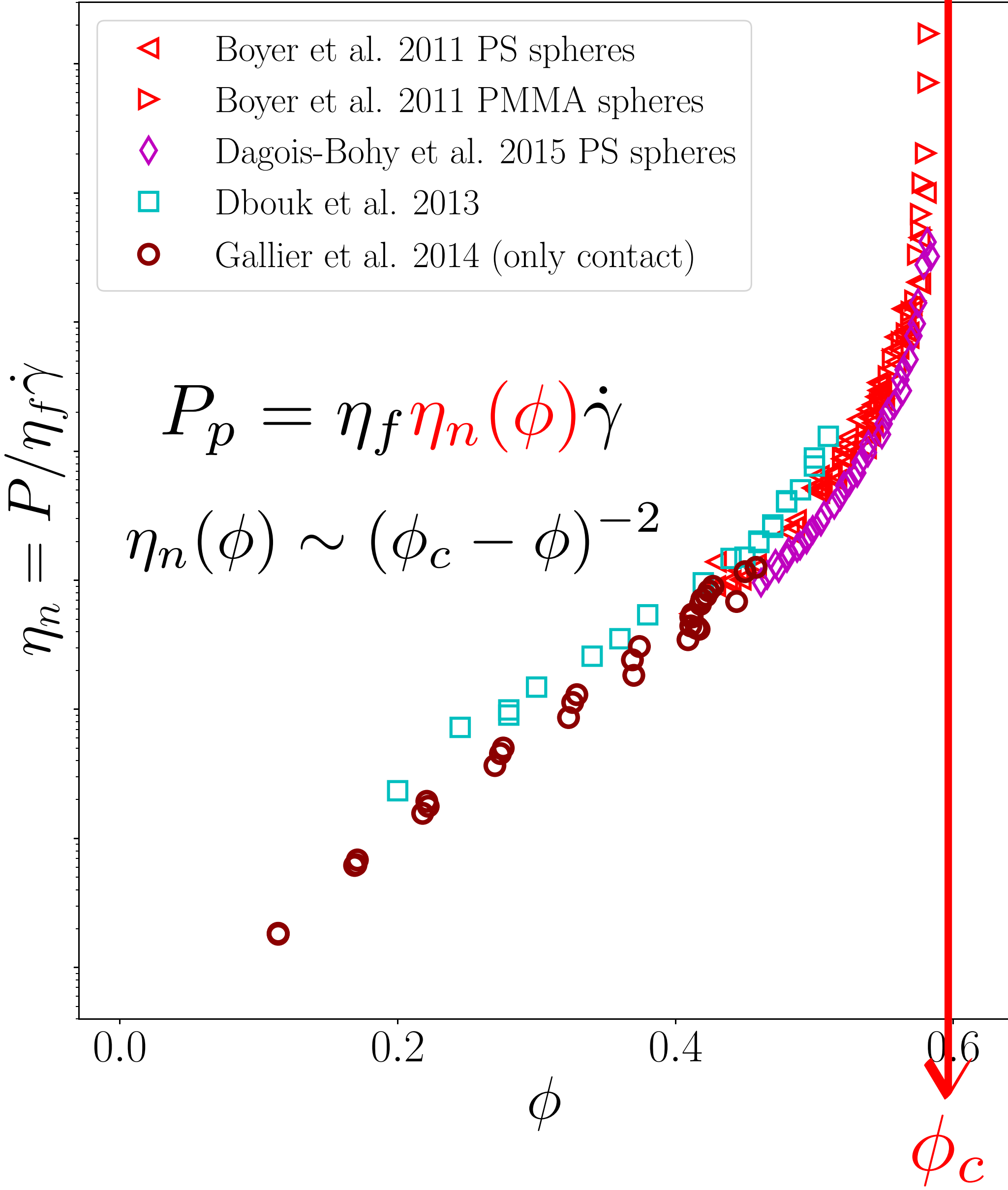
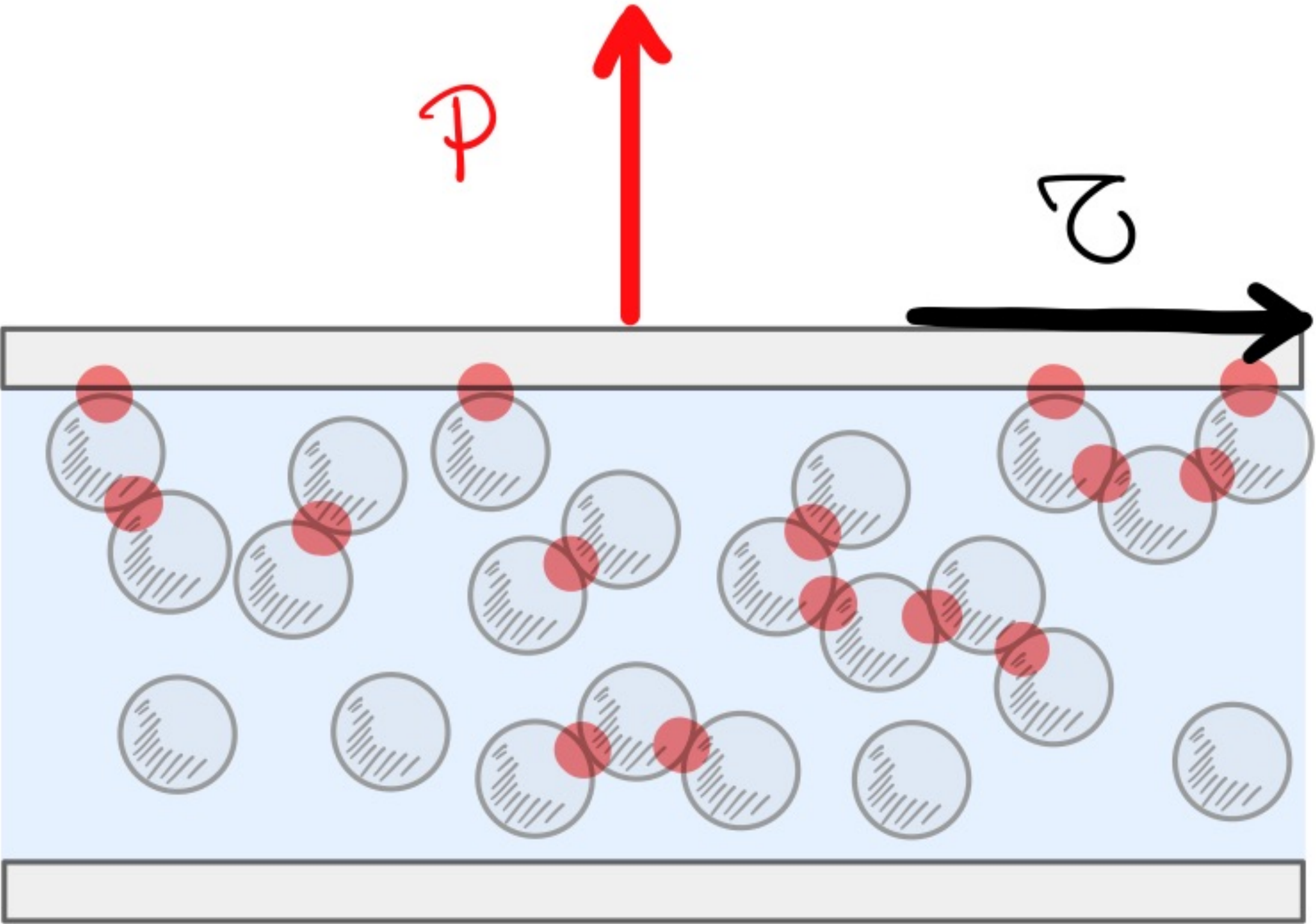


*Souzy, Phom & Metzger PRF (2016)*



# Even the simplest case introduces strange behaviours...

*e.g. Particle Pressure*



Guazzelli *PRFluids* (2024)

Guazzelli & Pouliquen *JFM* (2018)

# Dominant Interactions

*Guazzelli & Pouliquen JFM (2018)*

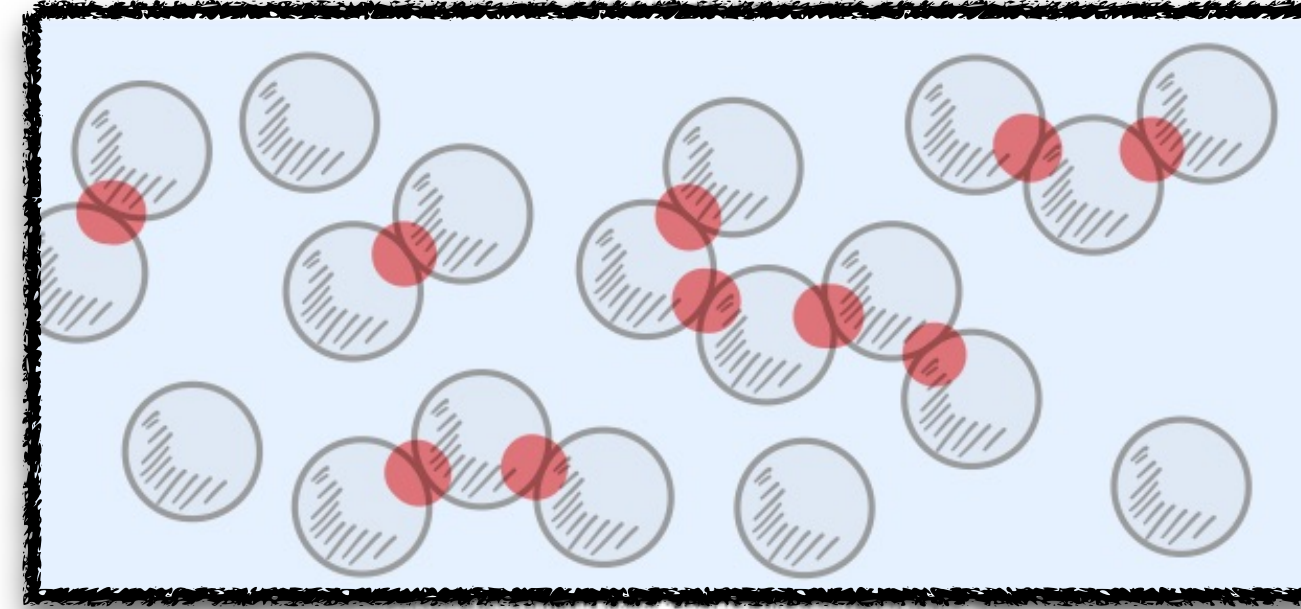
*Gallier, Lemaire, Peters & Lobry JFM (2013)*

## Dilute Regime

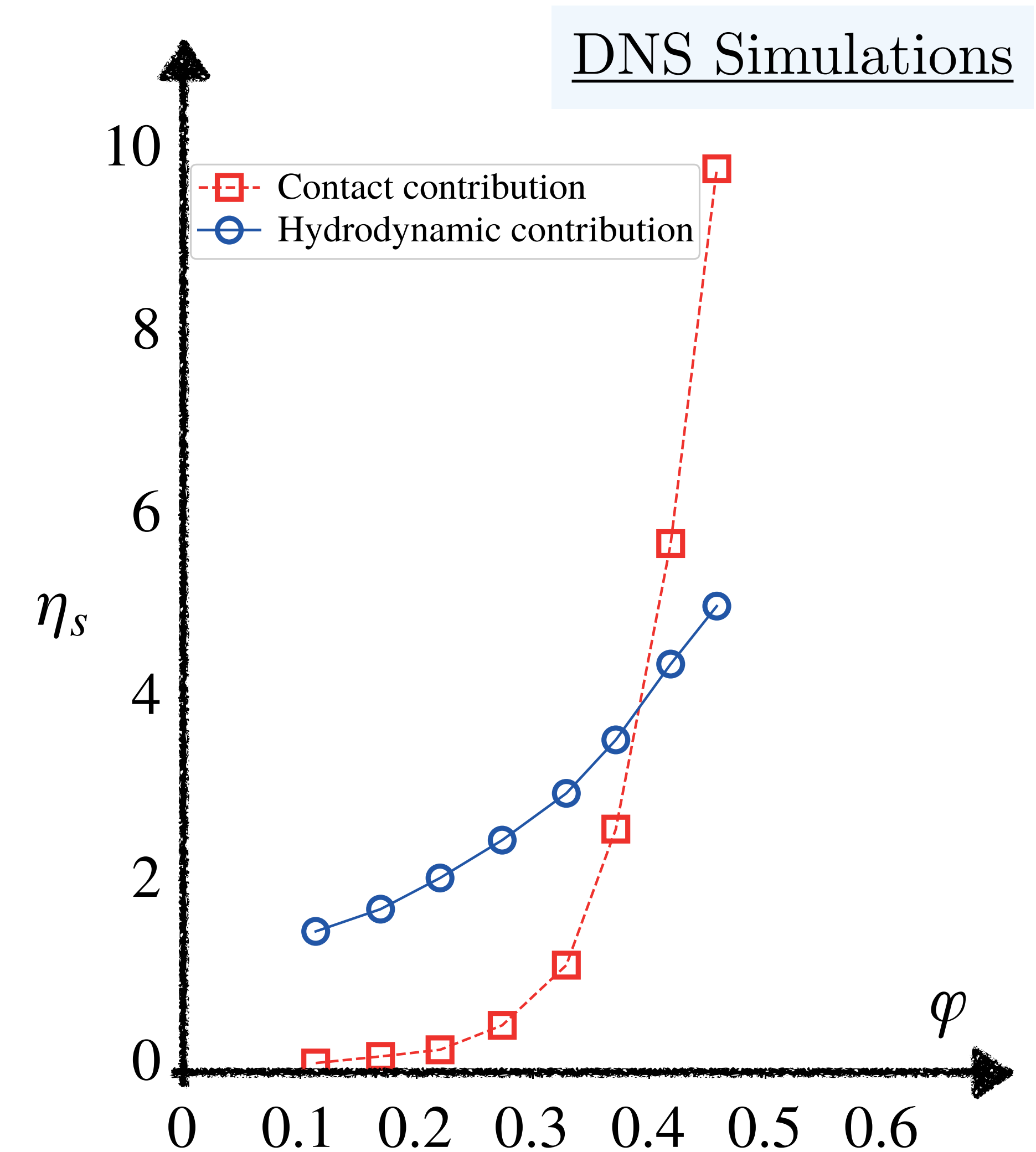


dominated by  
long-range hydrodynamic  
interactions

## Dense Regime



contact dynamics  
take over!



# An Alternative Approach

*GdR MiDi (2004)*  
*da Cruz et al (2005)*  
*Jop, Forterre & Pouliquen (2006)*

In many practical situations the volume is not imposed!



Pressure is imposed  
(e.g. by gravity!)



*Johnson et al. JGR (2012)*

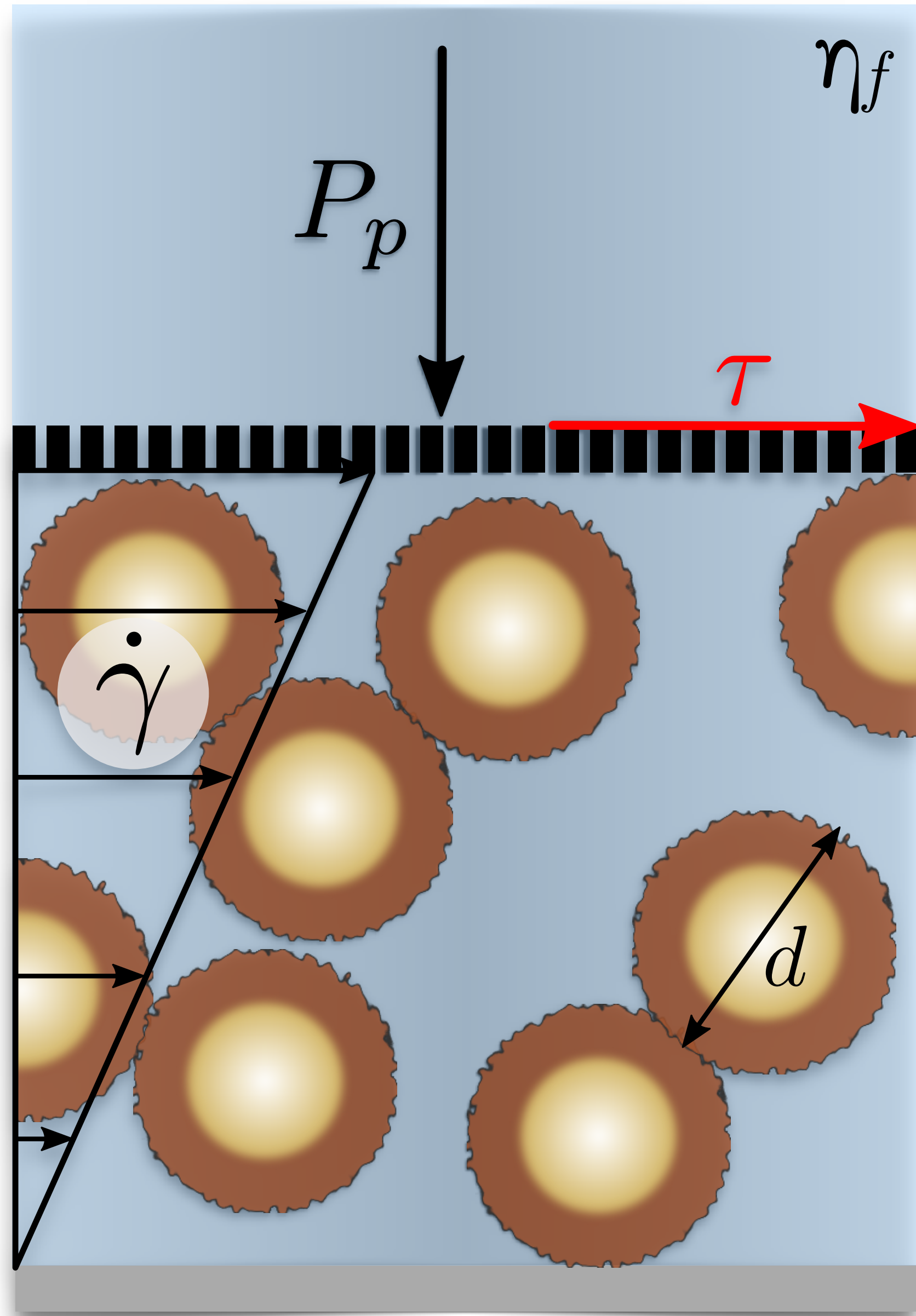


*Johnson & Gray JFM (2012)*



*Rocha et al. JFM (2019)*

# Pressure—imposed Rheology



Particle Pressure,  $P_p$

Shear Rate,  $\dot{\gamma}$



Imposed

Shear Stress,  $\tau$

Volume Fraction,  $\phi$



Measured

1 dimensionless Number

→  $J = \frac{\eta_f \dot{\gamma}}{P_p}$

Viscous Number

Viscous stress / Imposed Pressure

Dimensionless Shear Rate

Frictional Rheology:

$$\tau = \mu(J) P_p$$

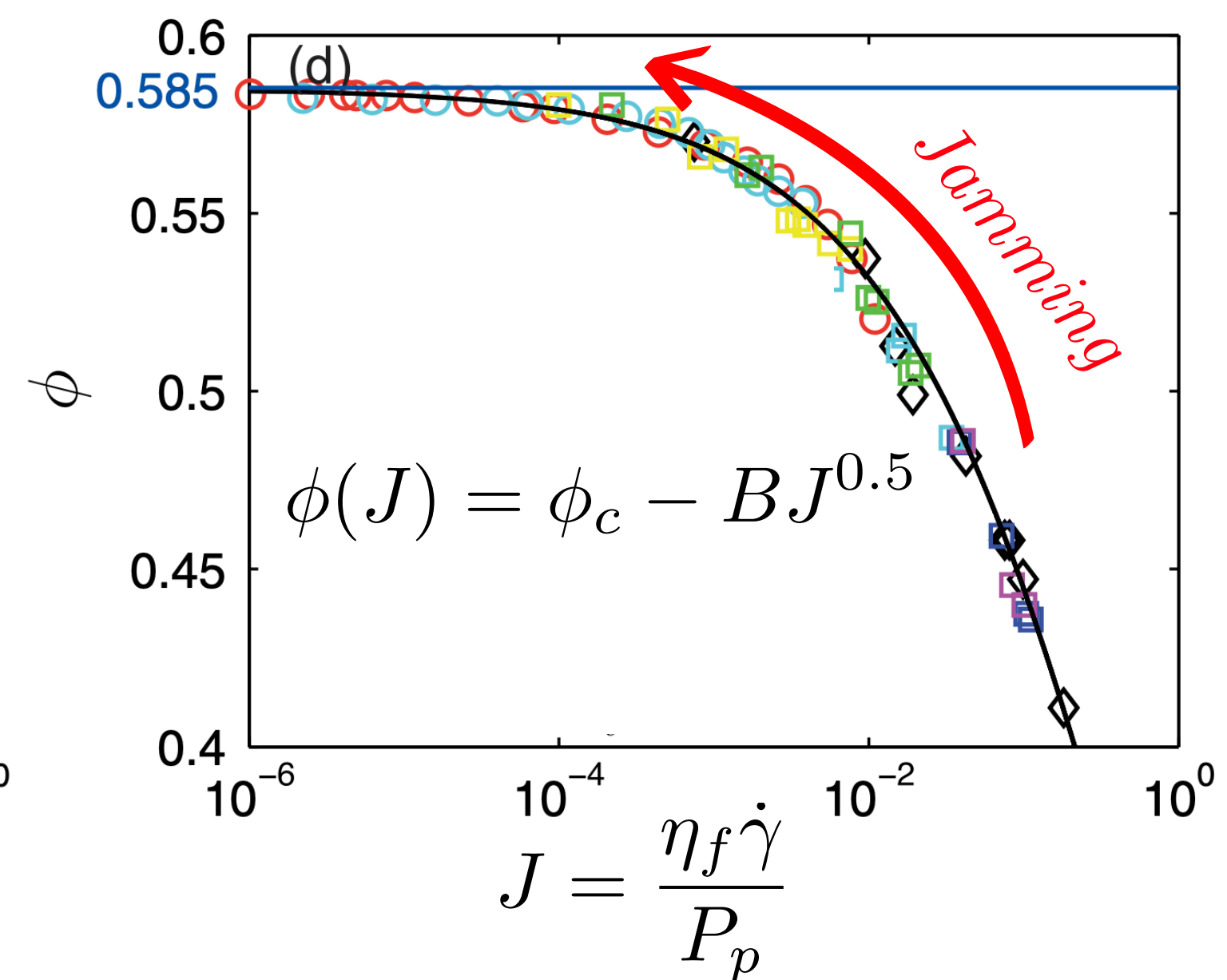
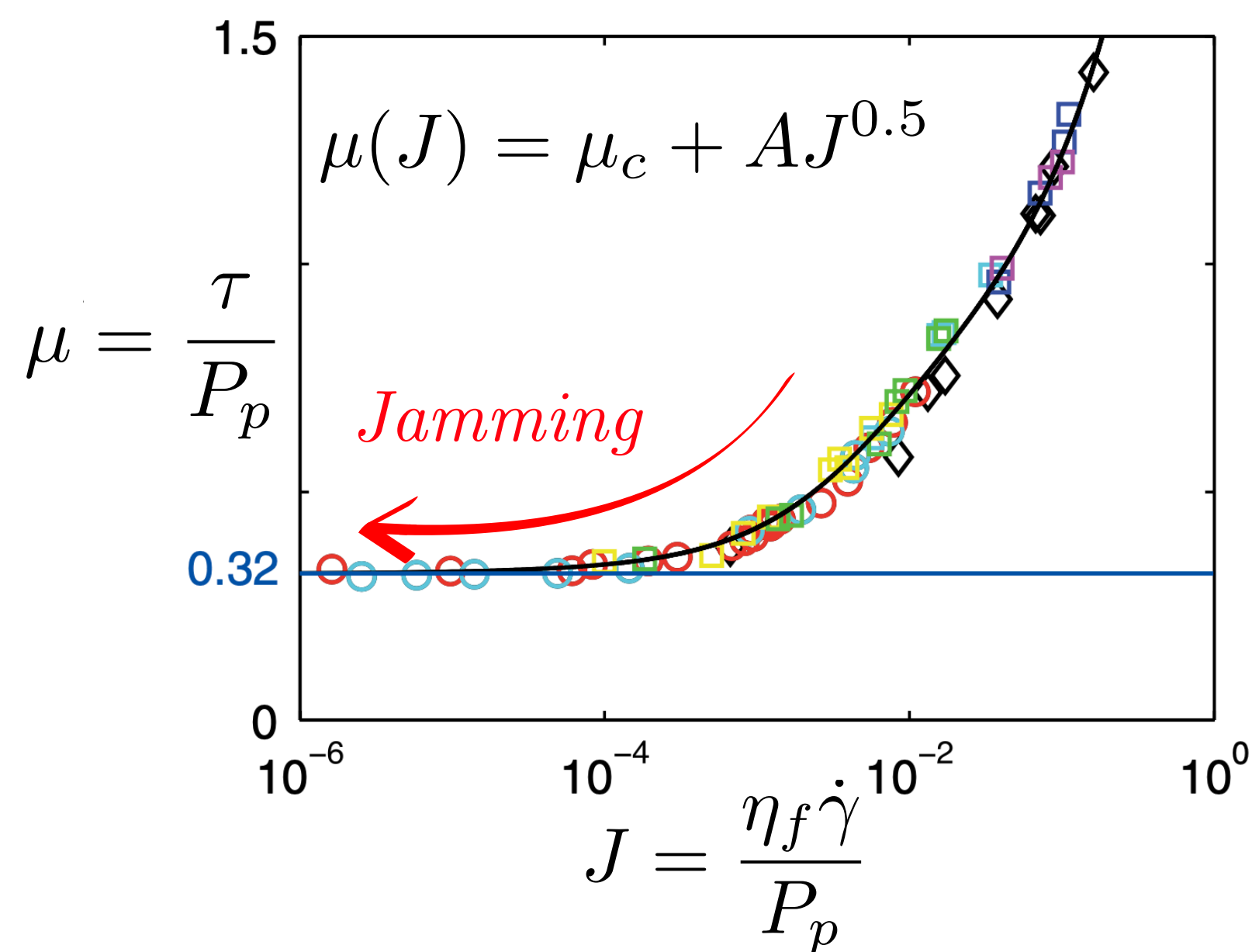
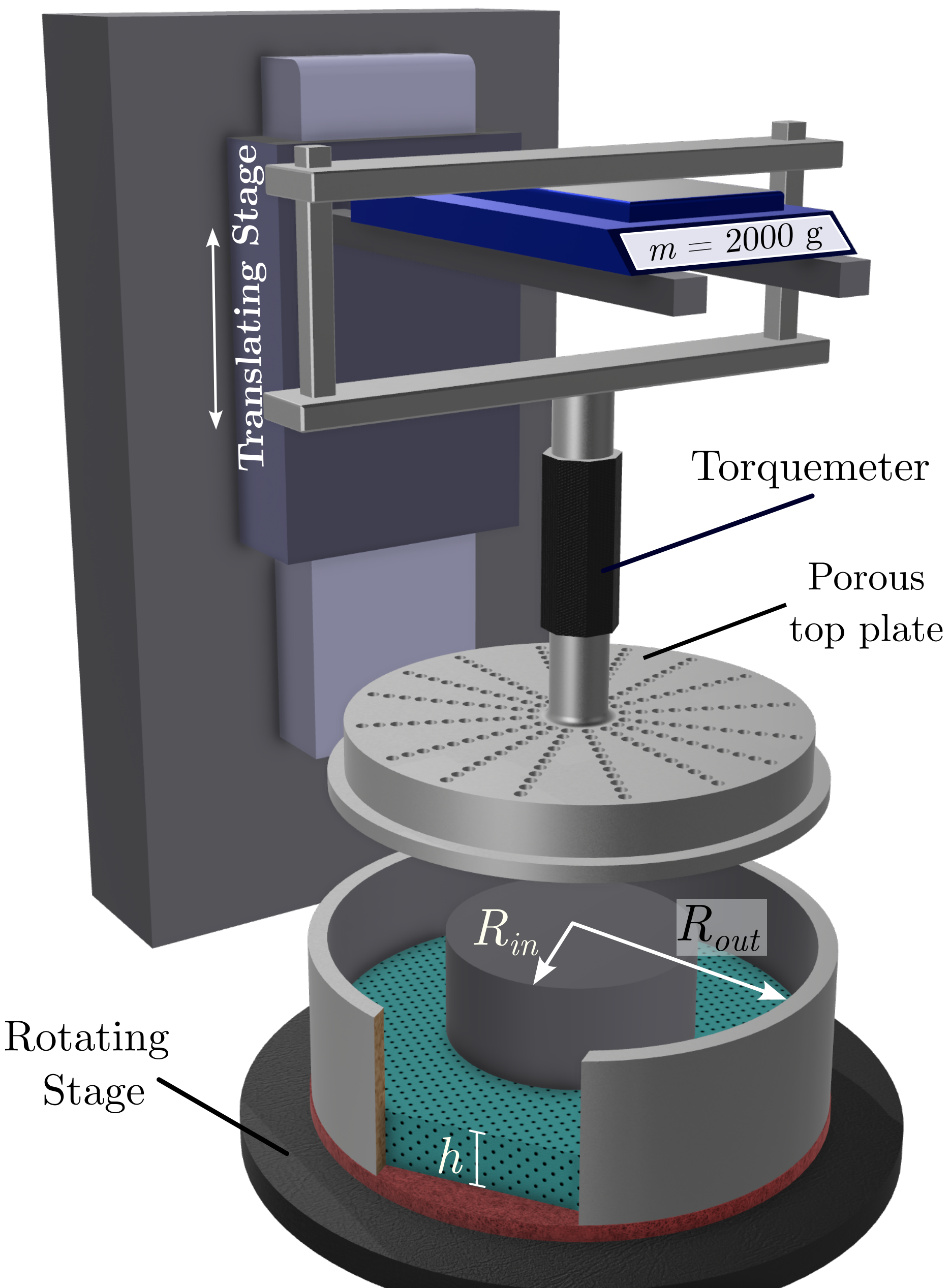
$$\phi = \phi(J)$$

Macroscopic (bulk)  
Friction Coefficient

# Pressure-imposed Rheology

Boyer, Guazzelli, Pouliquen PRL (2011)

Dagois-Bohy et al. JFM (2015)

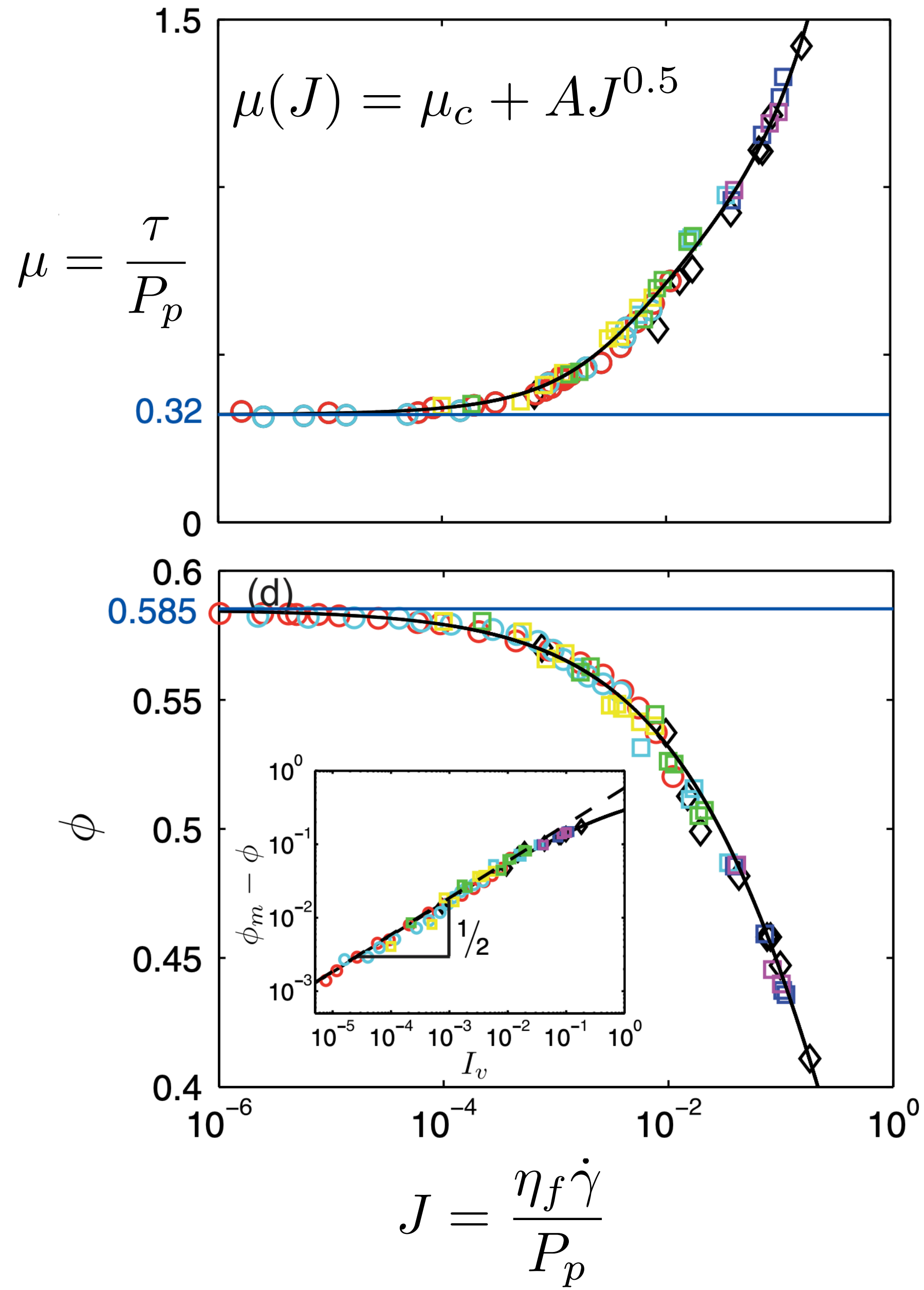


→ Allows particle pressure  $P_p$  to be measured directly.

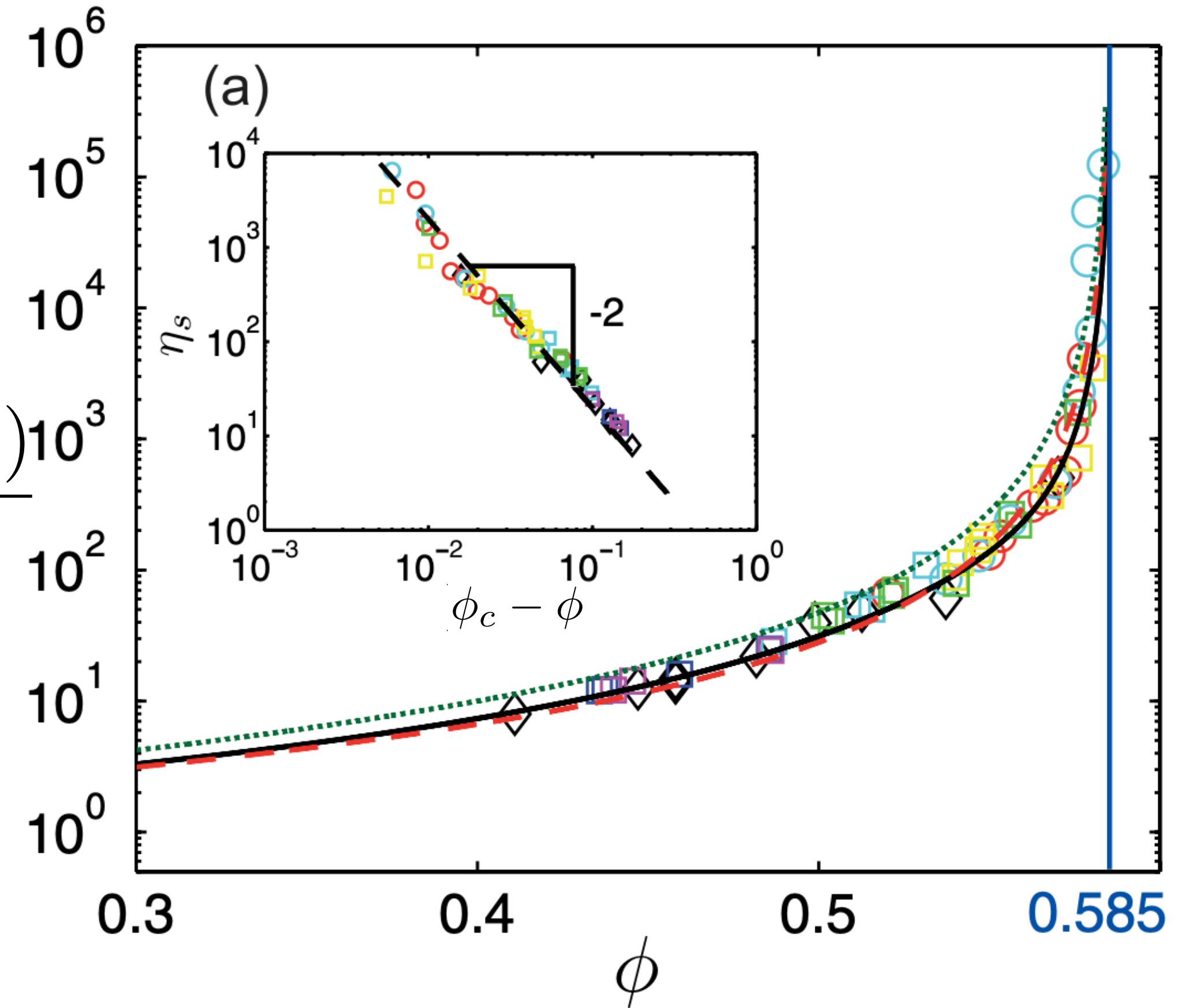
→ Since there is no divergence, it allows to get much closer to jamming!

→ Not very accurate in the dilute regime

# From Pressure— to Volume—Imposed Rheology



$$\eta_s = \frac{\mu(J(\phi))}{J} 10^3$$



# So Far...

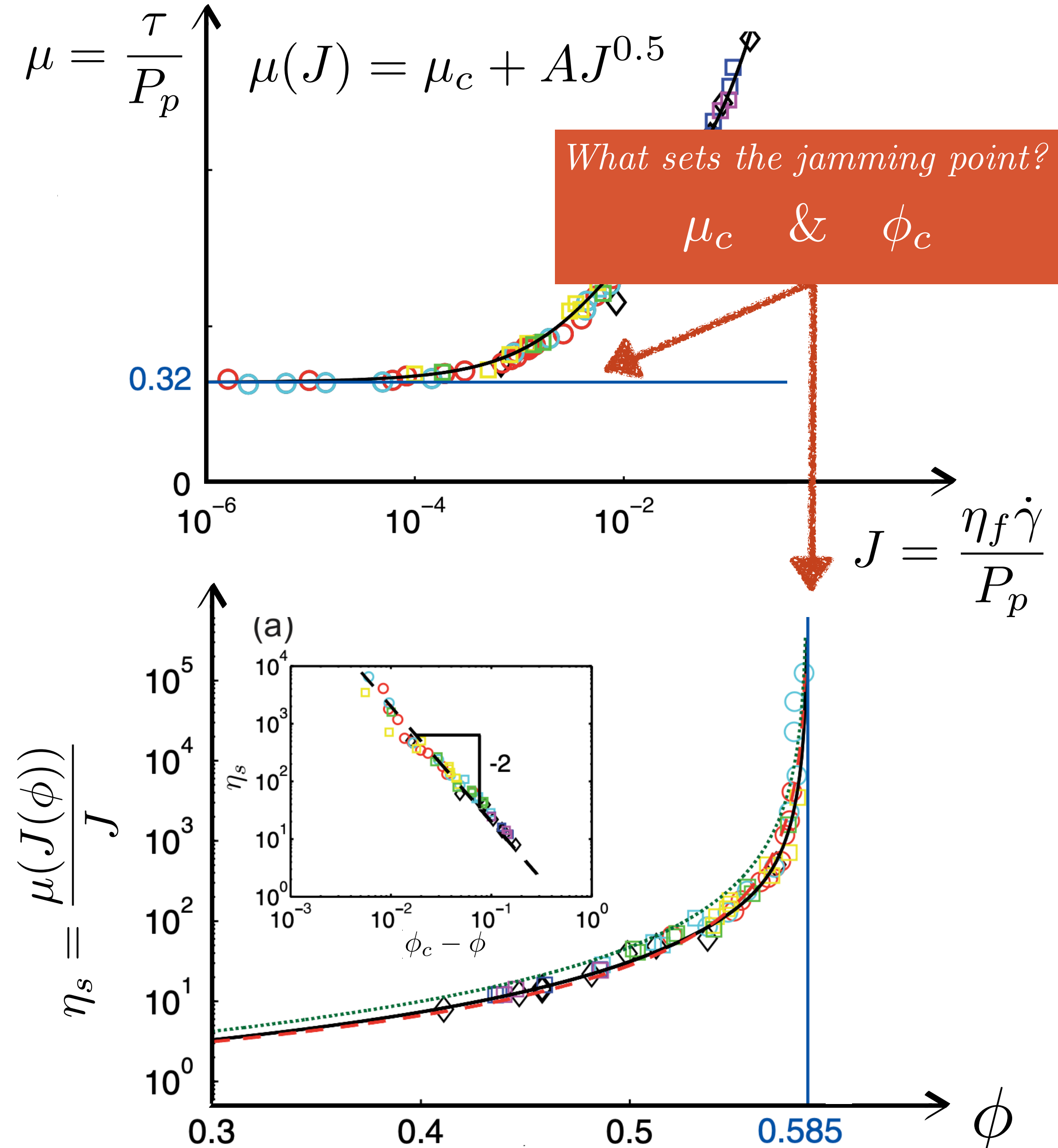
In the dense regime:

- i)* Long-range hydrodynamics become weak
- ii)* Dynamics is dominated by solid contacts

Volume—imposed *vs* Pressure—Imposed

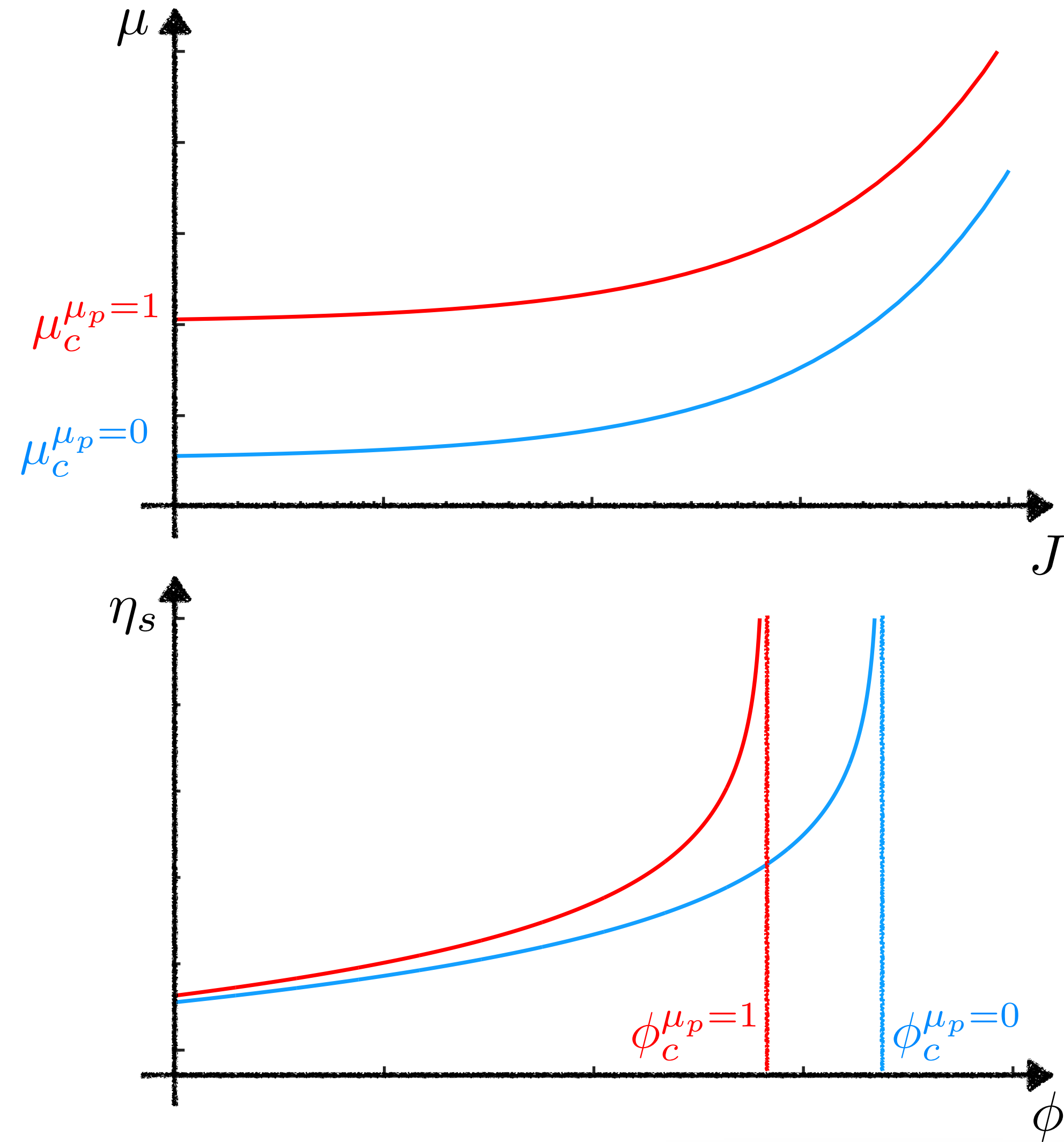
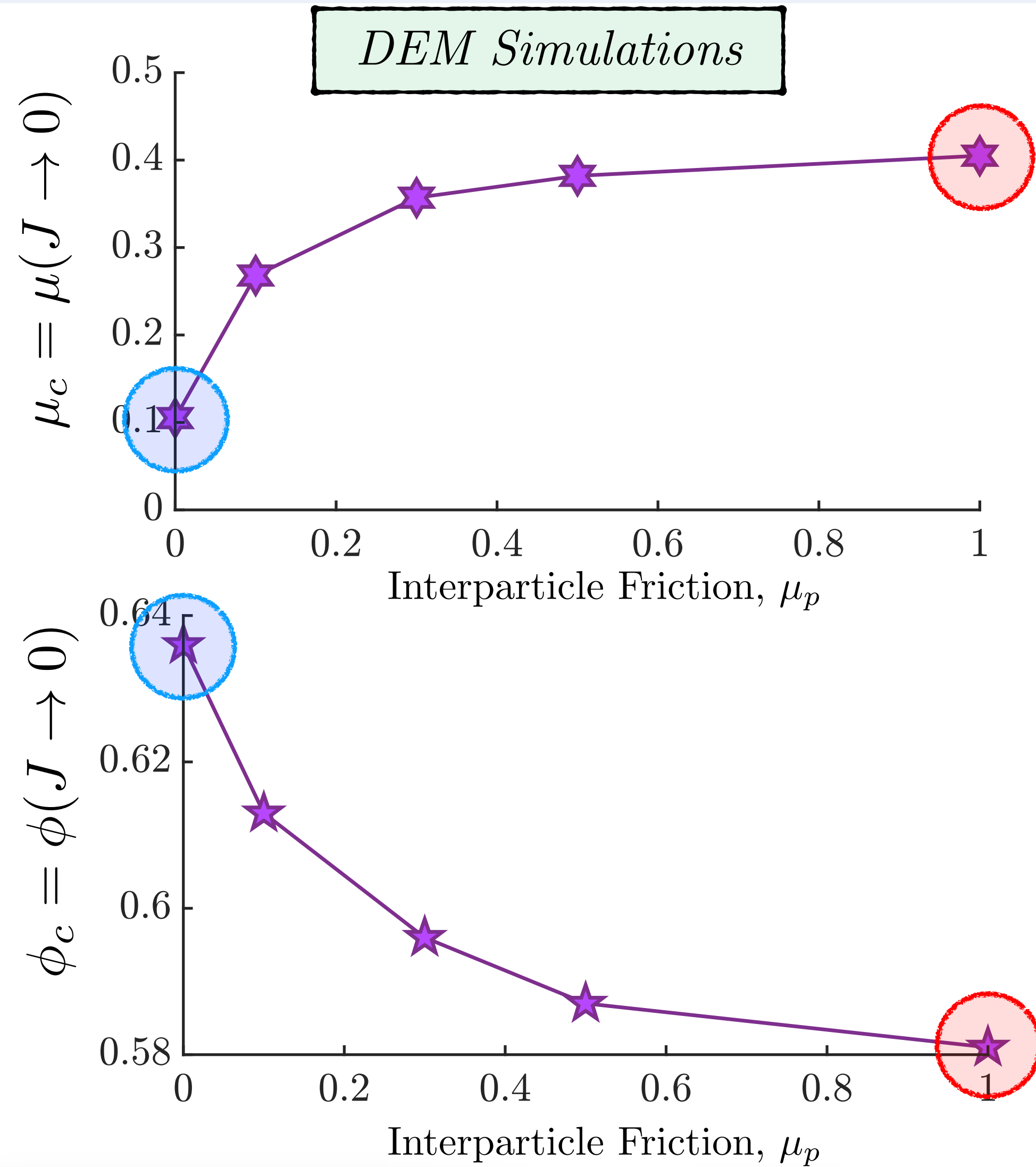
$$\begin{aligned} \tau &= \eta_f \eta_s(\phi) \dot{\gamma} & \tau &= \mu(J) P_p \\ P_p &= \eta_f \eta_n(\phi) \dot{\gamma} & \phi &= \phi(J) \end{aligned}$$

Equivalent Flow Rules!



# What sets the jamming point?

Chialvo, Sun & Sundaresan PRE (2012)



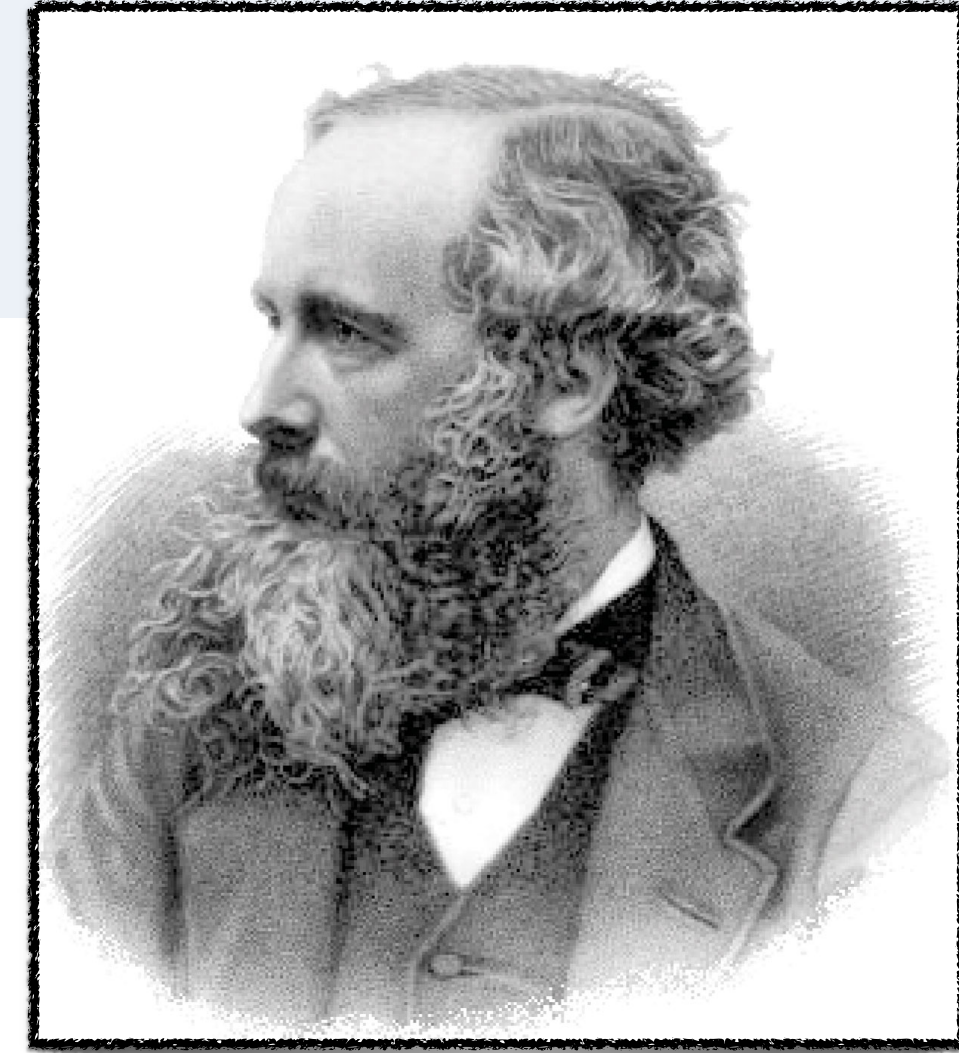
*The jamming point depends on the interparticle friction coefficient!!*



# Why $\mu_p$ affects the Jamming Point?

What is the minimum number of contacts to reach rigidity?

*Isostaticity — enough contacts to constraint all degrees of freedom*



*James C. Maxwell*



Maxwell's Stability Criterion

*Number of Constraints*  $\geq$  *Degrees of Freedom*

# Why $\mu_p$ affects the Jamming Point?

## Maxwell's Stability Criterion

$$\text{Number of Constraints} \geq \text{Degrees of Freedom}$$

### Frictionless Contacts:

$$\frac{z_c N}{2} = 3N$$

1 constraint [no penetration]      3 DoF [translation]

$$z_c = 6$$

contacts per particle

### Frictional Contacts:

$$\frac{3z_c N}{2} = 6N$$

3 constraint [1 normal + 2 tangential]      6 DoF [translation + rotation]

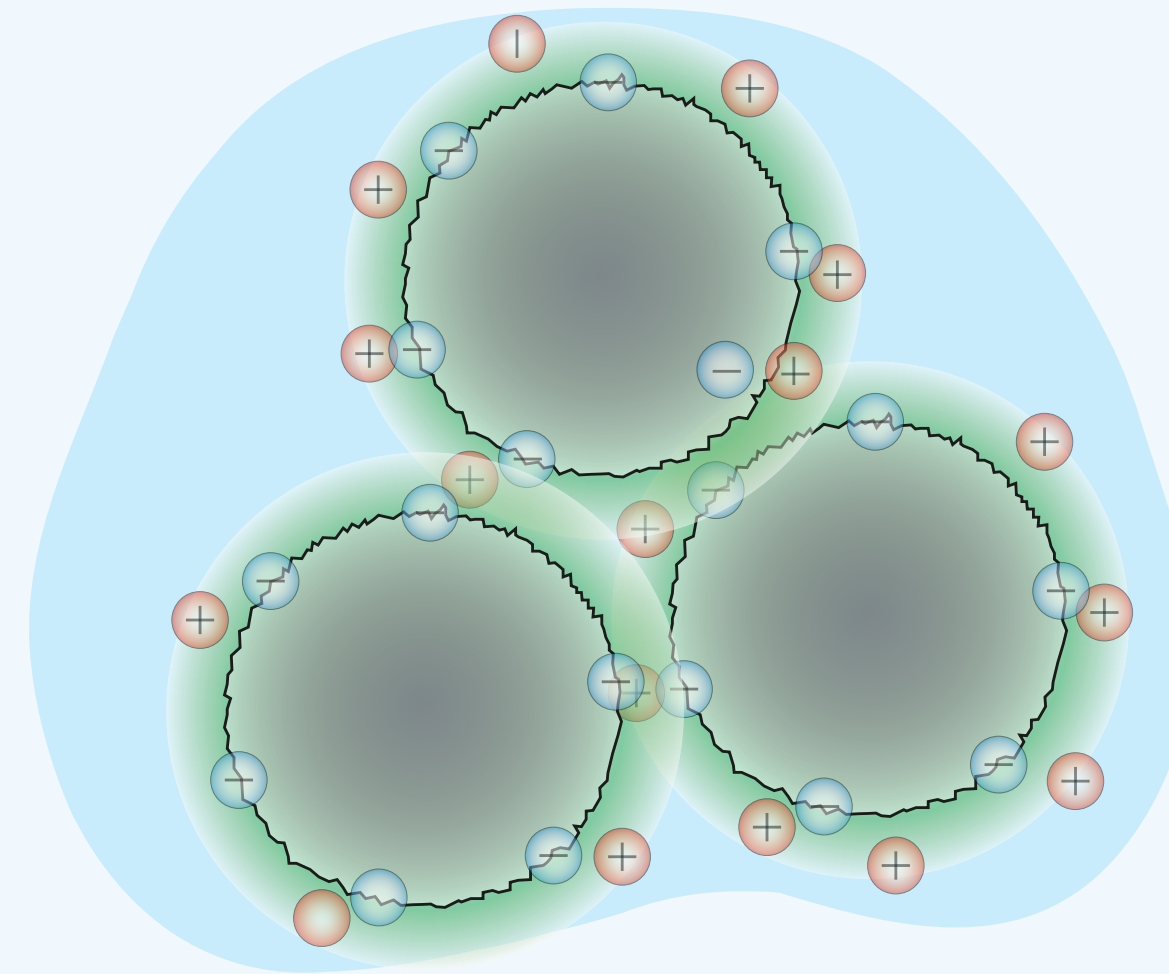
$$z_c = 4$$

contacts per particle

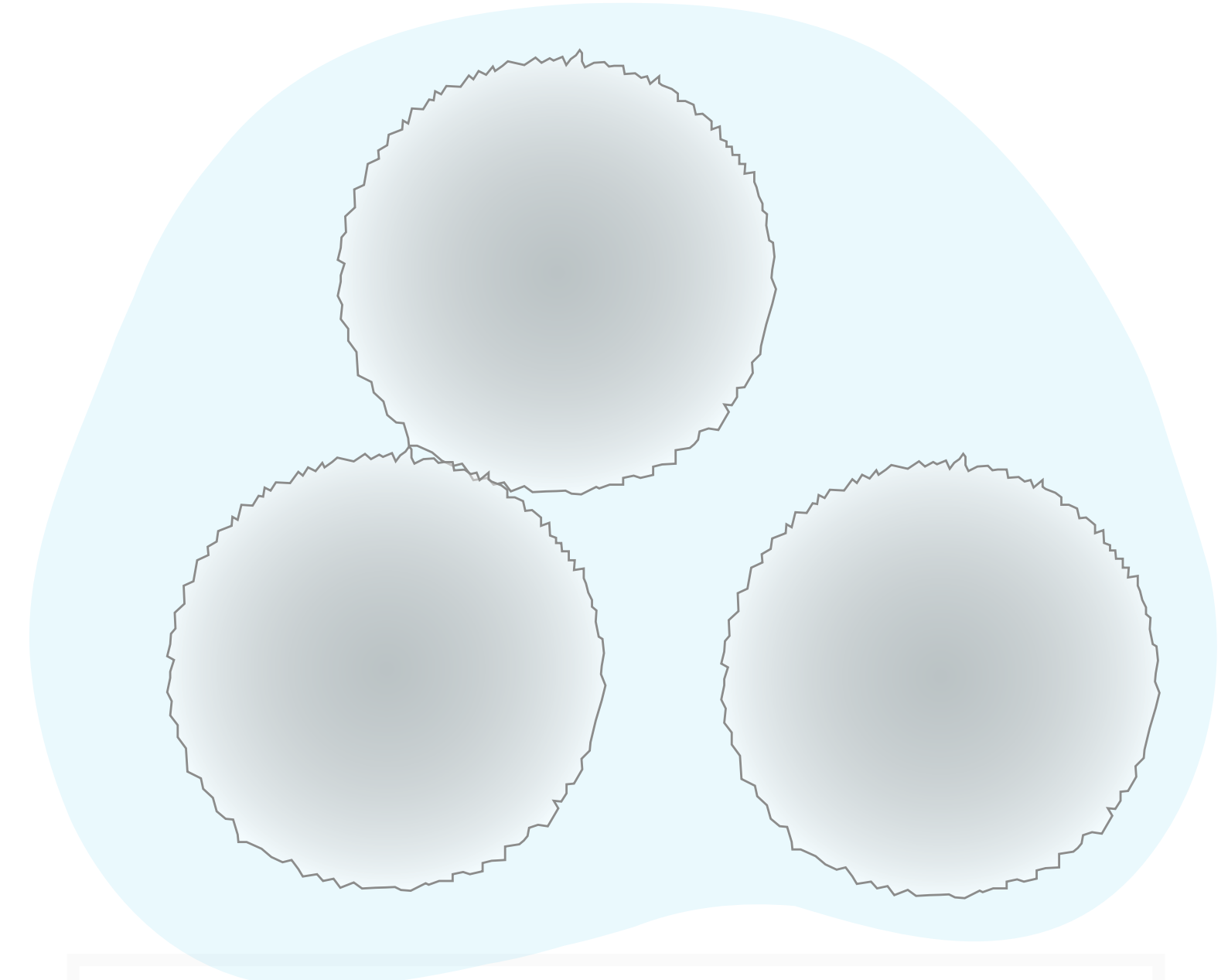
What if the contact can switch depending on flow properties such as stress or shear rate?

# More Recently: Non—Newtonian Behaviours

Brownian/colloidal suspensions



Granular suspensions



$1 \mu\text{m}$

$10 \mu\text{m}$

$100 \mu\text{m}$

Grain size

$d$

Repulsive forces (Electrostatics, Polymer brushes...)

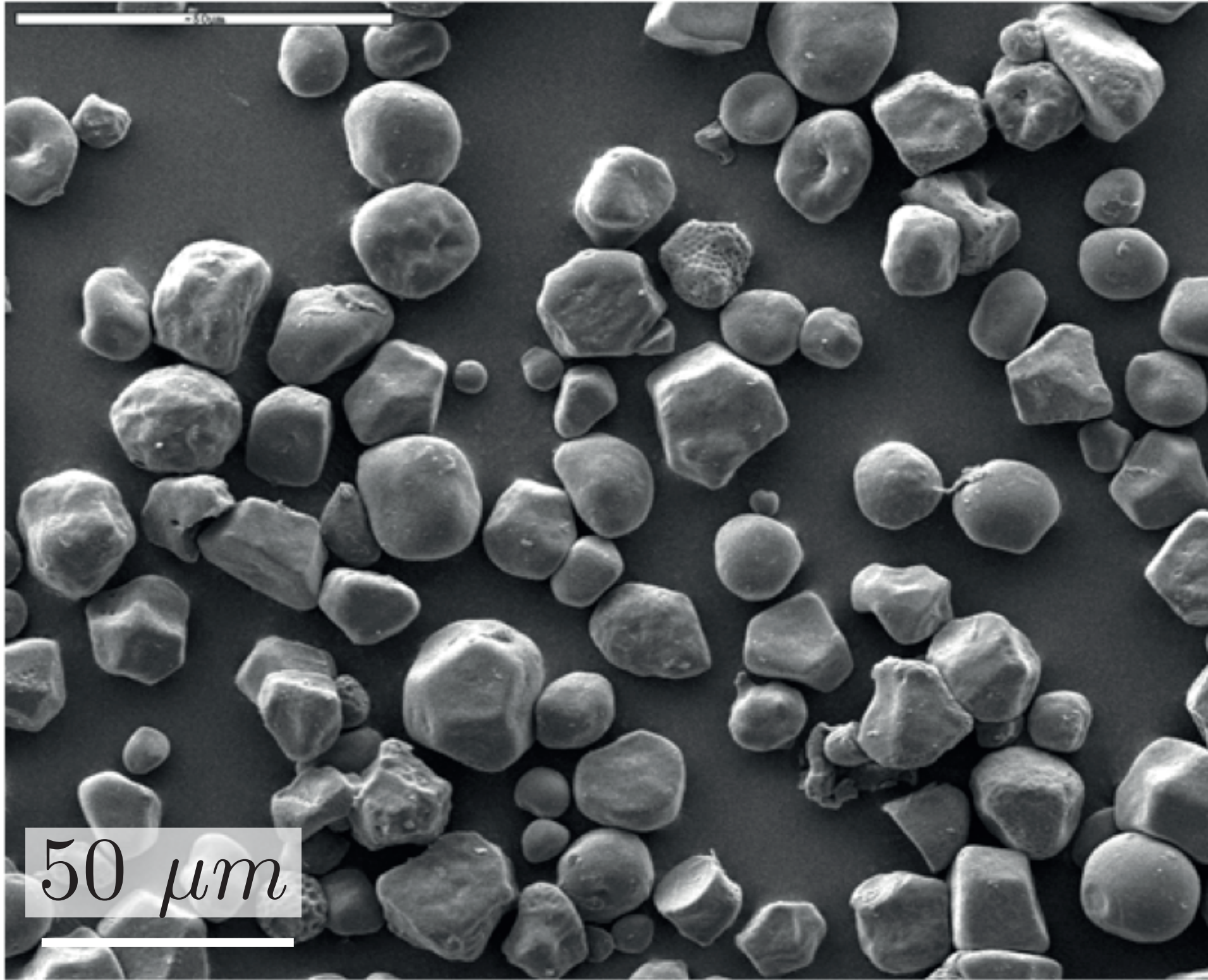
Adhesion forces (Van der Waals,...)

**Hydrodynamics**

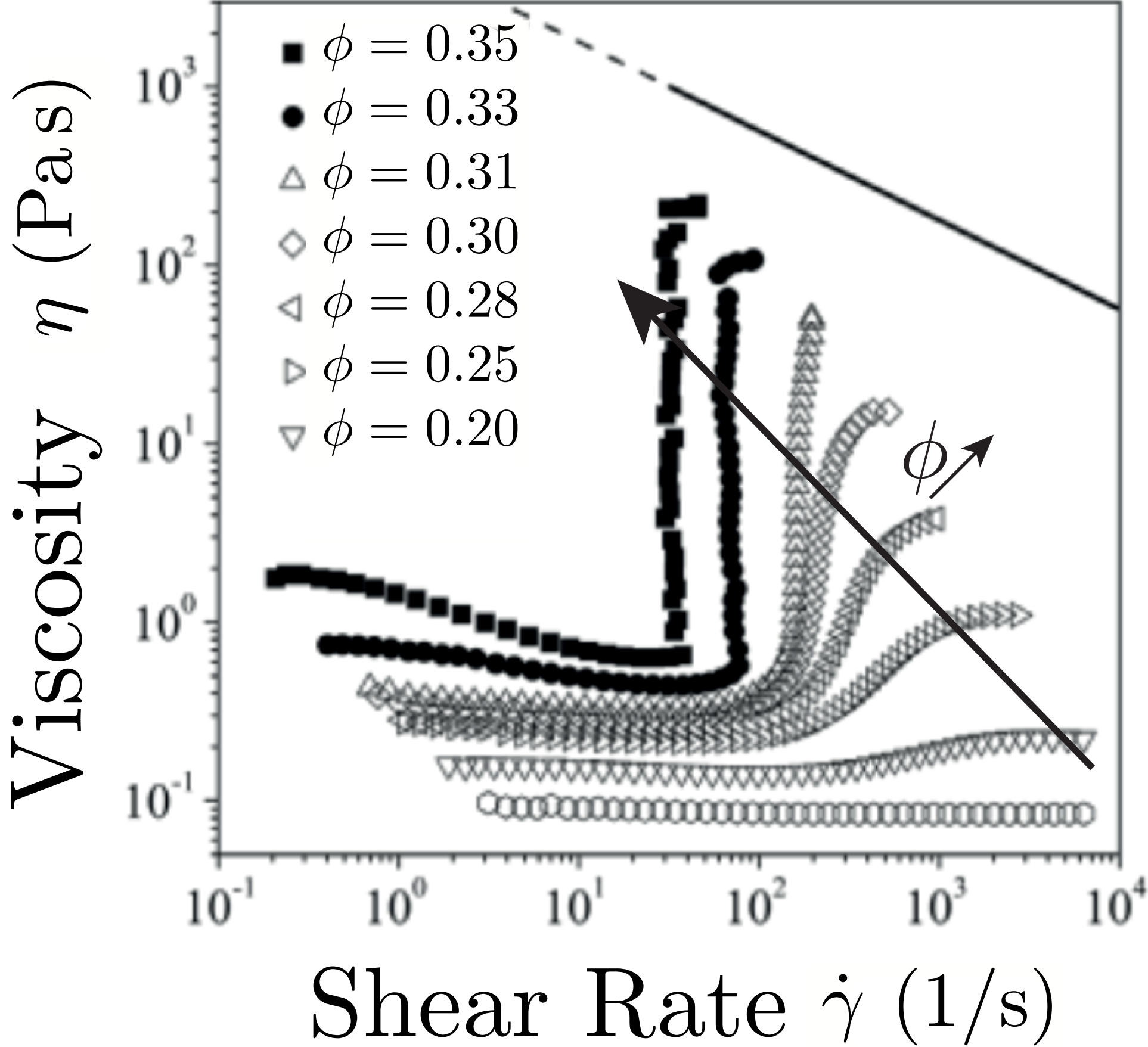
**Solid contacts**

**Friction**

# Shear—Thickening Suspensions: What are they?



*e.g. Cornstarch particles in water*



**Violent increase in suspension viscosity!**

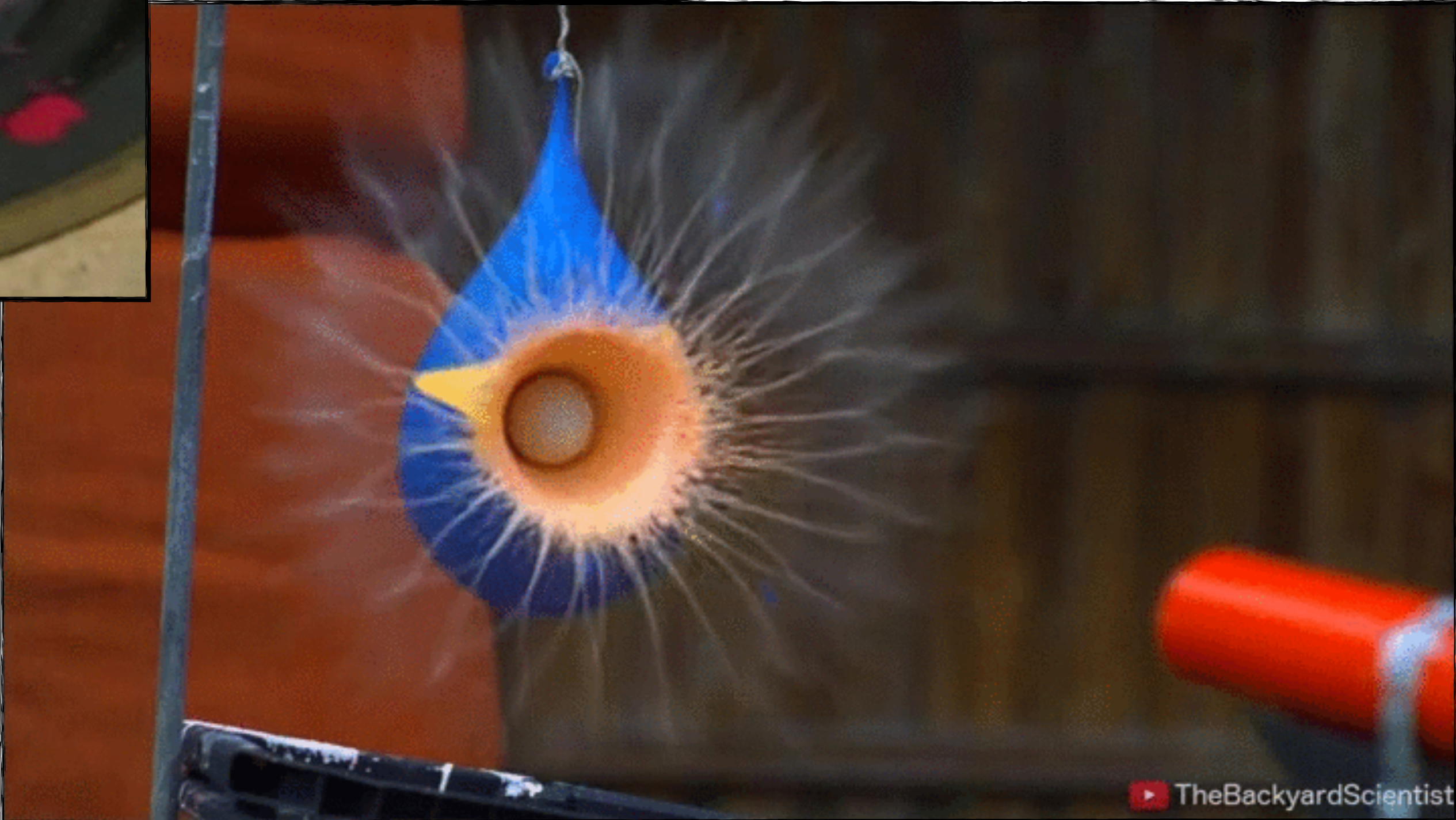


# Shear—Thickening Suspensions: Quite Fun!



*credits: The BackyardScientists (Youtube).*

*credits: The Slow Mo Guys (Youtube).*



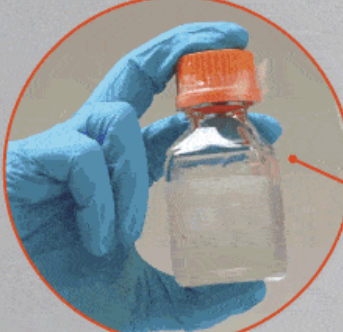
# Some Applications...

## Smart speedbumps

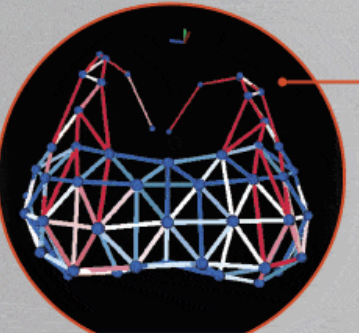


## Sports bra

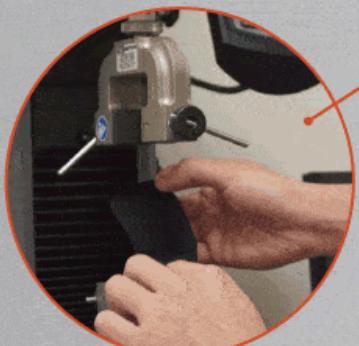
**MOTION SENSE TECHNOLOGY**  
PROVIDING UNPARALLELED SUPPORT




A vial of shear thickening fluid (STF) invented at the University of Delaware



Biomechanical study that included placing 56 markers on sports bras to track movement was critical to developing the technology



A research engineer with STF Technologies LLC, prepares to test the strength of a fabric sample.

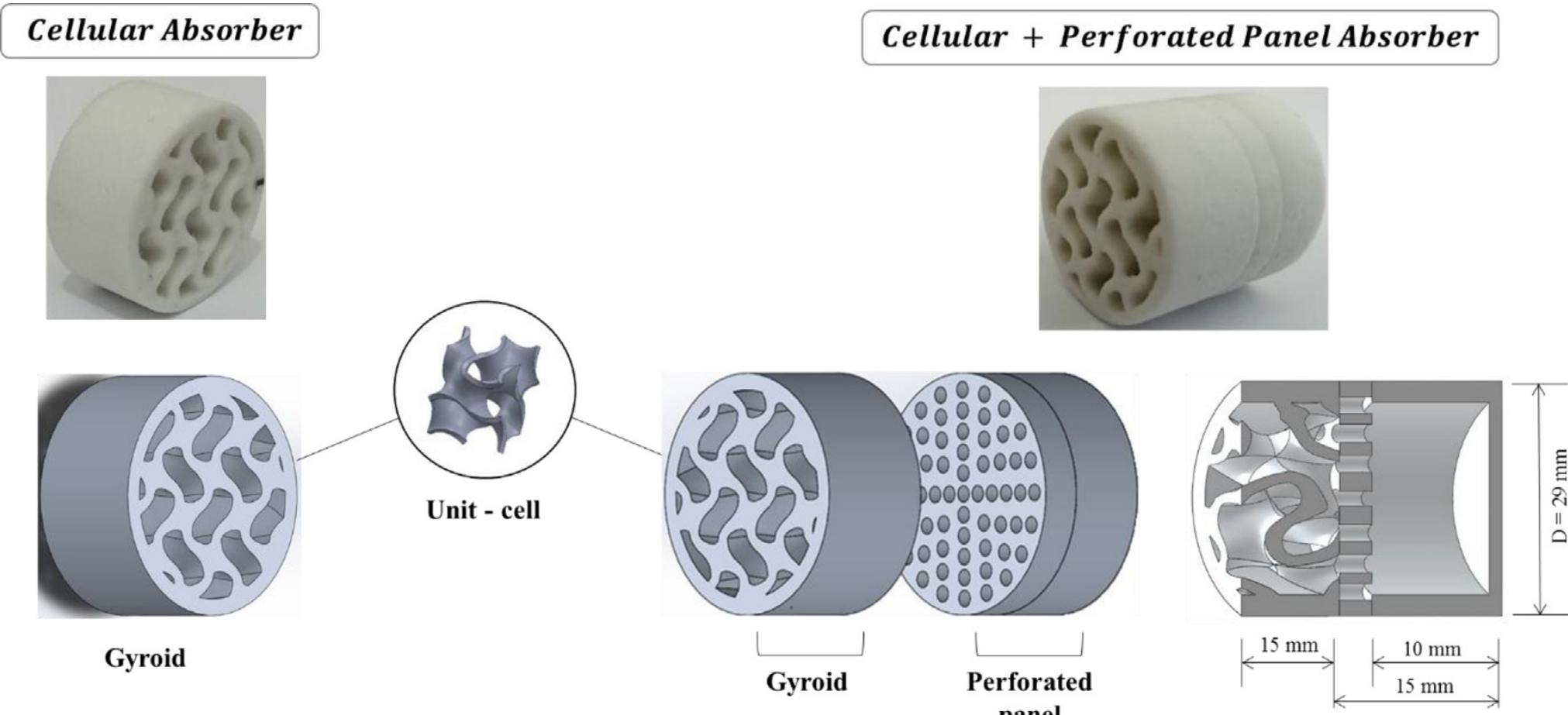
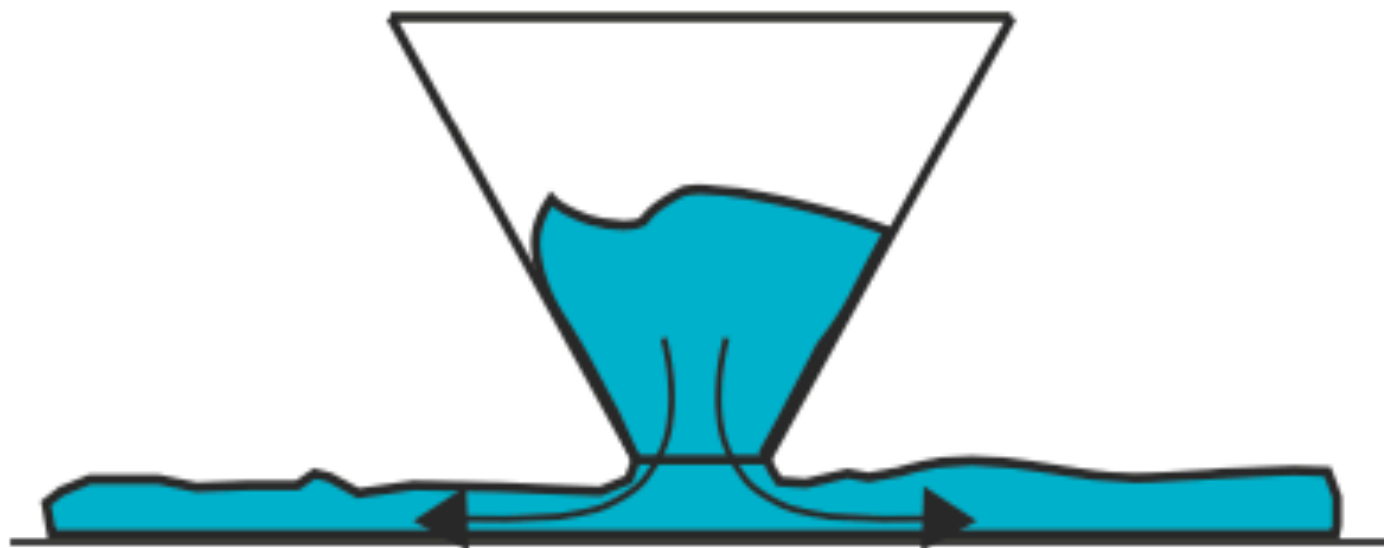


Reebok's PureMove Bra features proprietary Motion Sense Technology fabric able to respond to movement where and when wearers need it, thanks to UD's shear thickening fluid (STF).

1/2 Half of women who exercise experience breast pain.  
—Reebok Study

## Acoustic absorbers

## Modern concrete



# First Appearance in Scientific Journals

**DILATANCY AND ITS RELATION TO THIXOTROPY.**  
 BY H. FREUNDLICH AND H. L. RÖDER.  
*Received 29th November, 1937.*

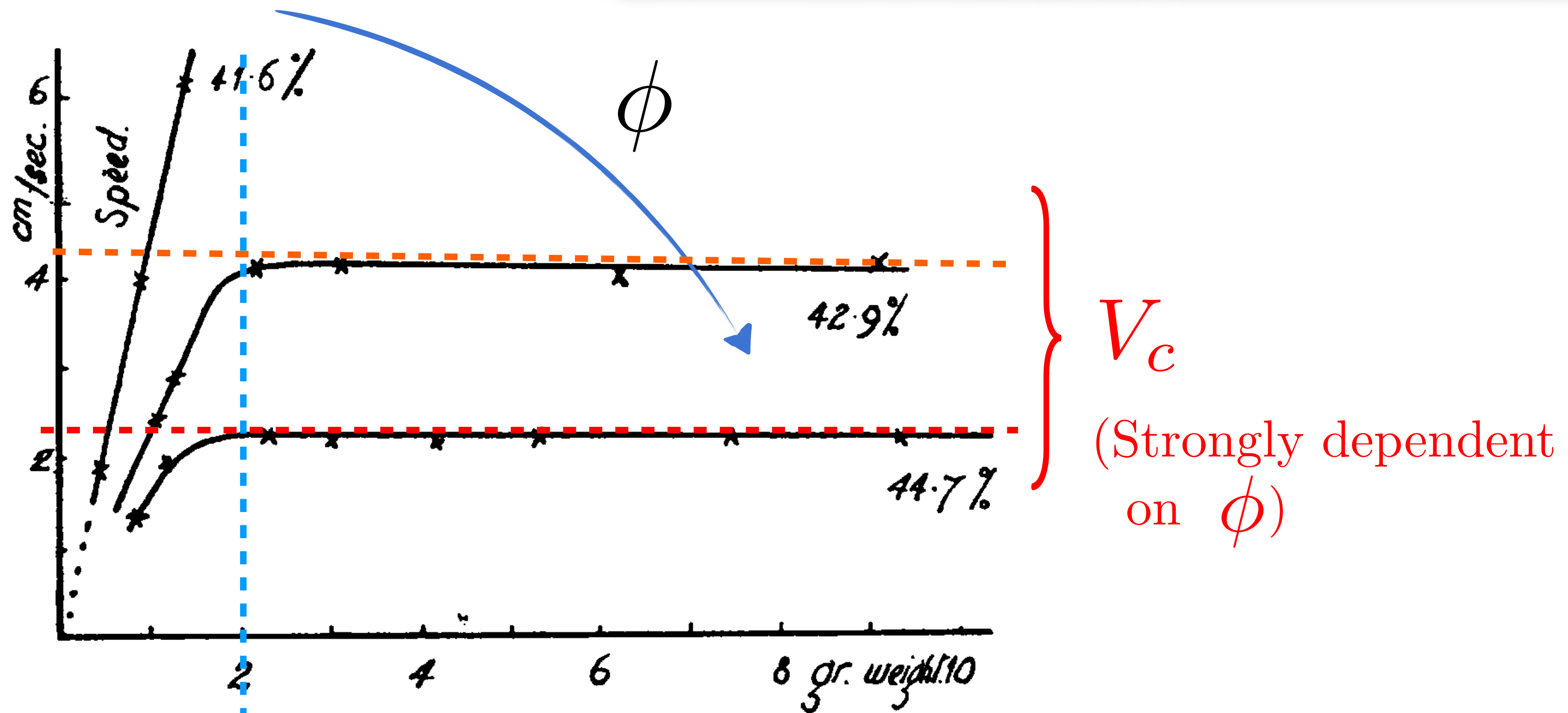
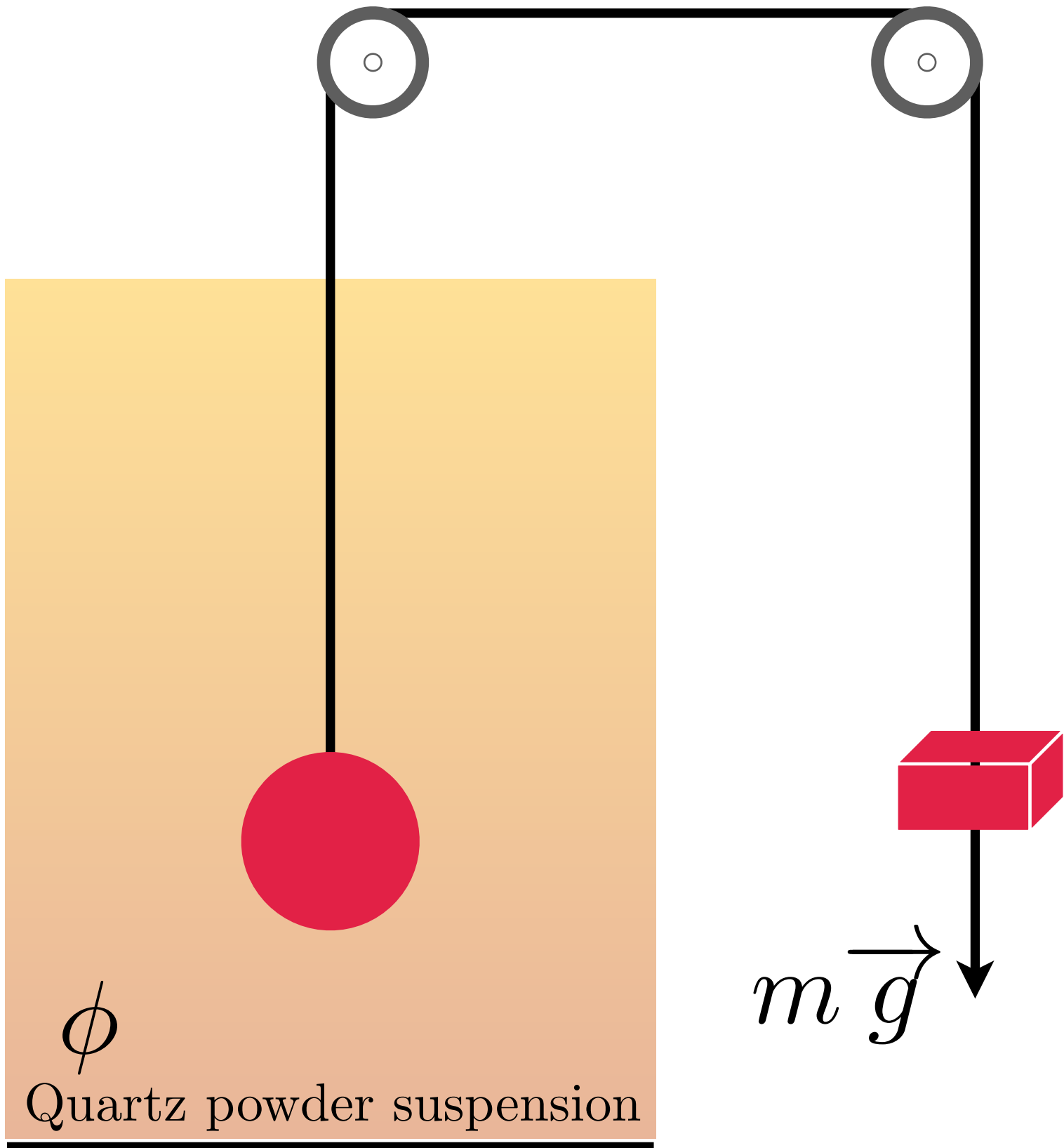
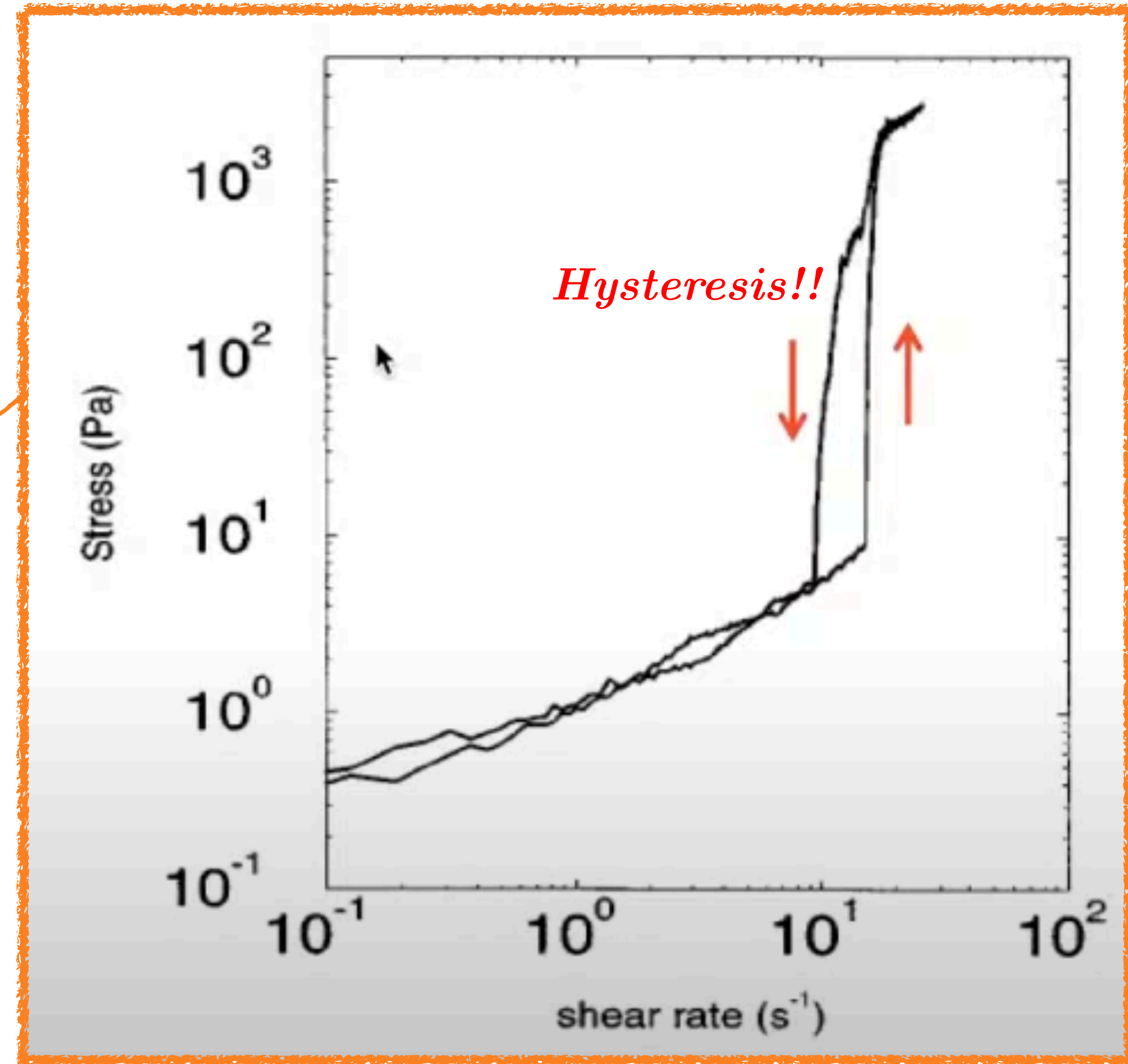
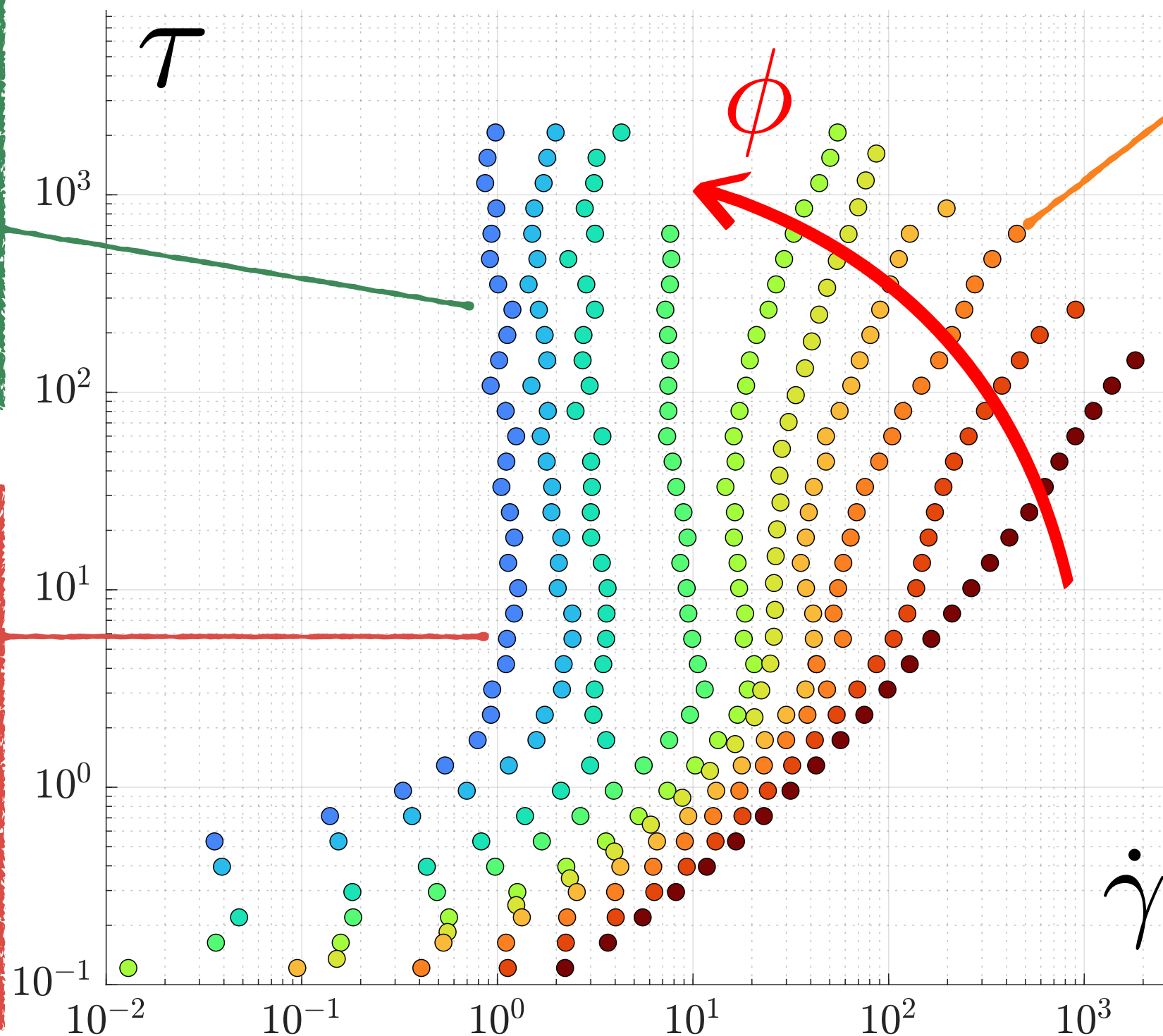
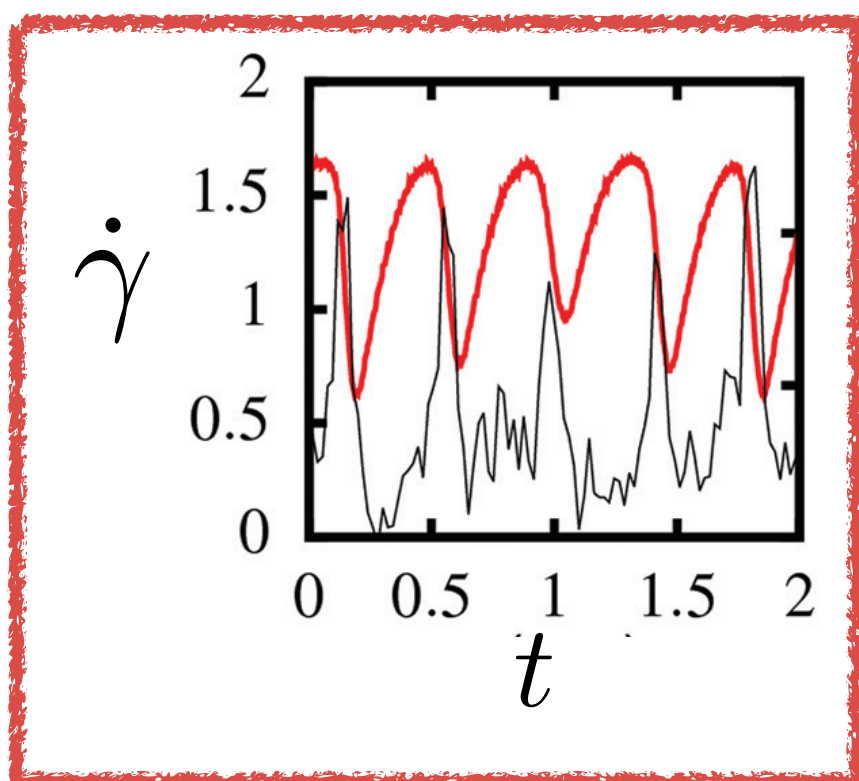
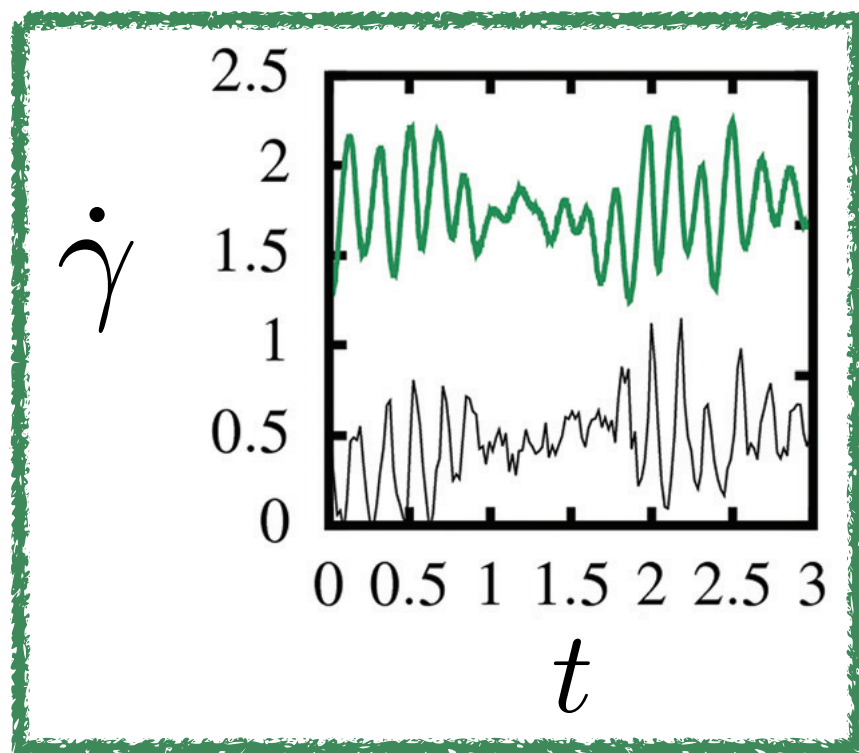
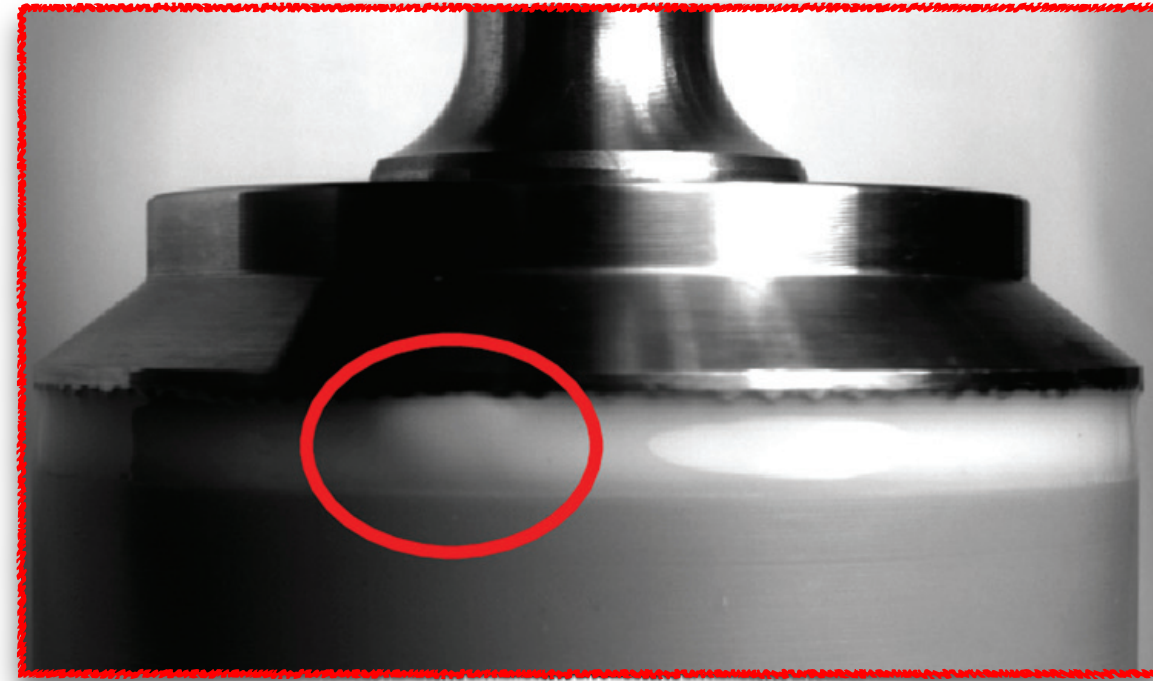
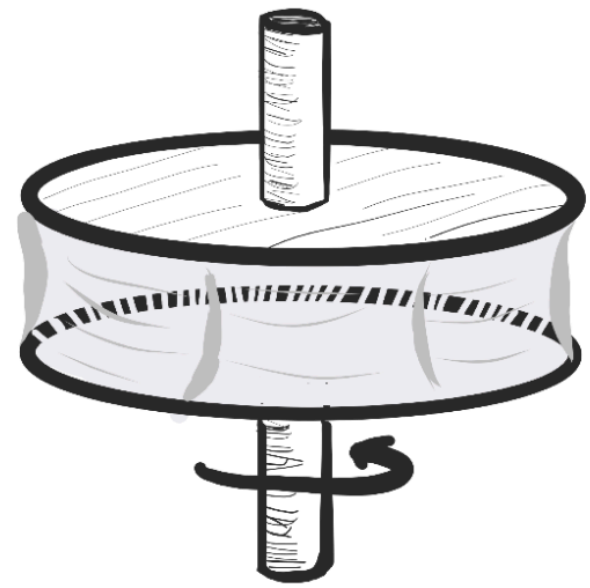


FIG. 2.

$F_c$  ( Very weak dependence on  $\phi$  )



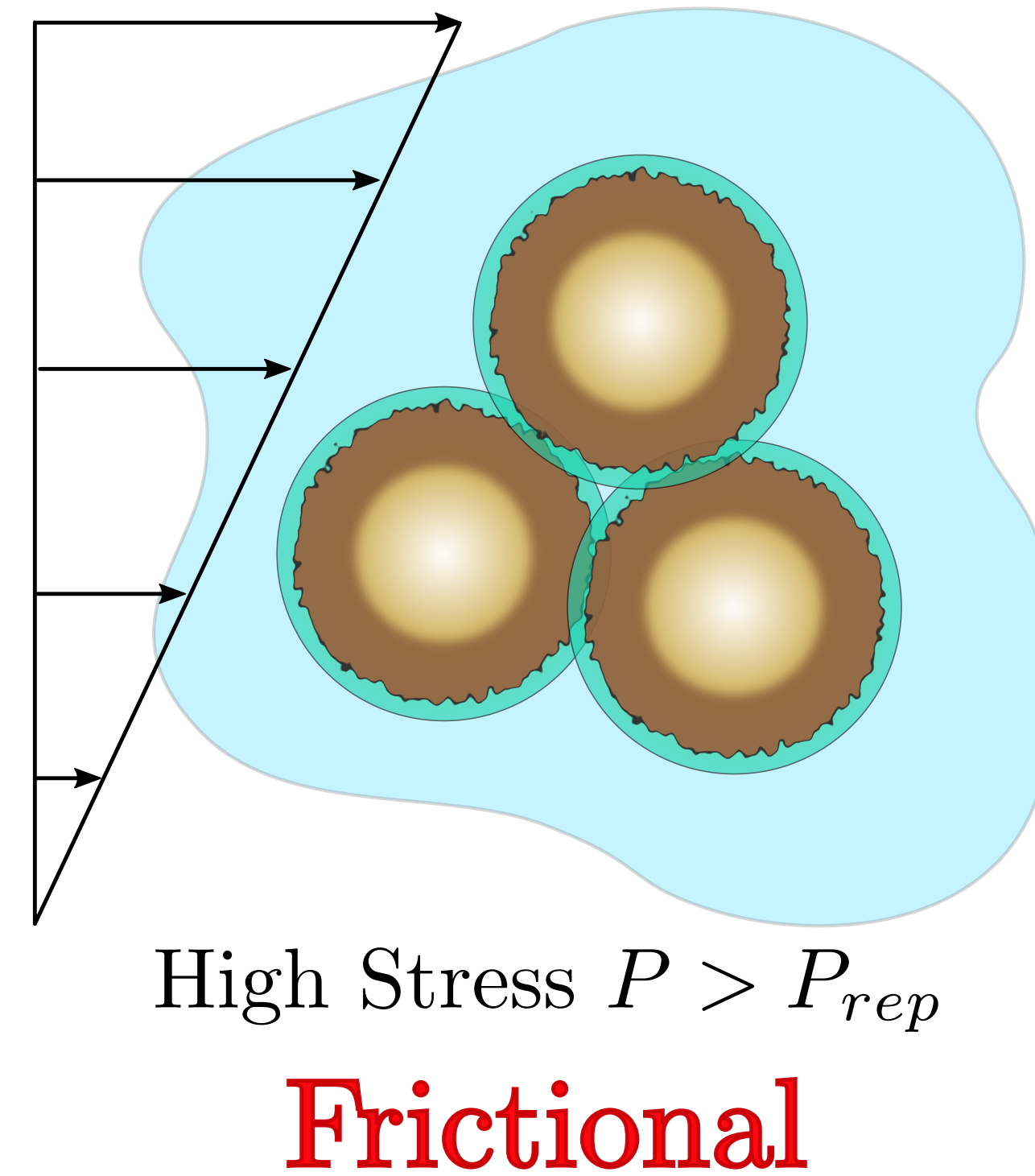
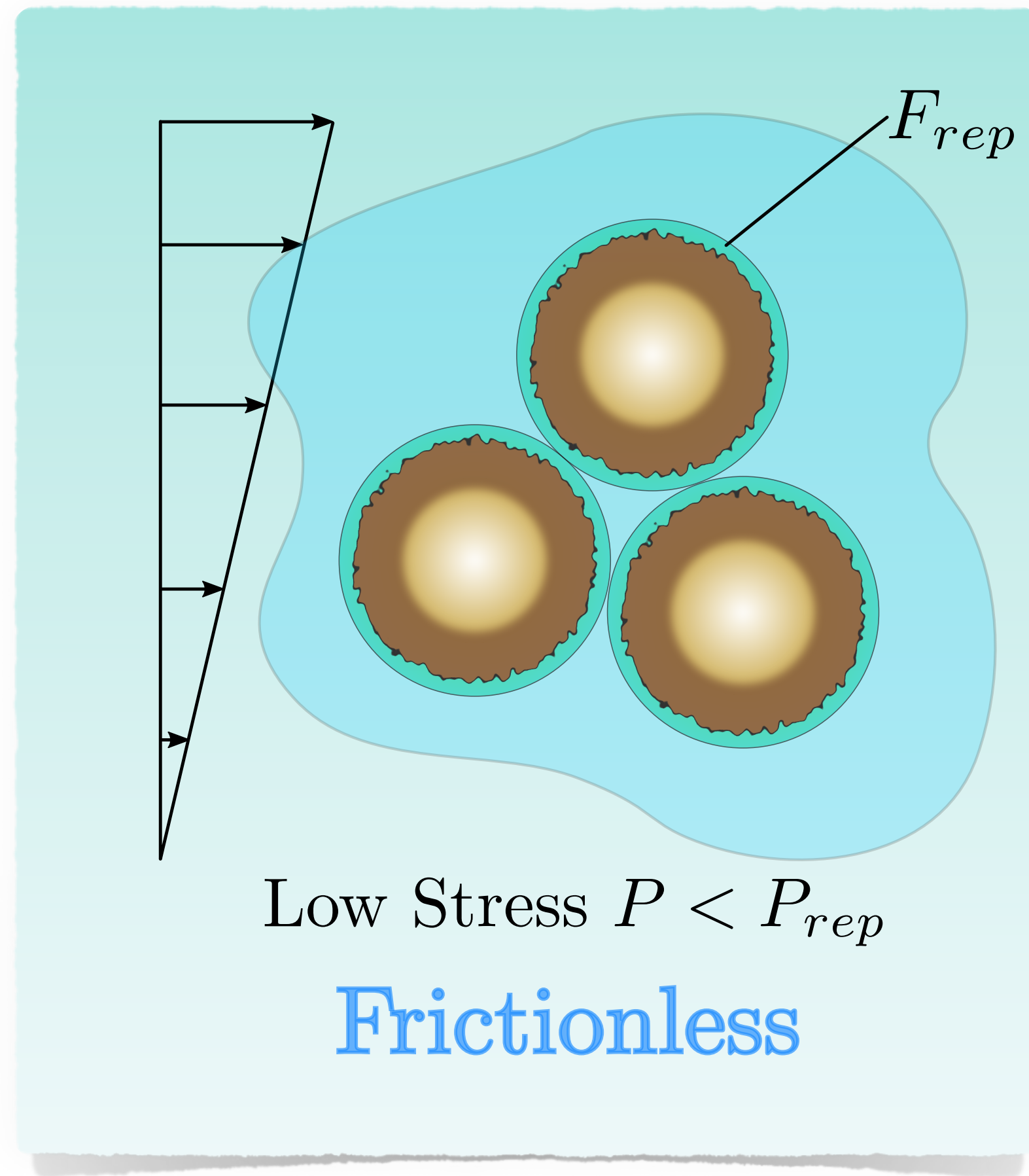
# Experimental Observations: Volume—imposed Rheology



# Origin of Shear Thickening ?

Key Idea: A short-range repulsive force between the grains (Seto *et al.* PRL 2013)

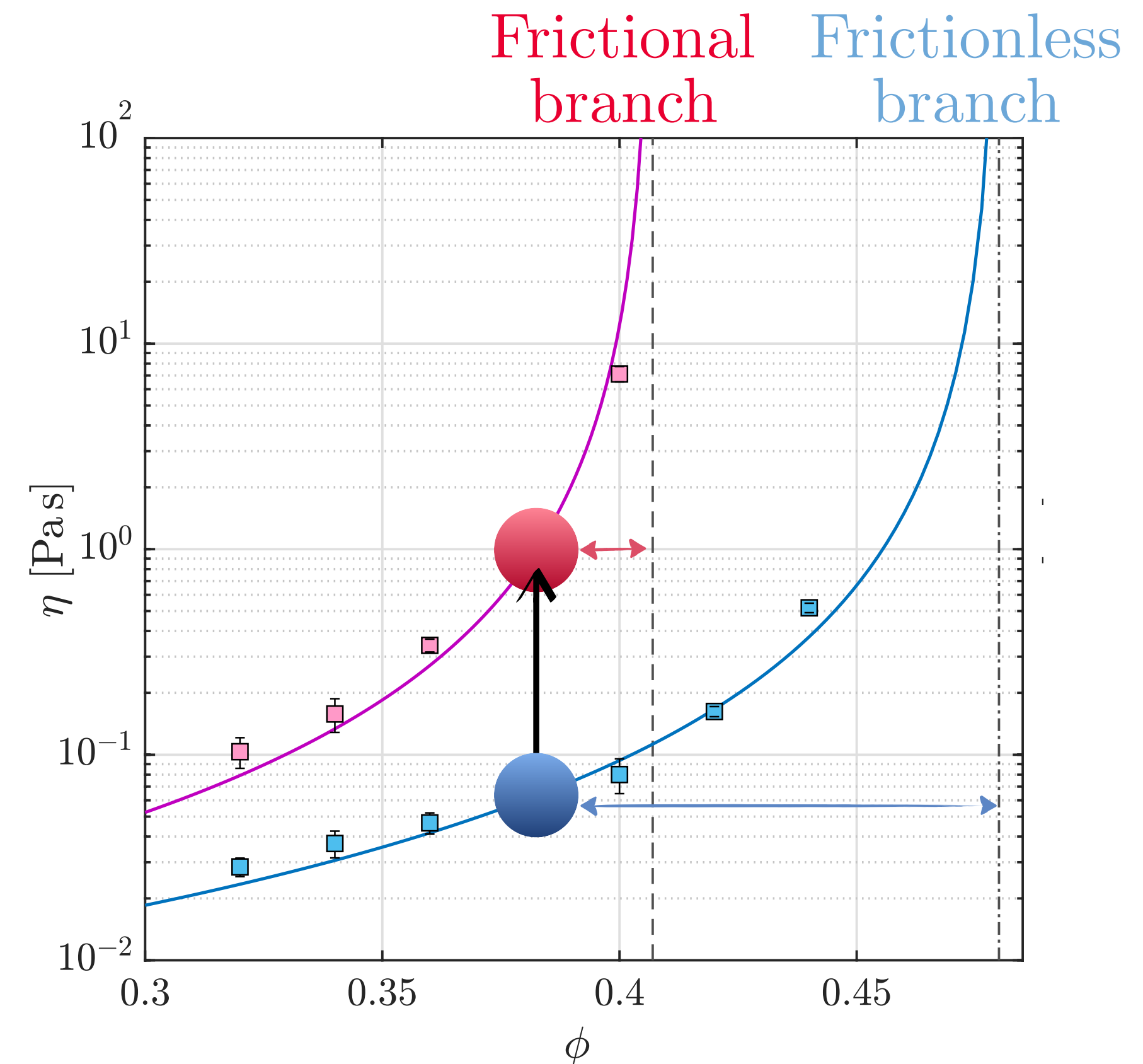
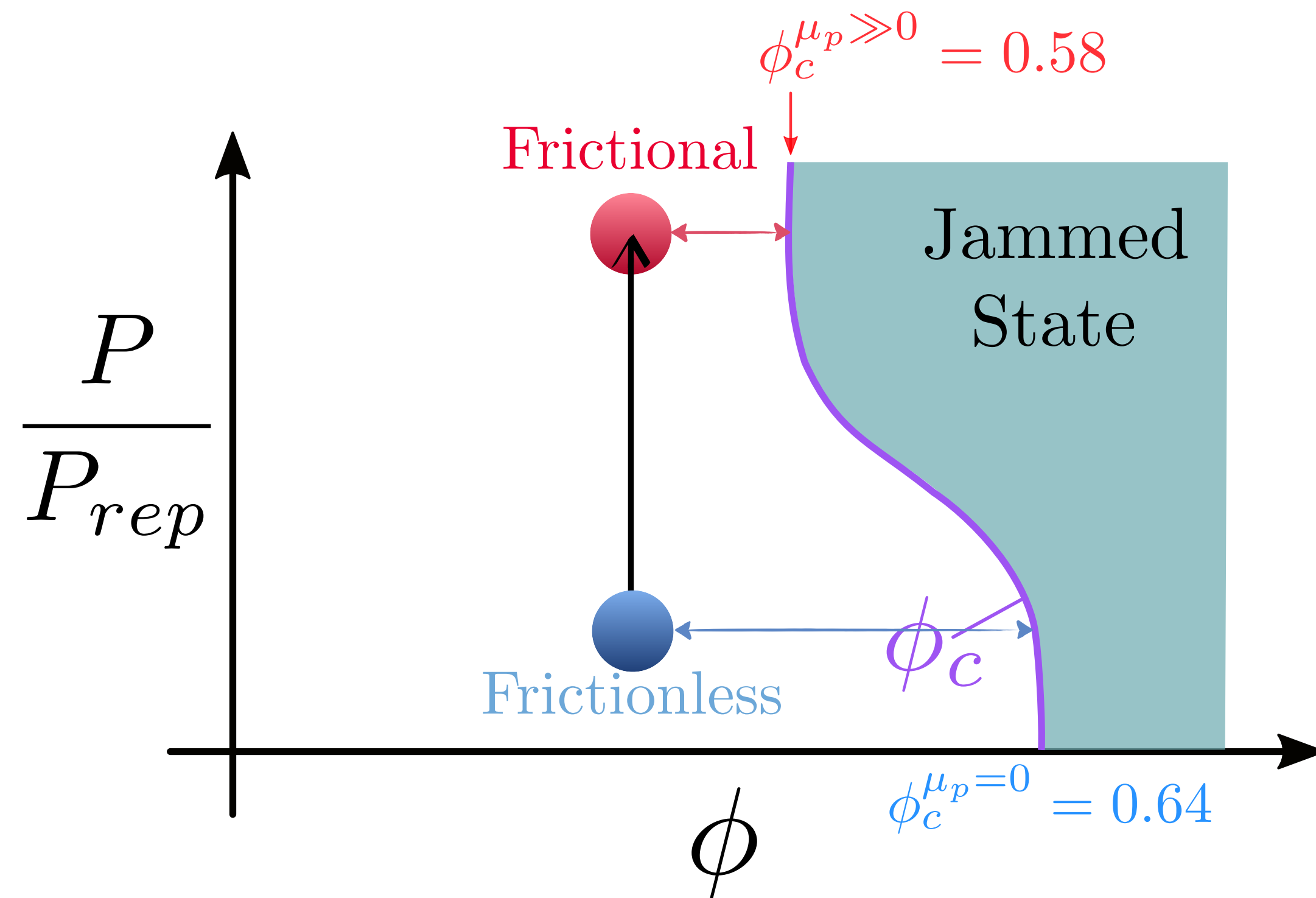
$$P_{rep} \sim \frac{F_{rep}}{d^2}$$



→ “Activates” a **FRictionLESS** state at low stress!

# Why is this so dramatic?

- \* The critical volume fraction  $\phi_c$  is a function of the interparticle friction  $\mu_p$ !



- When the confining pressure increases the system gets closer to the jamming point!
- Introduces a STRESS scale to the problem!

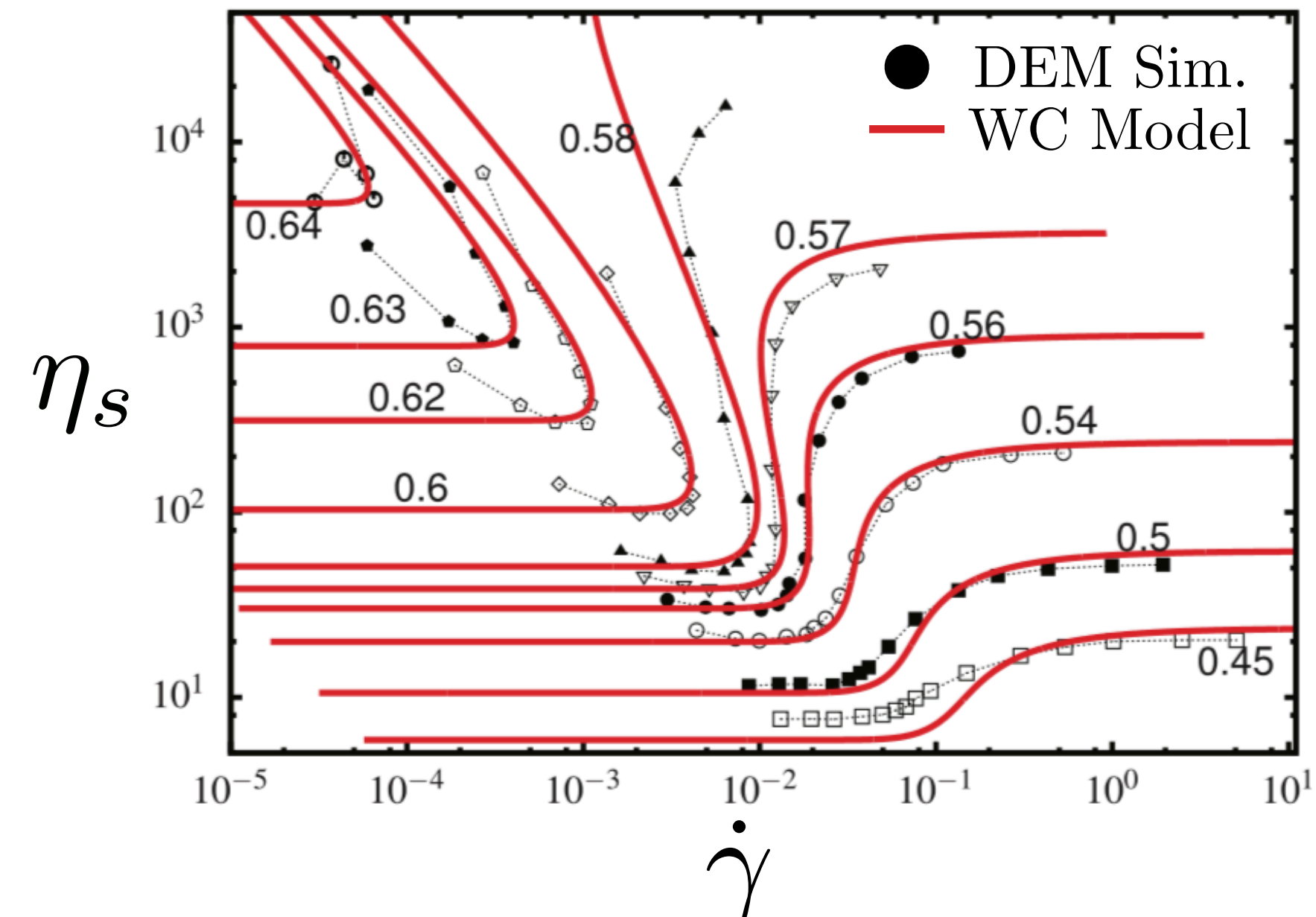
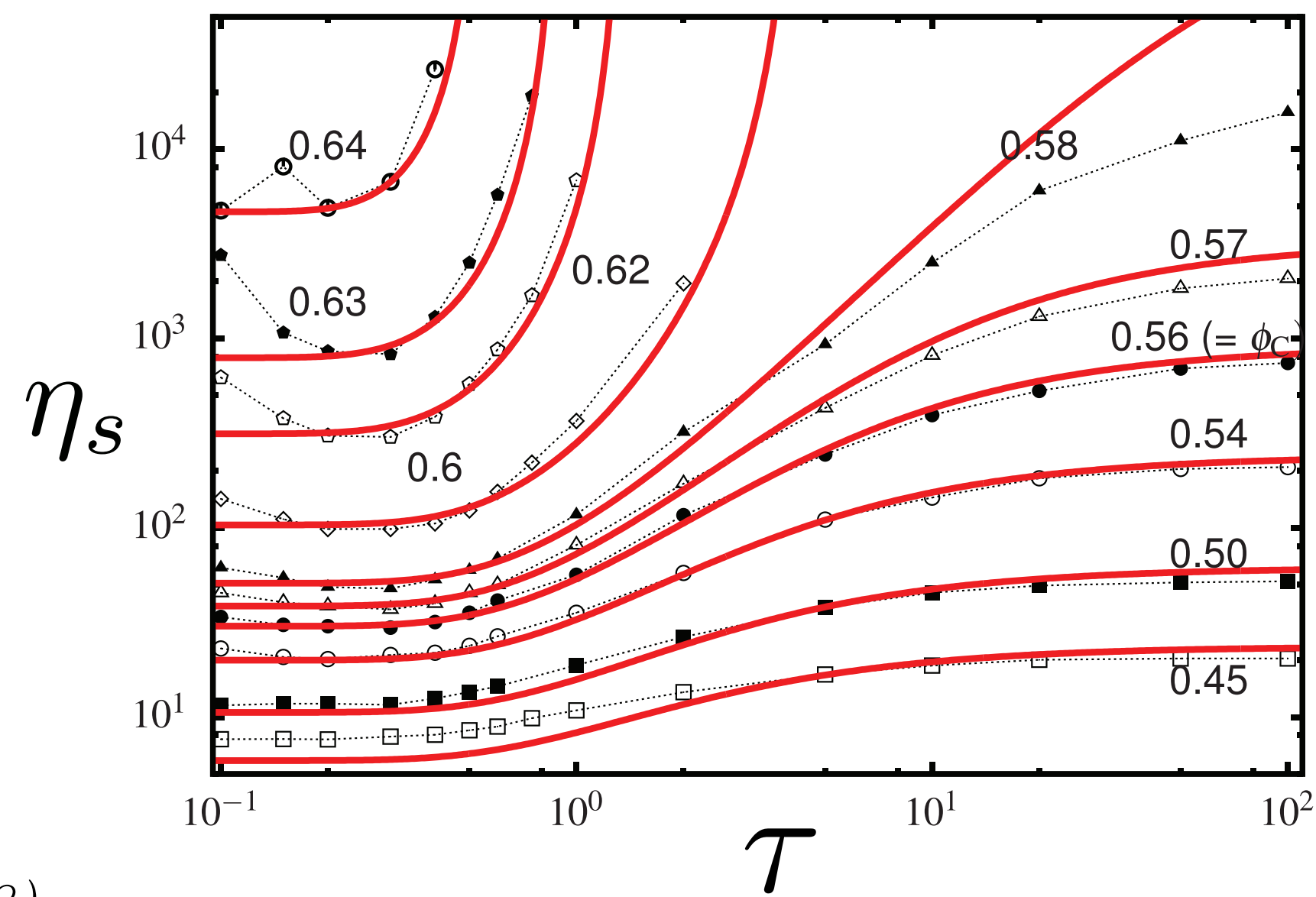
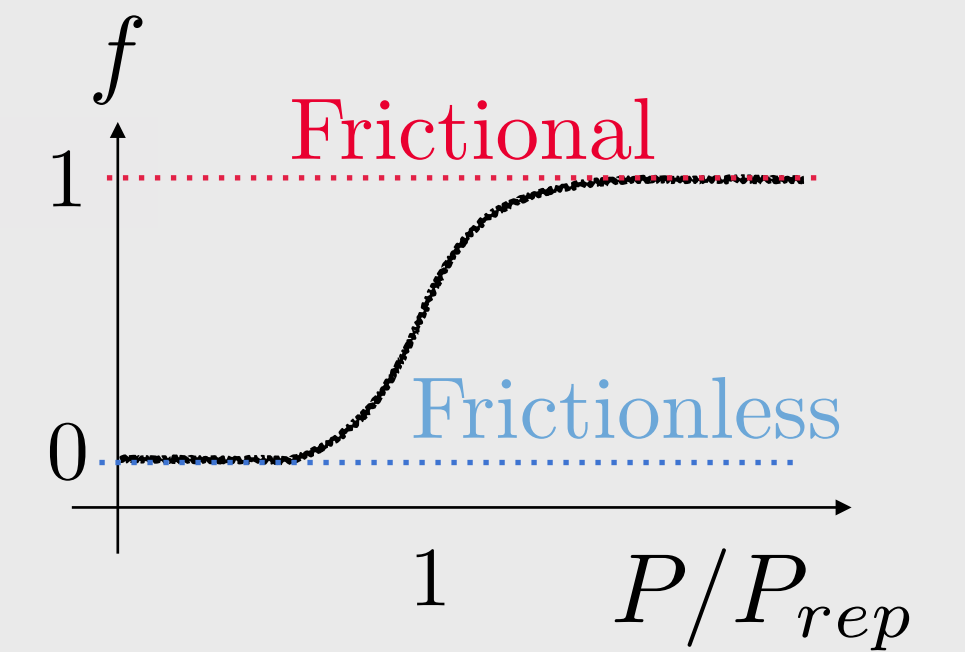
# Frictional Transition Model:

(Wyart & Cates PRL 2014)

$$\frac{\eta_s}{\eta_f} = \left[ \phi_c - \phi \right]^{-2} \quad \& \quad \phi_c \left( \frac{P}{P_{rep}} \right) = \phi_c^{\mu > 0} f + (1 - f) \phi_c^{\mu = 0}$$

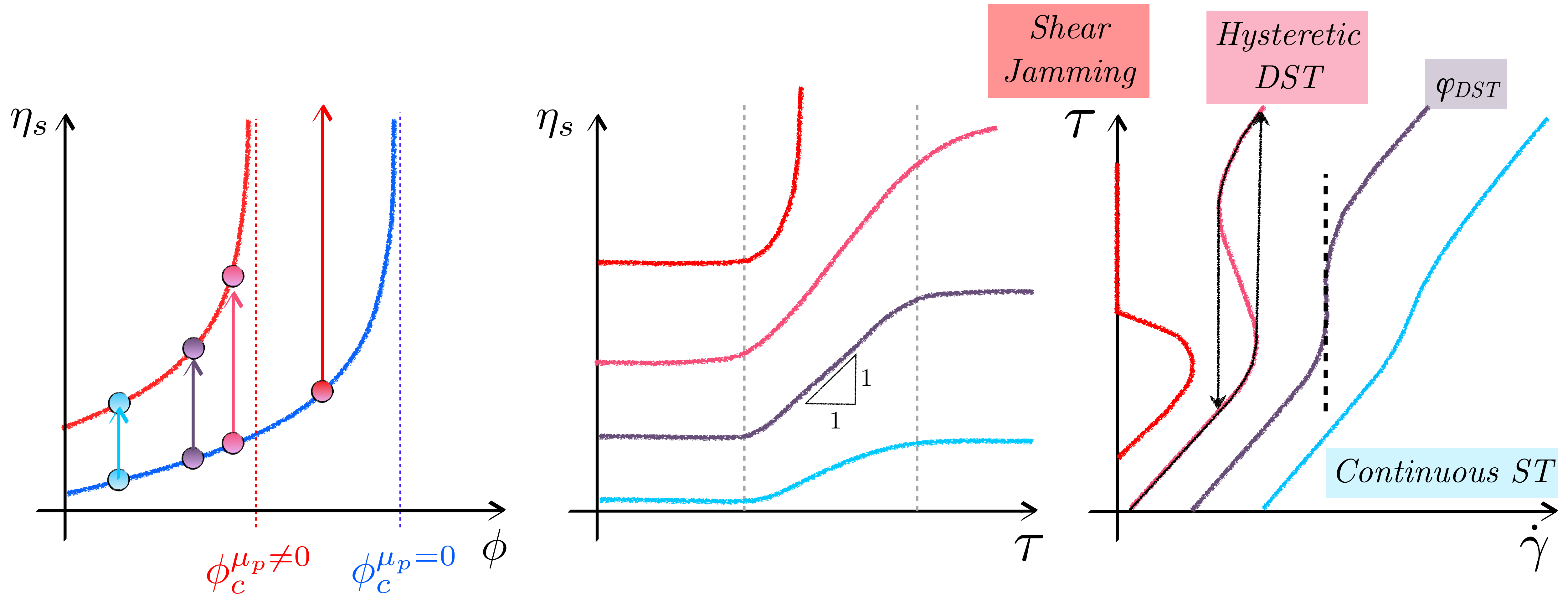
Order Parameter:

*Fraction of frictional contacts*  $\rightarrow$   $f = 0 \rightarrow$  Frictionless when  $P < P_{rep}$   
 $f = 1 \rightarrow$  Frictional when  $P > P_{rep}$



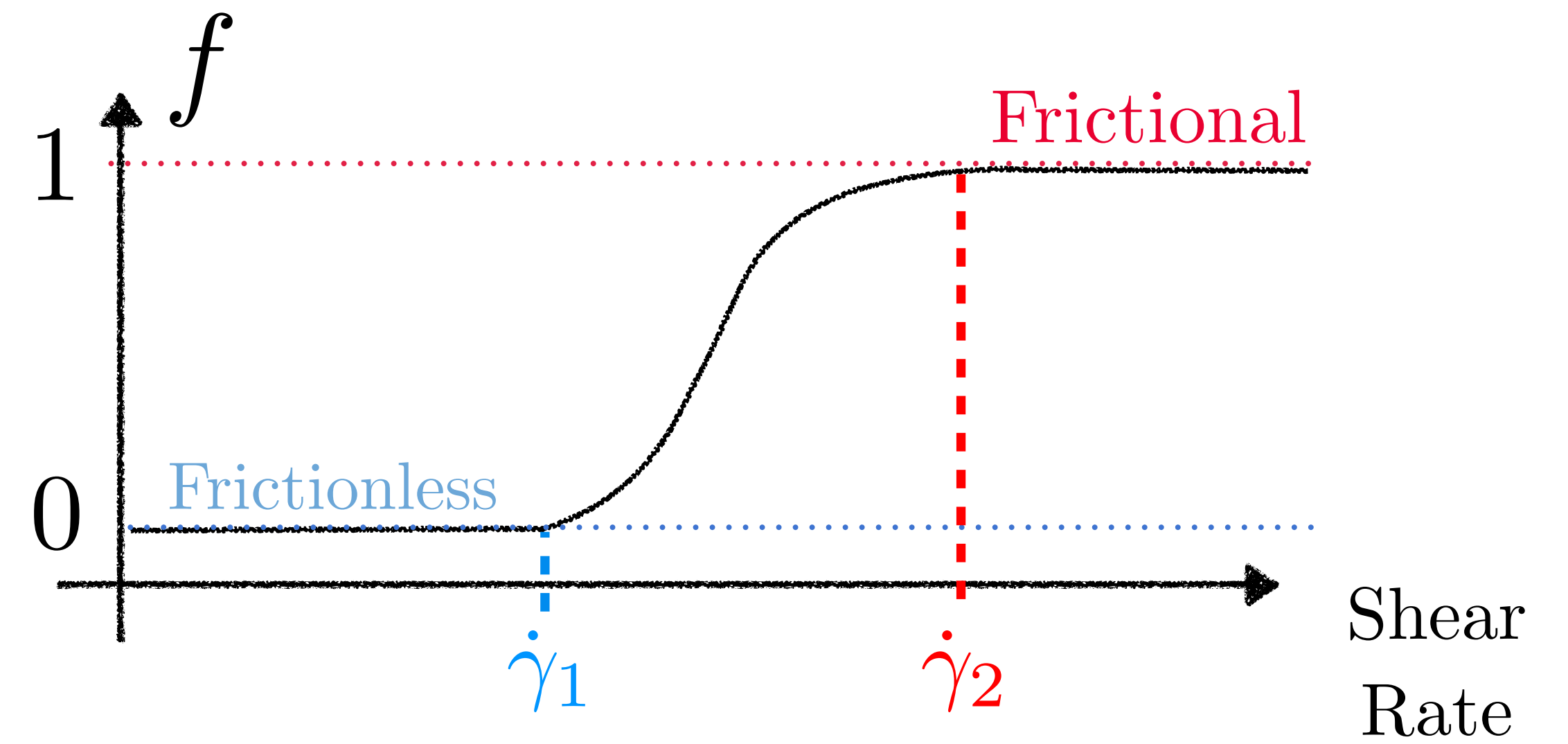
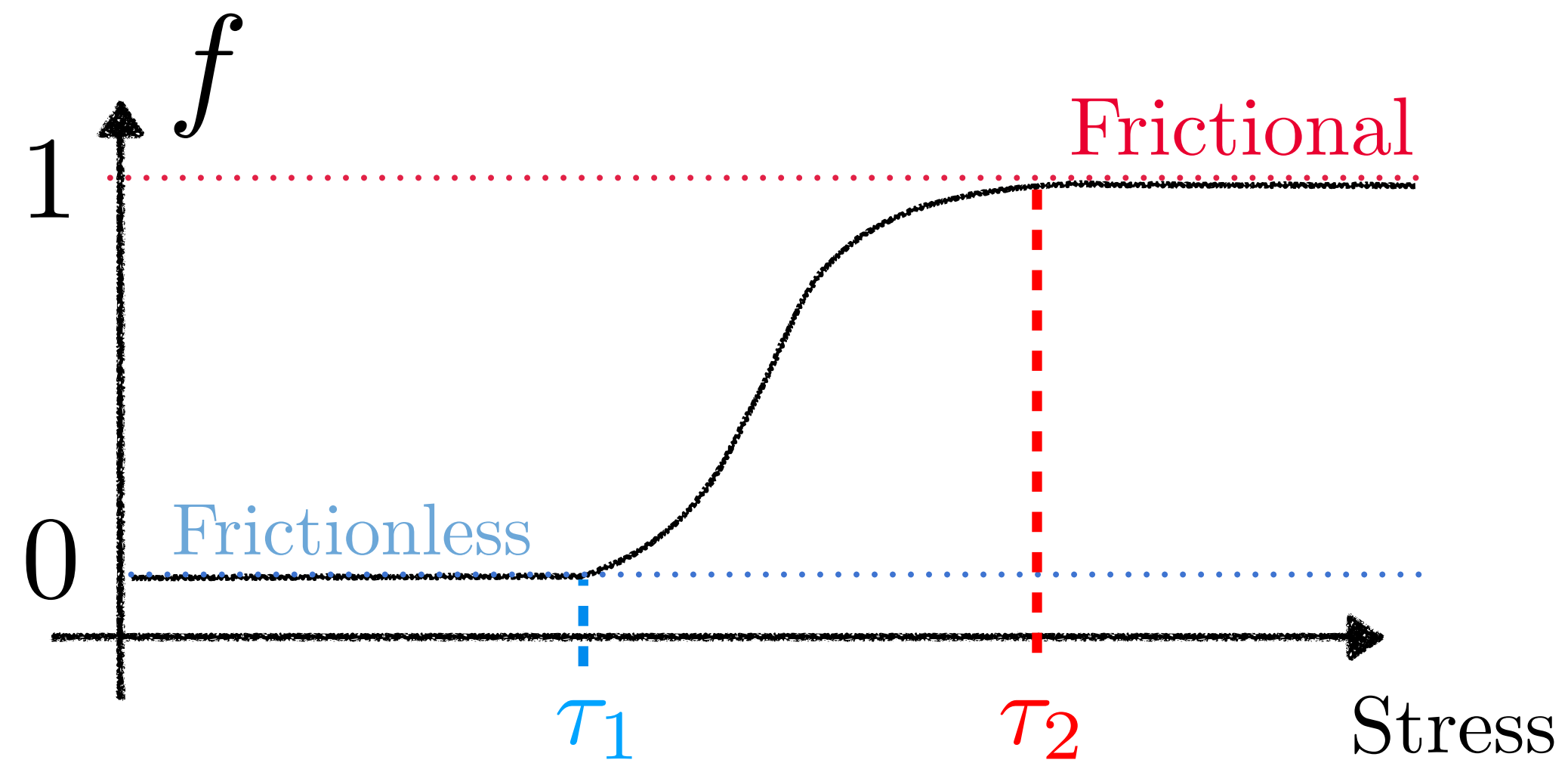
(Singh et al JoR 2018)

# Frictional Transition Model

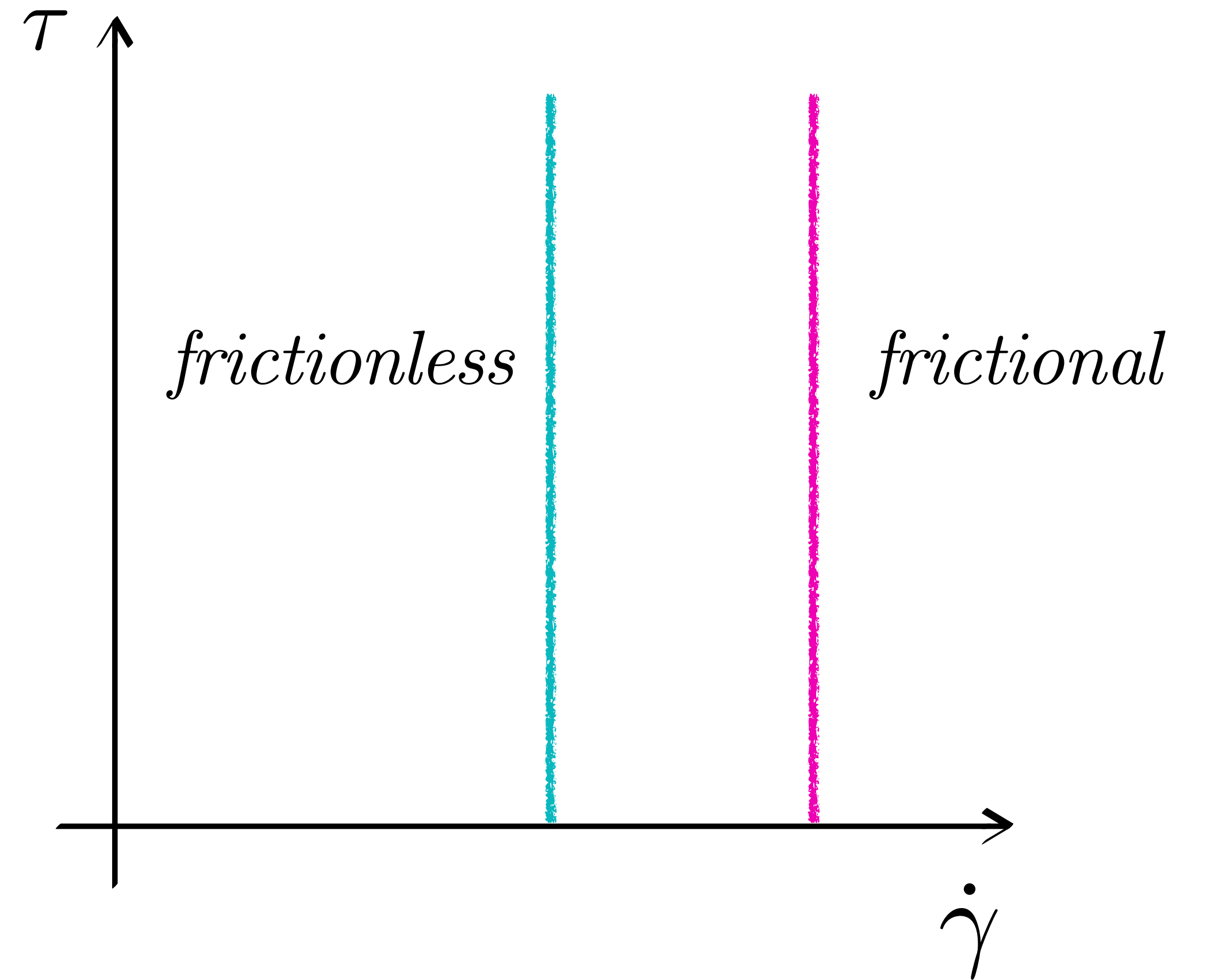
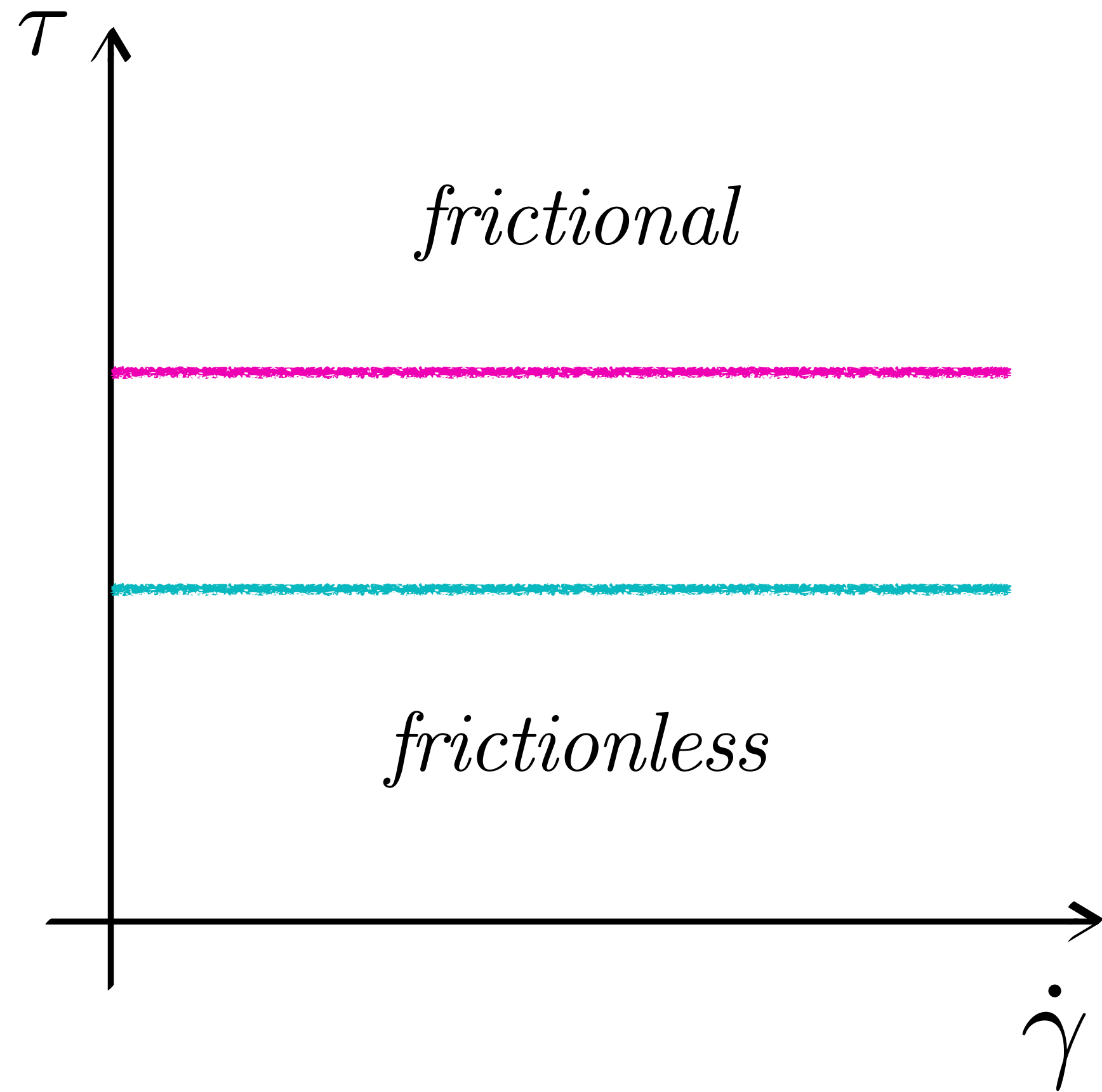


# Frictional Transition Model

Does it give similar results?



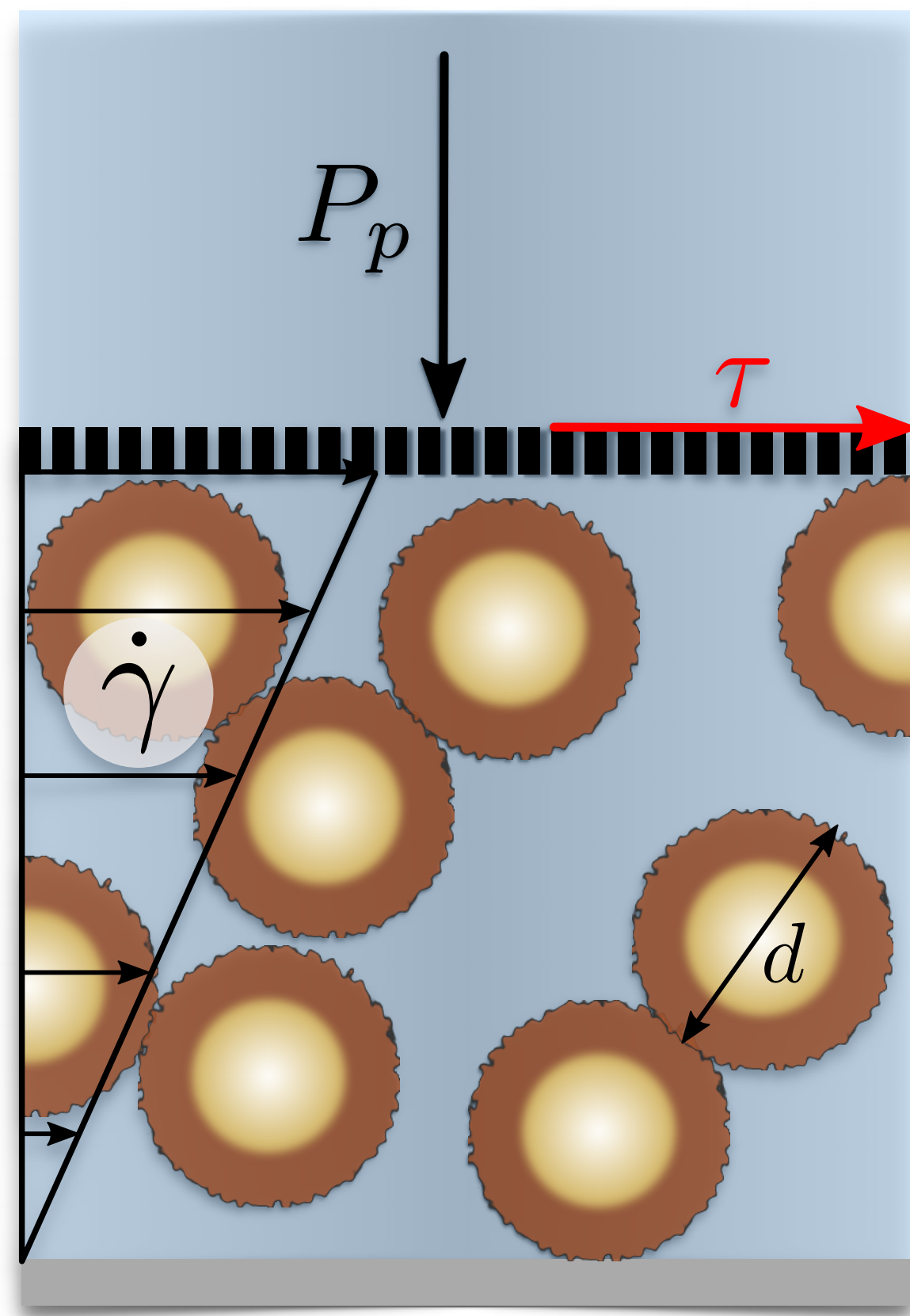
# Frictional Transition Model



Experimental Evidence of the Frictional Transition?

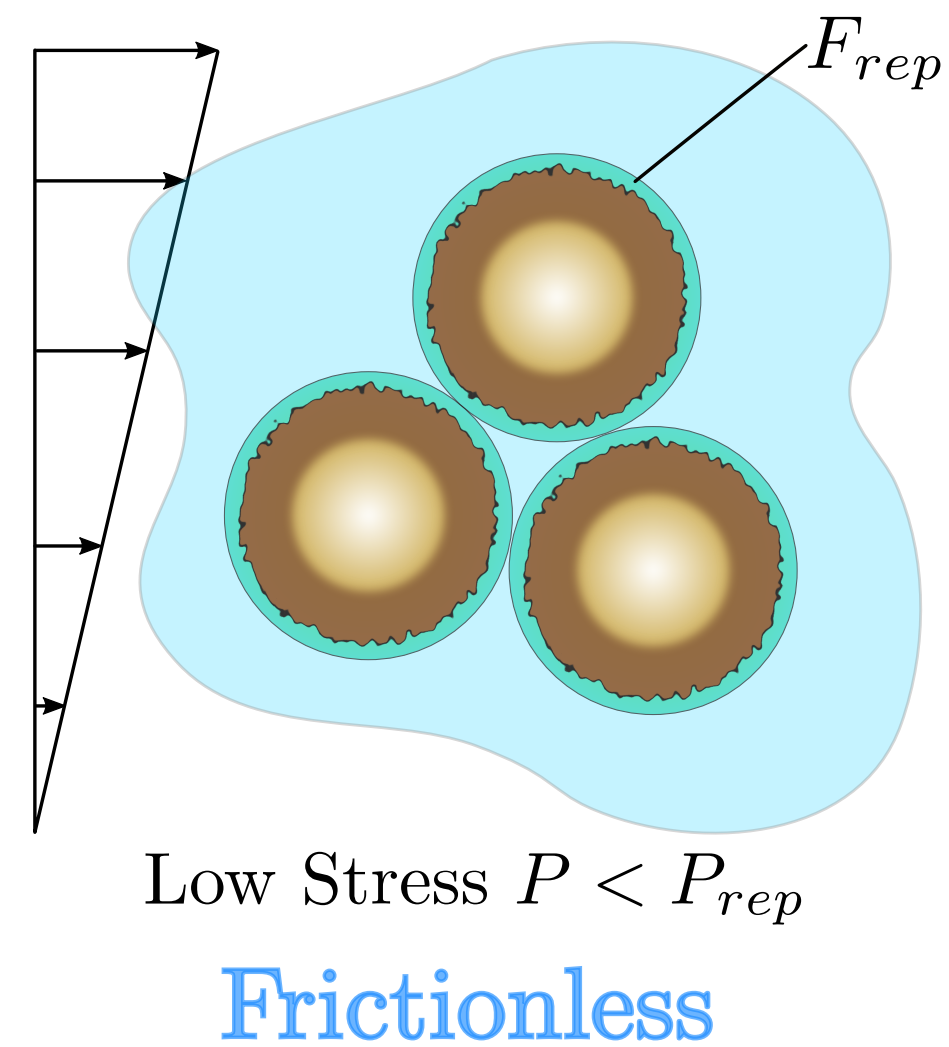
# Experimental Evidence of the Frictional Transition?

## Pressure-imposed Rheology

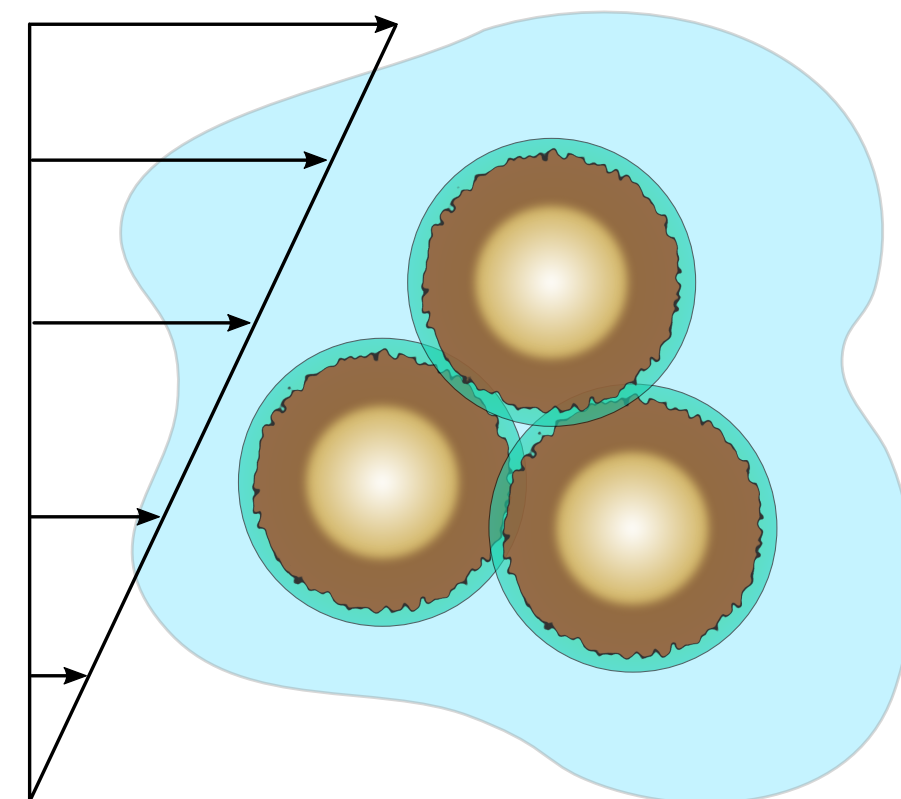


$$\mu = \frac{\tau}{P_p}$$

## Frictional Transition:



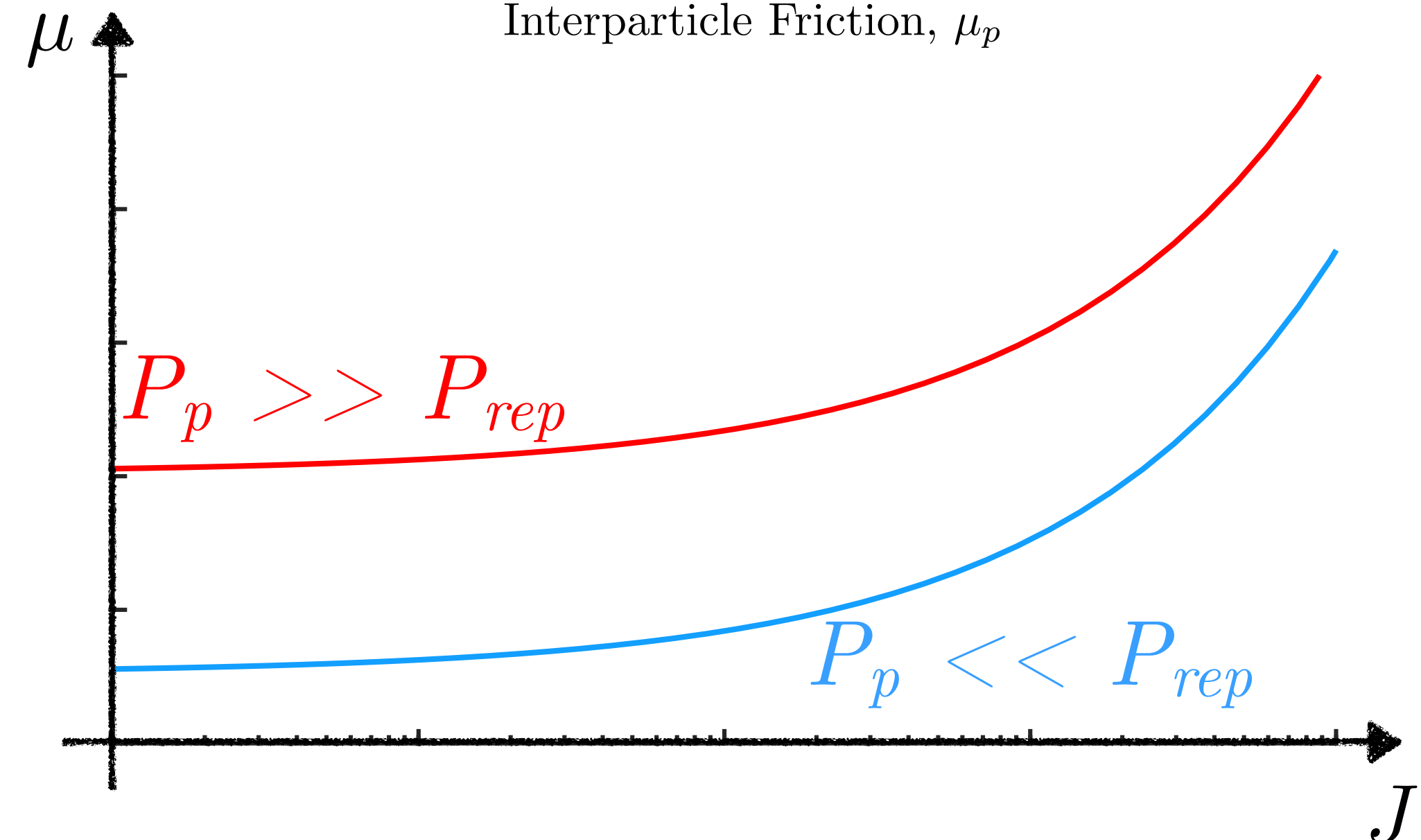
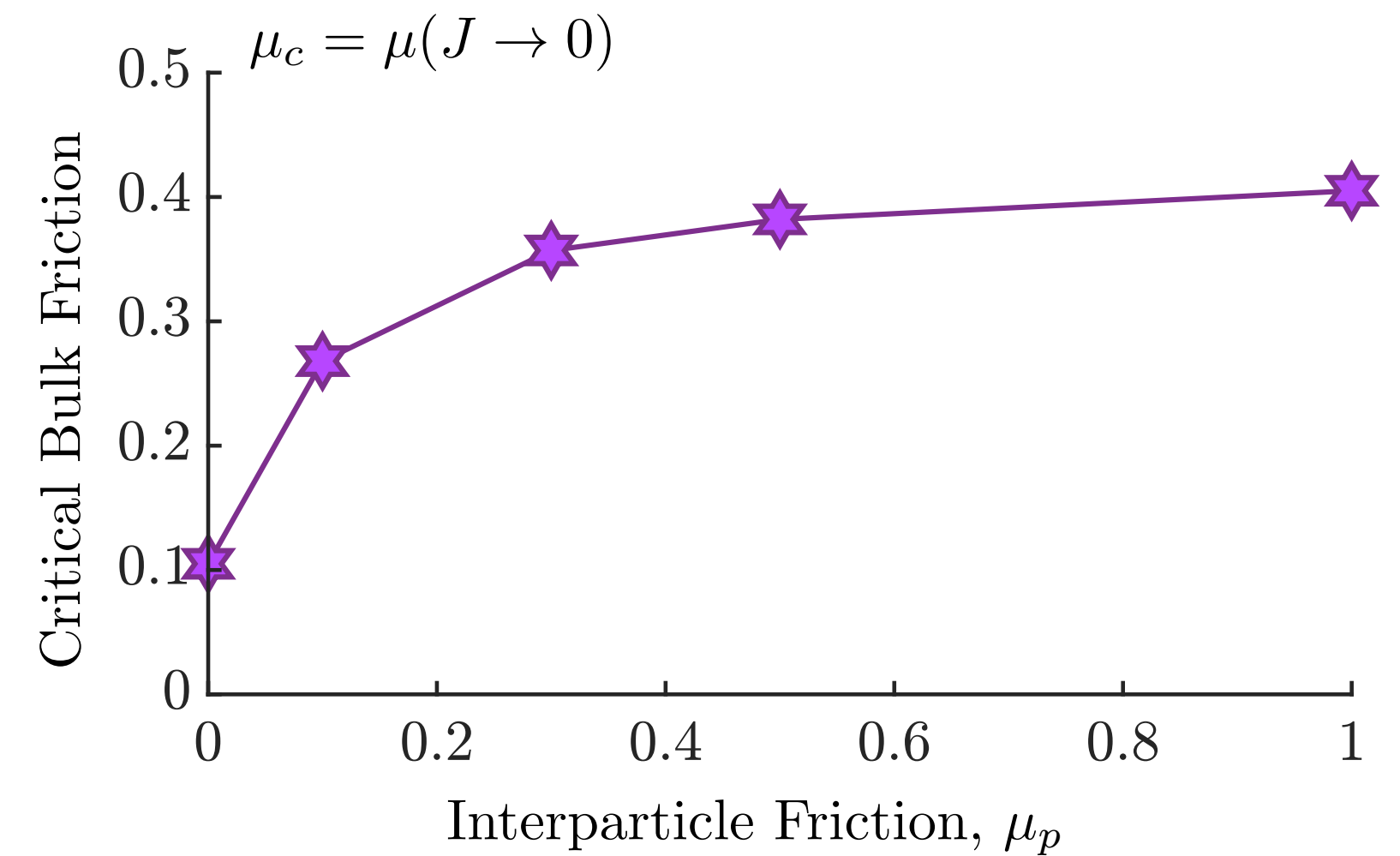
Low Stress  $P < P_{rep}$



High Stress  $P > P_{rep}$

**Frictional**

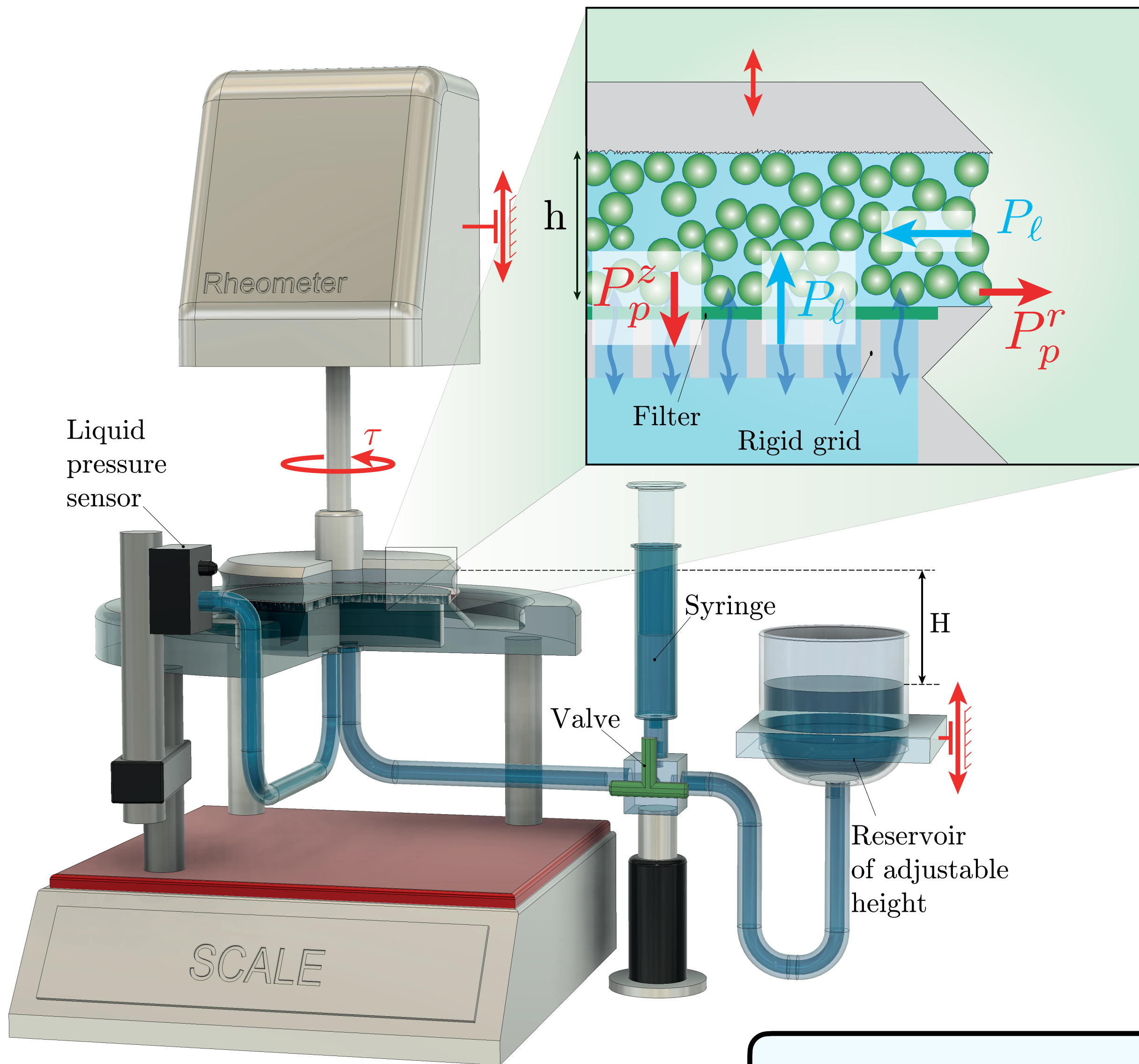
## What do we expect?





# The Capillarytron

*Etcheverry, Forterre & Metzger PRX (2022)*



Imposed liquid pressure:  $P_\ell = -\rho g H$

Radial force balance:  $P_p^r = -P_\ell$

Capillary interface controls  $P_p$

Vertical force balance:  $mg = (P_p^z + P_\ell)\pi R^2$

Standard rheology:

$$\eta_s(\phi) = \frac{\tau}{\eta_f \dot{\gamma}} \quad \eta_n(\phi) = \frac{P_p^z}{\eta_f \dot{\gamma}}$$

Frictional rheology:

$$\mu(J) = \frac{\tau}{P_p^z} \quad \phi = \phi(J) \quad J = \frac{\eta_f \dot{\gamma}}{P_p^z}$$

Able to perform both  $P_p$ -imposed or  $\phi$ -imposed measurements!

# A Model Shear-thickening Suspension

*Clavaud et al. PNAS (2017)*

*Perrin et al. PRX (2019)*

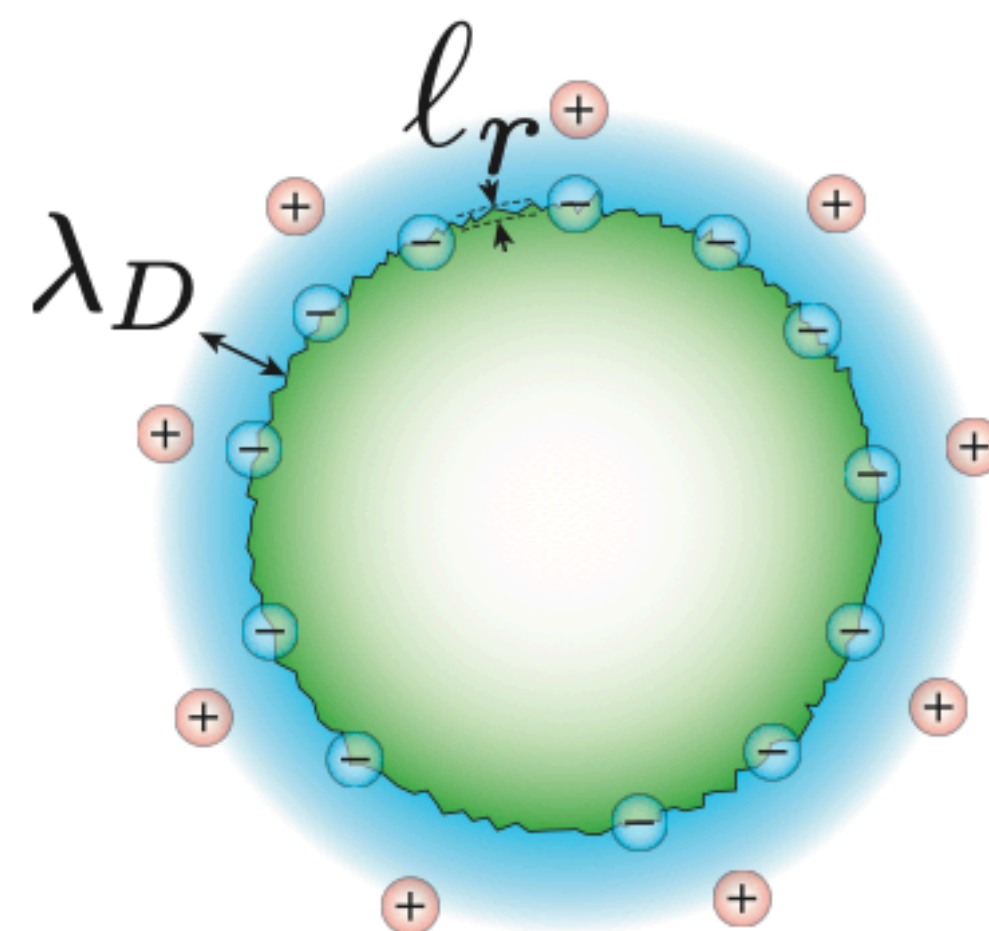
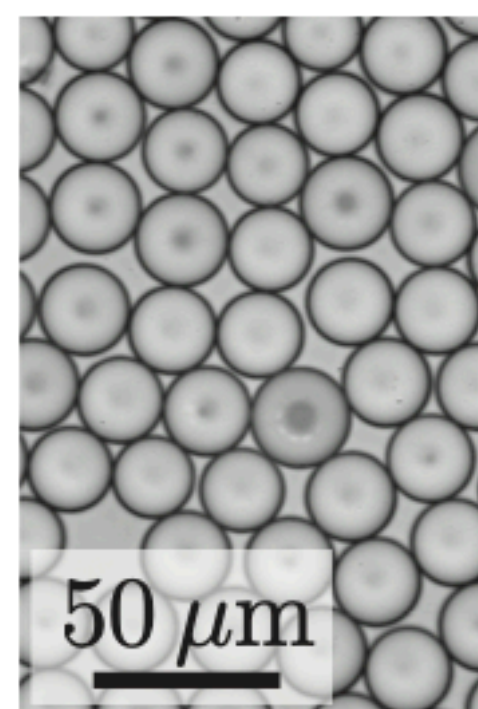
*Perrin et al. PRL (2021)*

*Etcheverry, Forterre & Metzger PRX (2023)*

Silica spheres

$$d = 25 \mu\text{m}$$

Water + NaCl



Repulsive pressure:

$$P^* = \frac{F_0 e^{-r/\lambda_D}}{d^2} \quad (\sim 50 \text{ Pa in pure water})$$

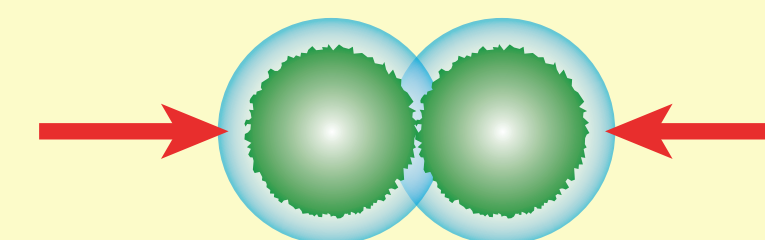
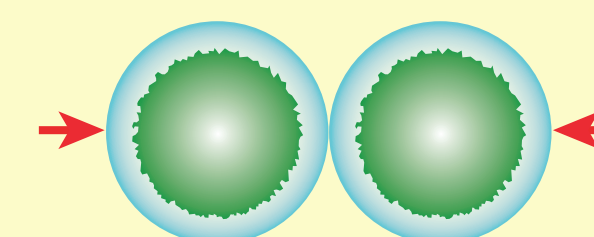
Debye length:

$$\lambda_d = \frac{0.304}{\sqrt{[NaCl]}} \quad (\text{nm})$$

## Frictional transition model:

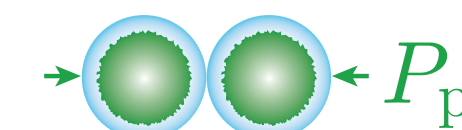
*(Seto et al. PRL 2013, Mari et al. JoR 2014, Wyart & Cates PRL 2014)*

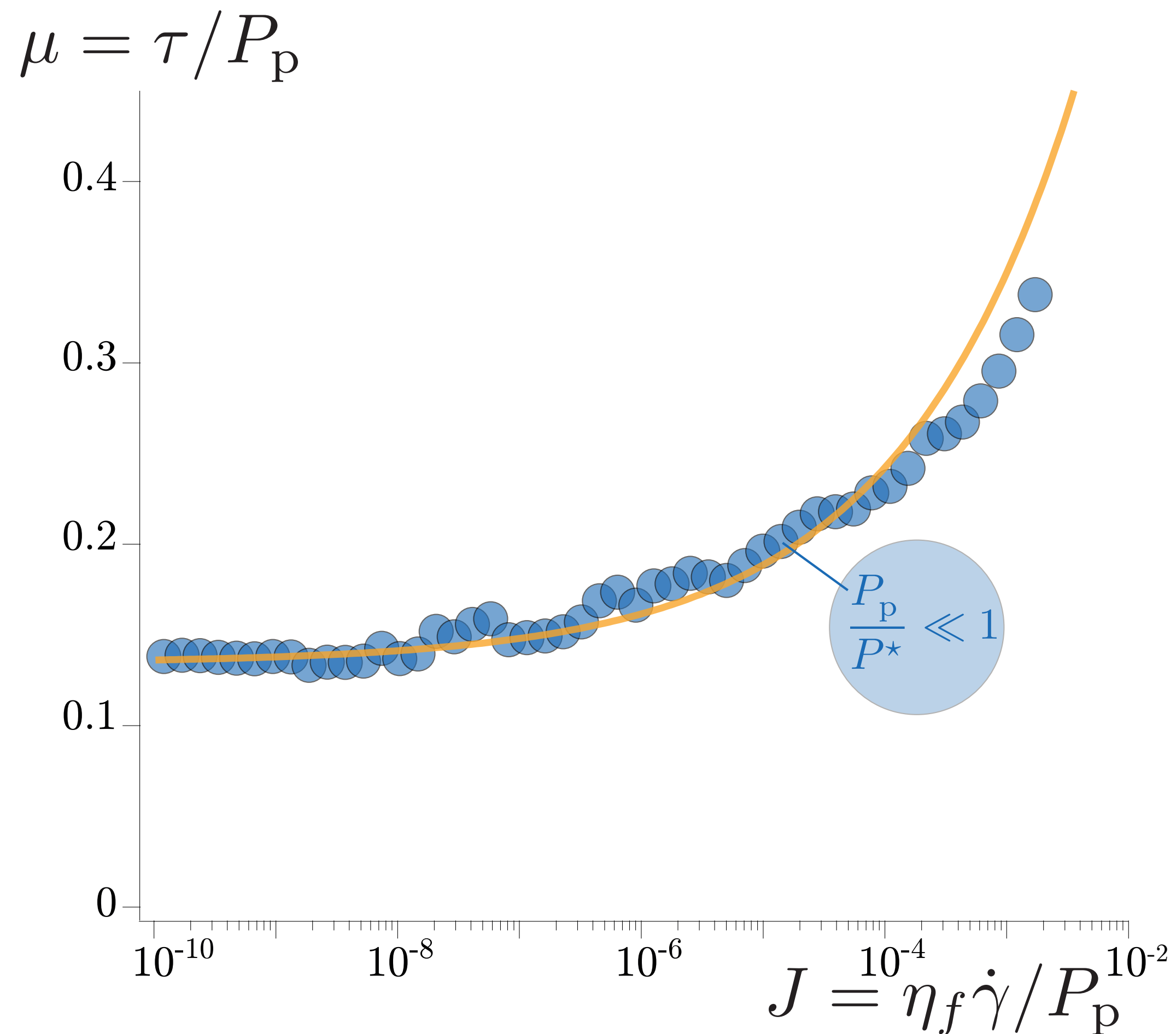
$$J = \frac{\eta \dot{\gamma}}{P_p} \quad \frac{P_p}{P^*}$$

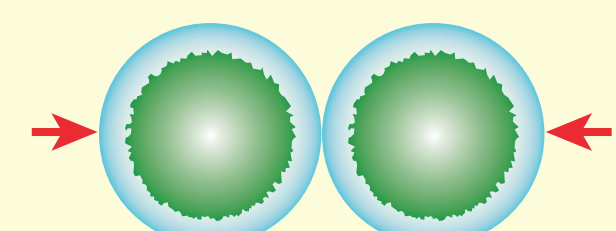


# Probing the Frictional Transition

*Etcheverry, Forterre & Metzger PRX (2022)*

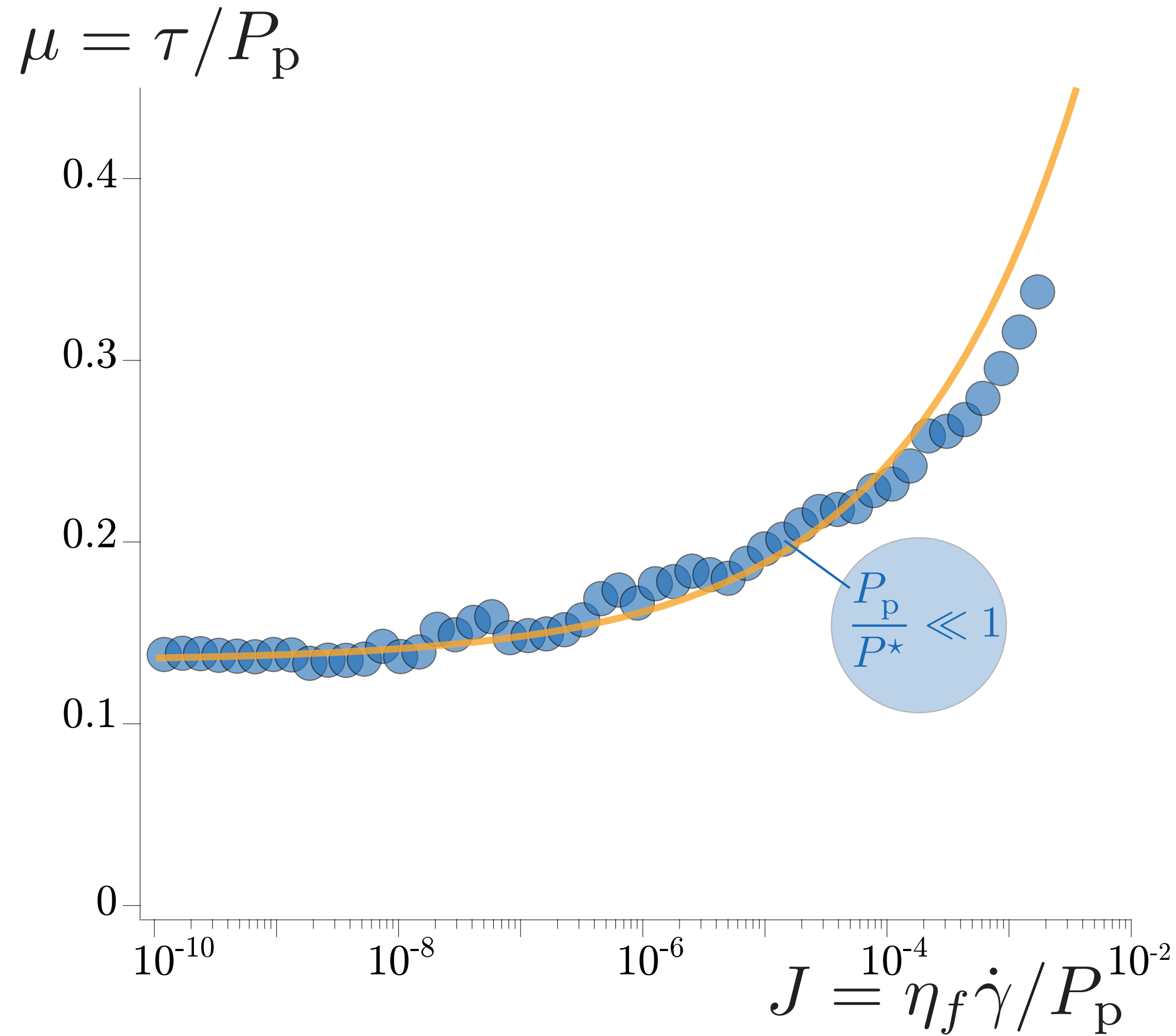
	$P_p/P^*$	Solvent	Frictional state
●	$\ll 1$	H <sub>2</sub> O	Frictionless 

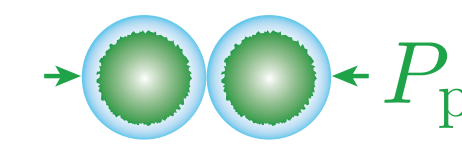
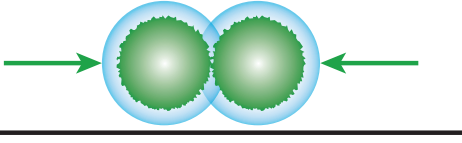
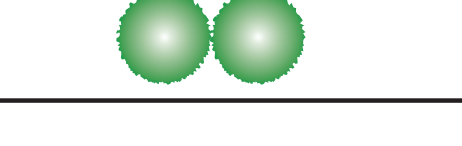


	Experiment	W&C Model
$\frac{P_p}{P^*} \ll 1$	$\mu = 0.13 + 1.7J^{0.3}$ Frictionless particles!	 Frictionless

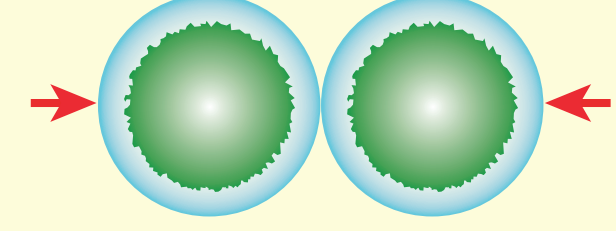
# Probing the Frictional Transition

*Etcheverry, Forterre & Metzger PRX (2022)*



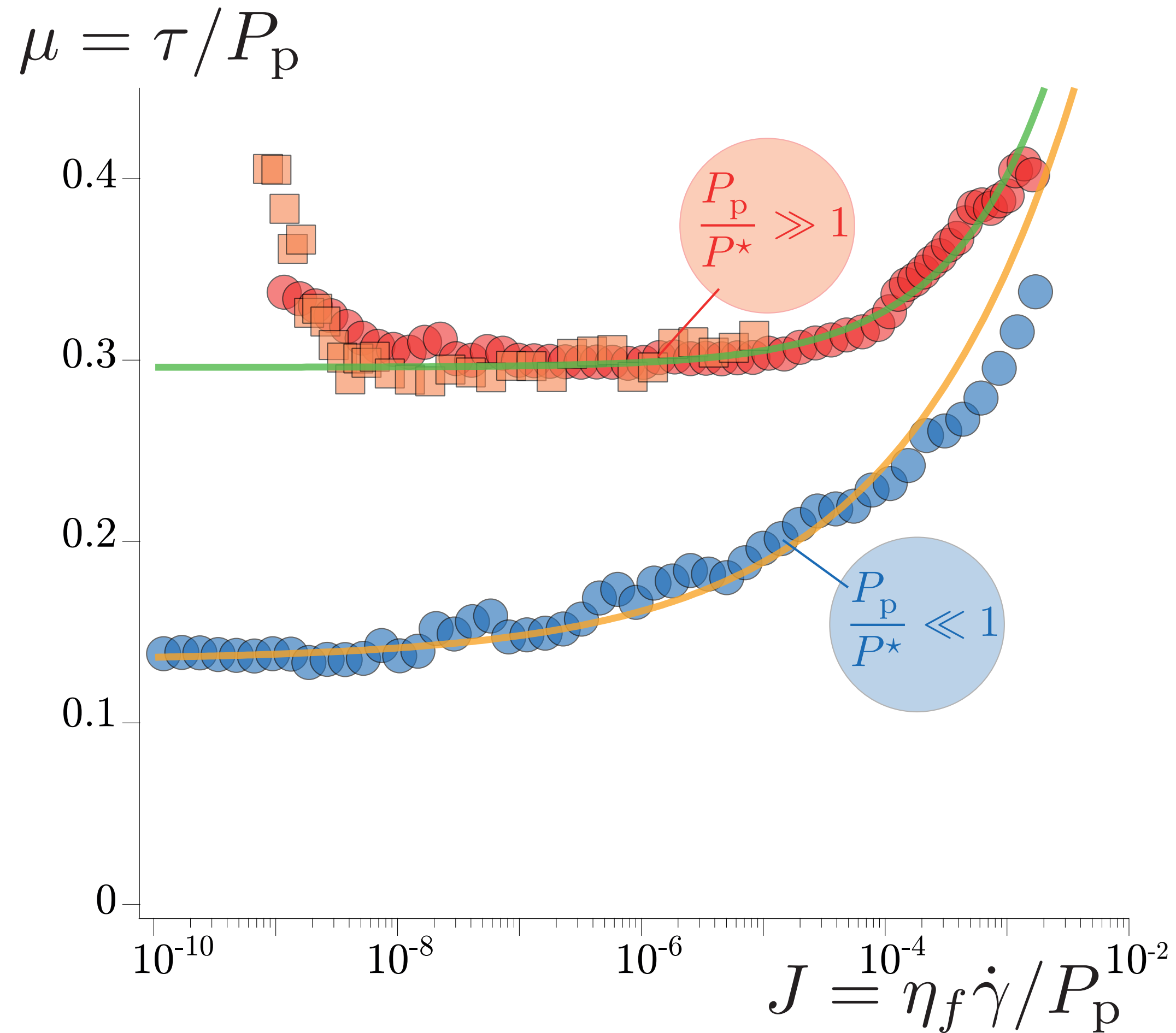
	$P_p / P^*$	Solvent	Frictional state
$\bullet$	$\ll 1$	$H_2O$	Frictionless 
$\blacksquare$	$\gg 1$	$H_2O$	Frictional 
$\bullet$	$\gg 1$	$H_2O + NaCl$	Frictional 

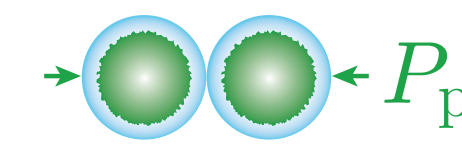
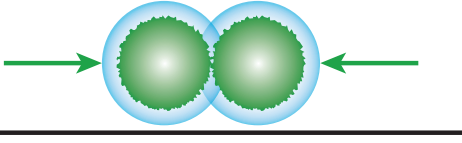
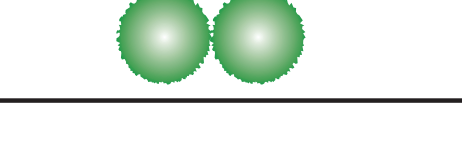
$\nearrow P_p$   
 $\searrow P^*$

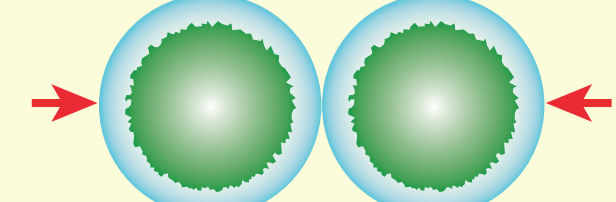
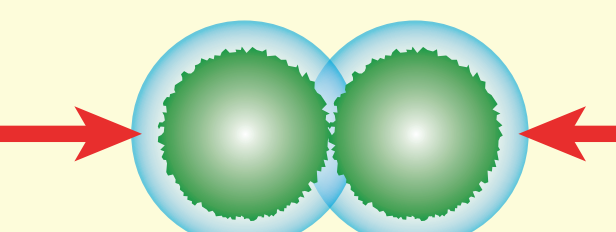
	Experiment	W&C Model
$\frac{P_p}{P^*} \ll 1$	$\mu = 0.13 + 1.7 J^{0.3}$ Frictionless particles!	 Frictionless

# Probing the Frictional Transition

*Etcheverry, Forterre & Metzger PRX (2022)*

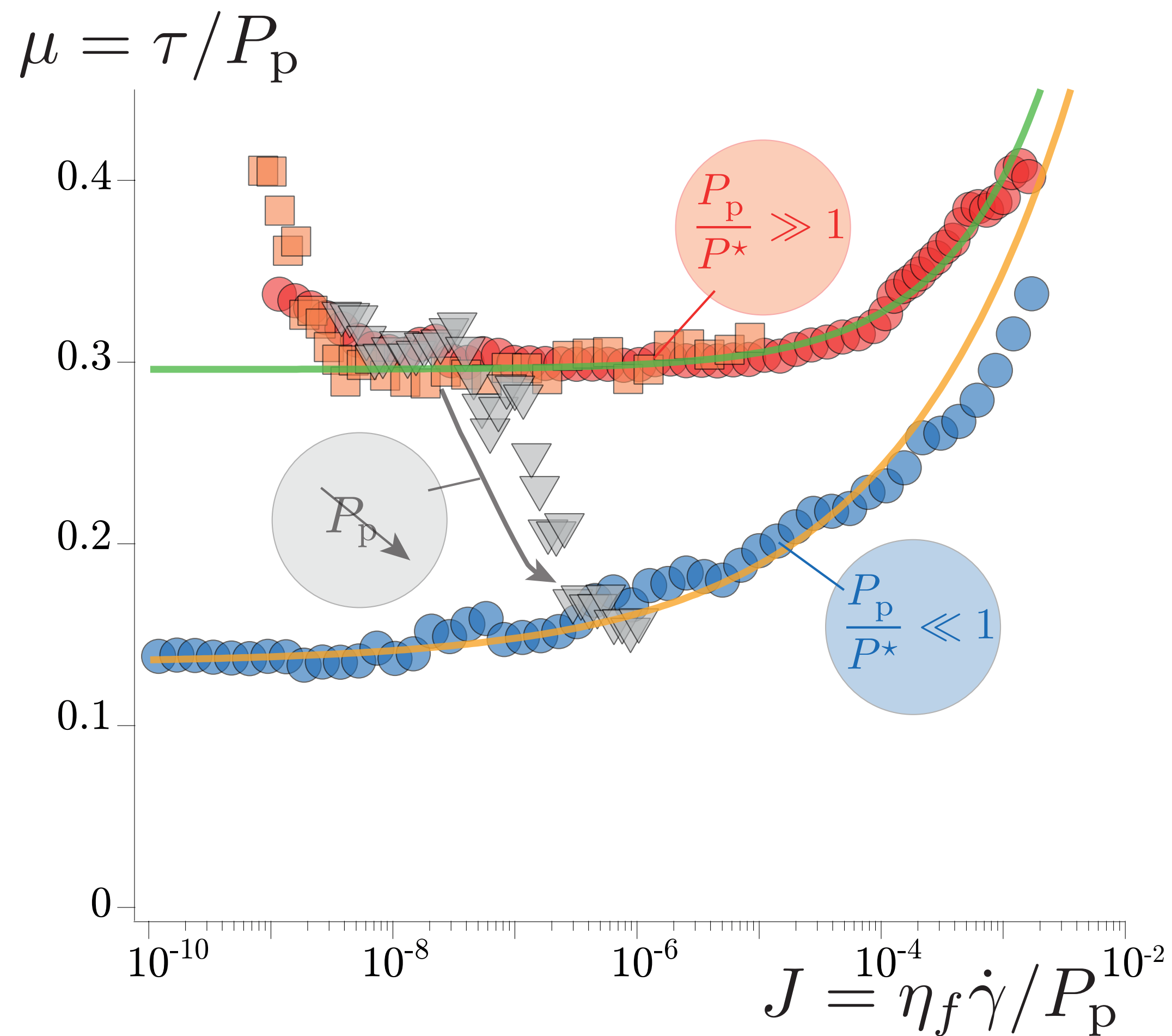


	$P_p / P^*$	Solvent	Frictional state
$\nearrow P_p$	$\ll 1$	H <sub>2</sub> O	Frictionless 
	$\gg 1$	H <sub>2</sub> O	Frictional 
$\searrow P^*$	$\gg 1$	H <sub>2</sub> O+NaCl	Frictional 

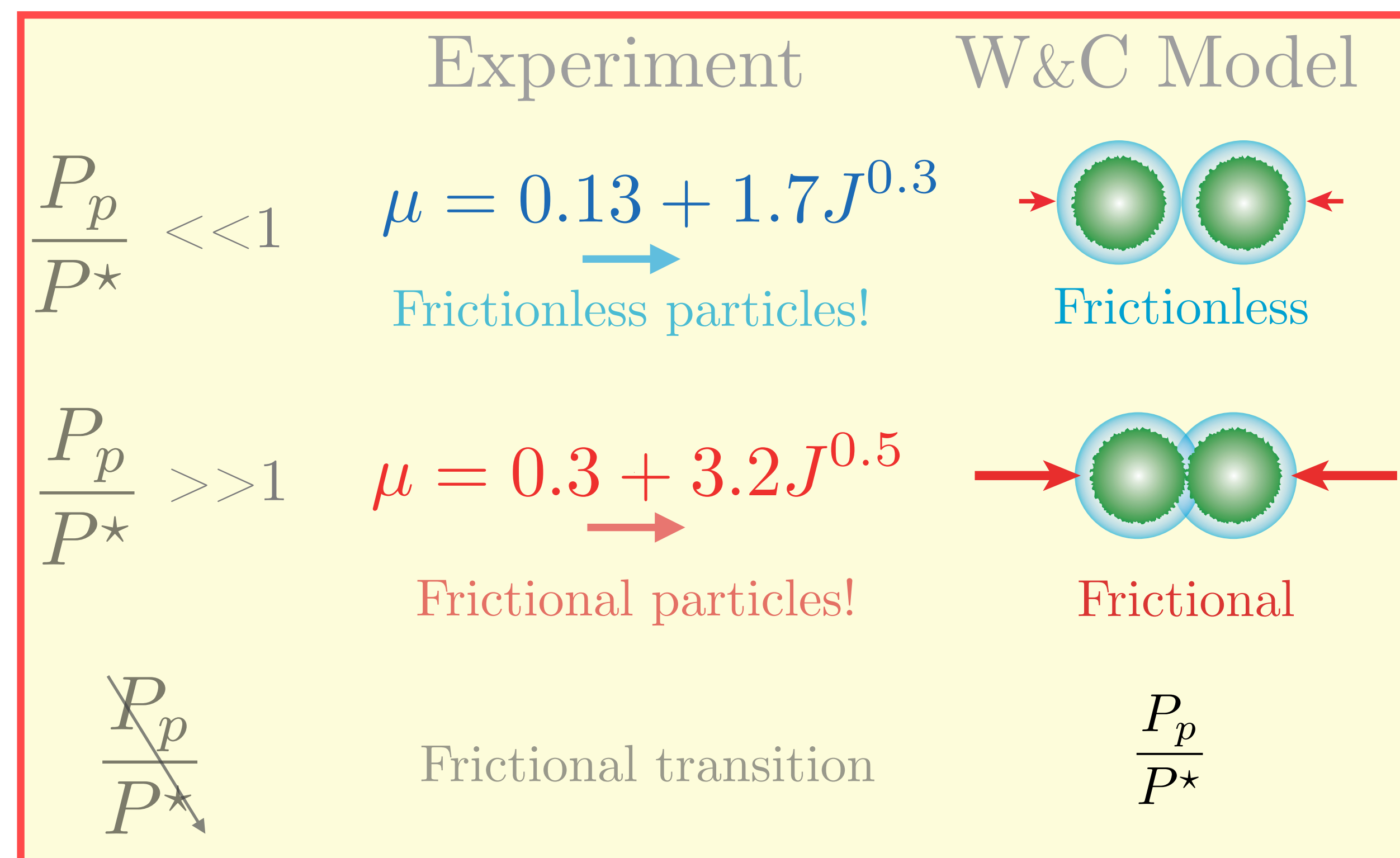
	Experiment	W&C Model
$\frac{P_p}{P^*} \ll 1$	$\mu = 0.13 + 1.7J^{0.3}$ Frictionless particles!	 Frictionless
$\frac{P_p}{P^*} \gg 1$	$\mu = 0.3 + 3.2J^{0.5}$ Frictional particles!	 Frictional

# Probing the Frictional Transition

*Etcheverry, Forterre & Metzger PRX (2022)*

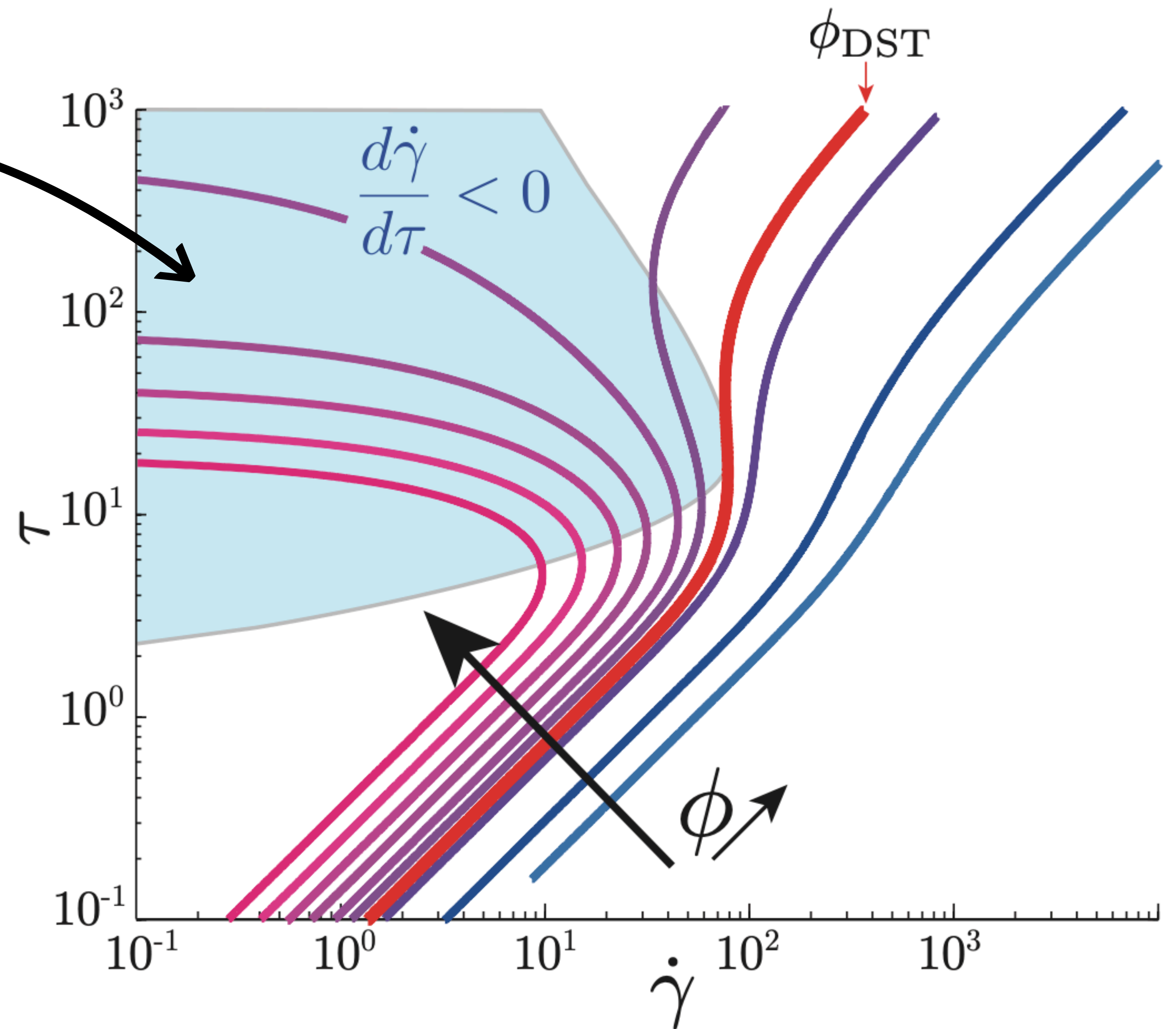


	$P_p / P^*$	Solvent	Frictional state
●	$\ll 1$	H <sub>2</sub> O	Frictionless
■	$\gg 1$	H <sub>2</sub> O	Frictional
●	$\gg 1$	H <sub>2</sub> O+NaCl	Frictional
▼	$\gg 1$ to $\ll 1$	H <sub>2</sub> O	Frictional to Frictionless

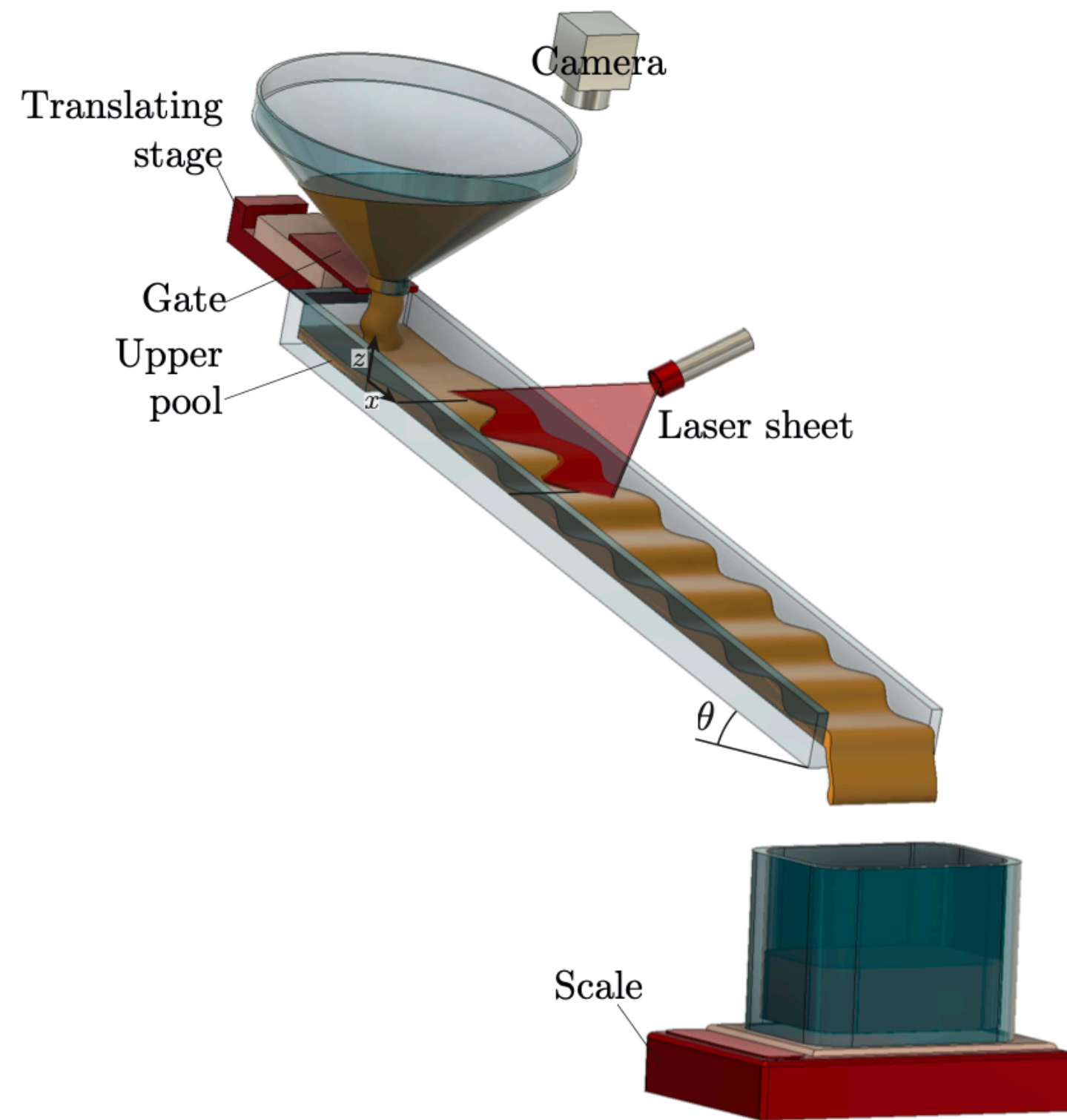


# Hydrodynamics of Shear—thickening Suspensions

Consequences of this velocity—weakening [*unstable*] branch to hydrodynamics?



# Shear—thickening Suspensions down inclines: Oobleck Waves



Not understood, no flow rules !  
(Balmforth Phys. Let. A 2005)

*Darbois—Texier et al. Comm. Phys. (2020)*

*Darbois—Texier et al. JFM (2023)*

*Kapitza Waves in Water*

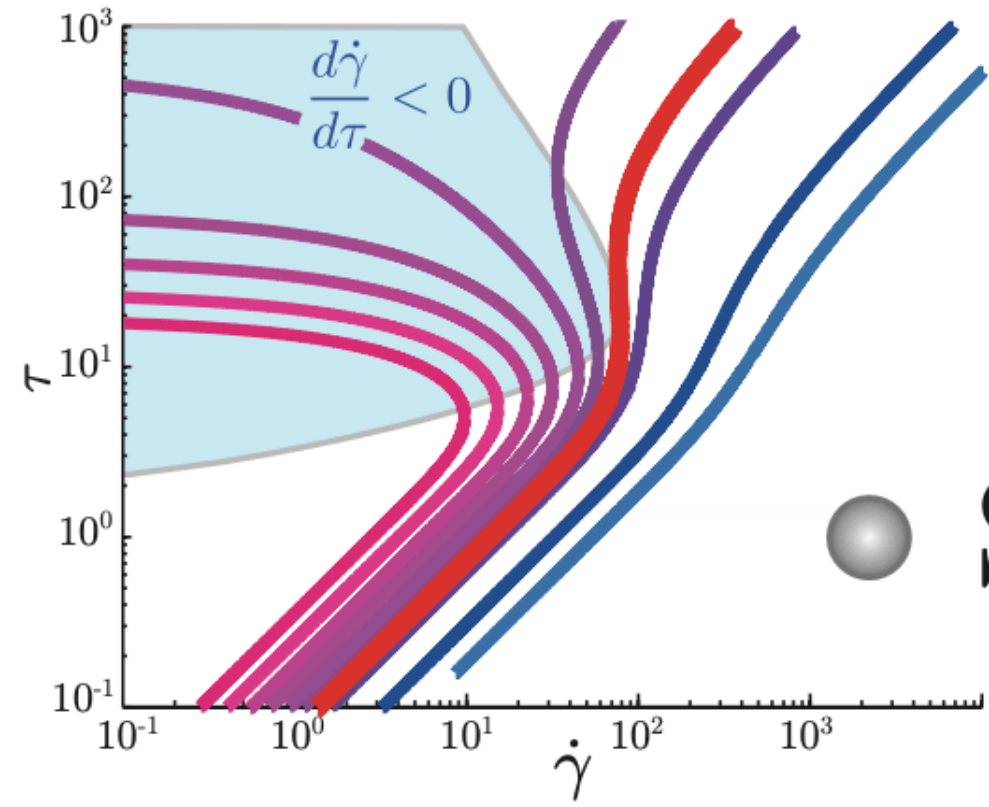


*Inertial Instability!*

$$Re_c = Re_K$$

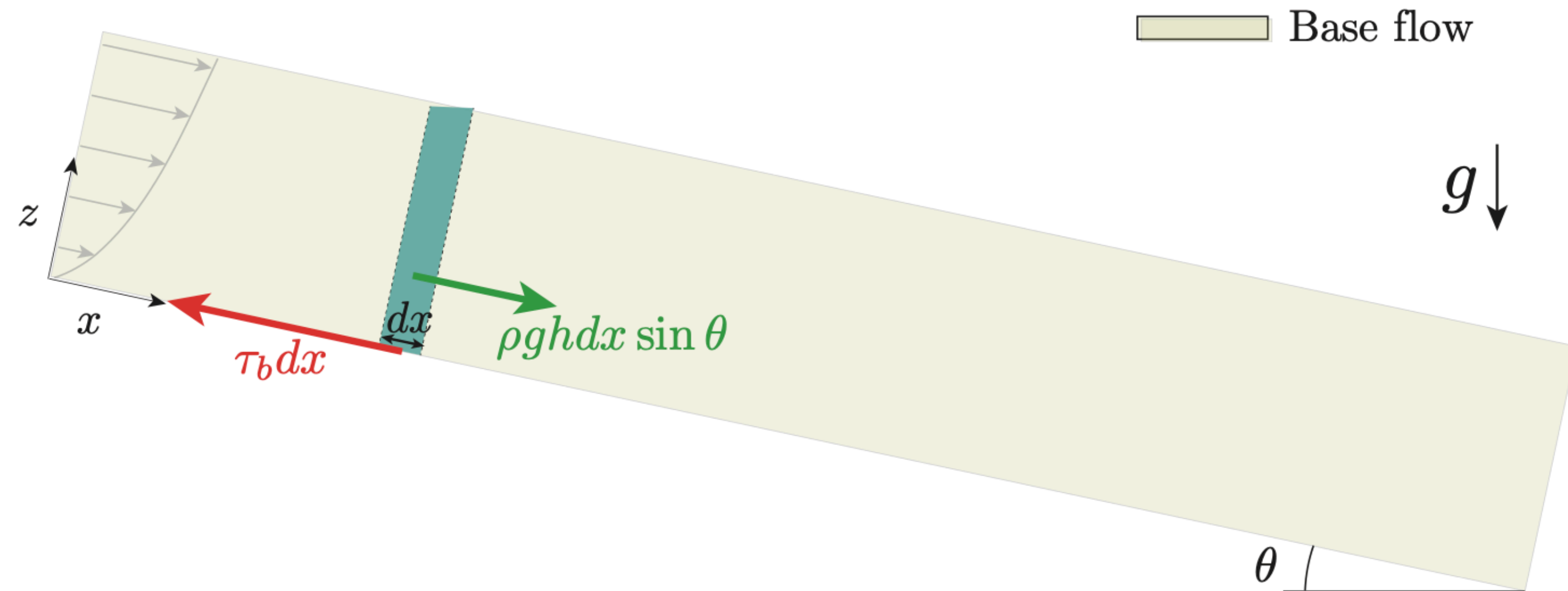


# Instability Mechanism without Inertia



● S-shaped  $A = \frac{d\dot{\gamma}}{d\tau} < 0$

● No inertia  $Re \ll 1$

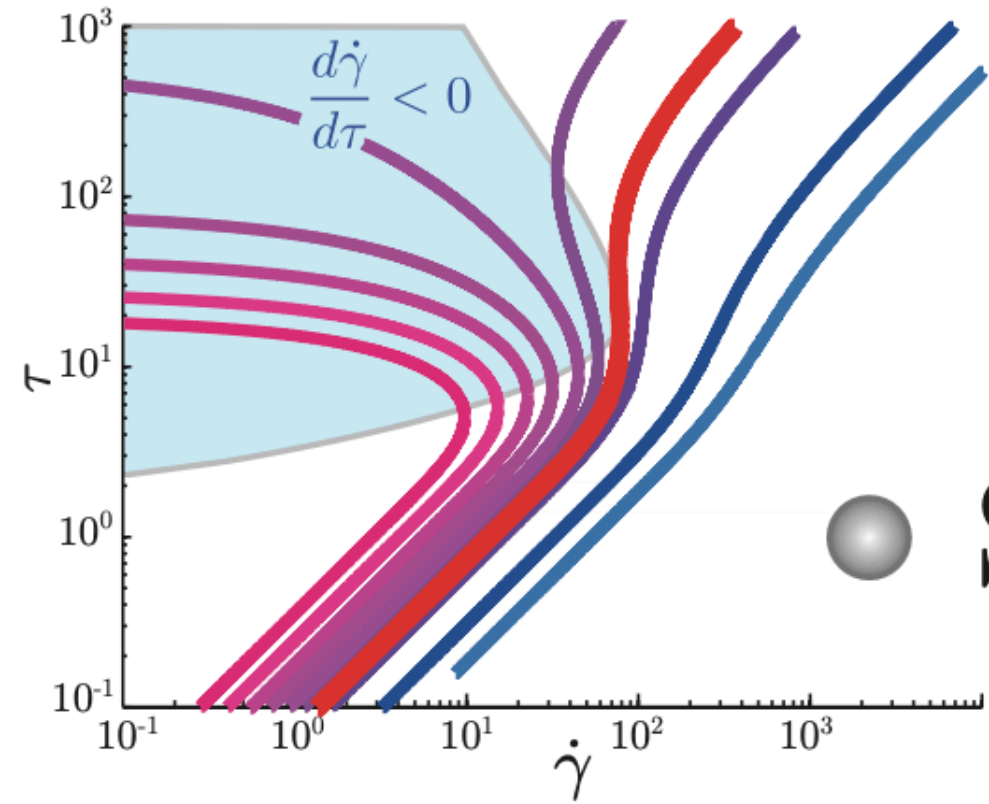


Force balance (depth averaged):

$$\tau_b = \rho g h \sin \theta$$

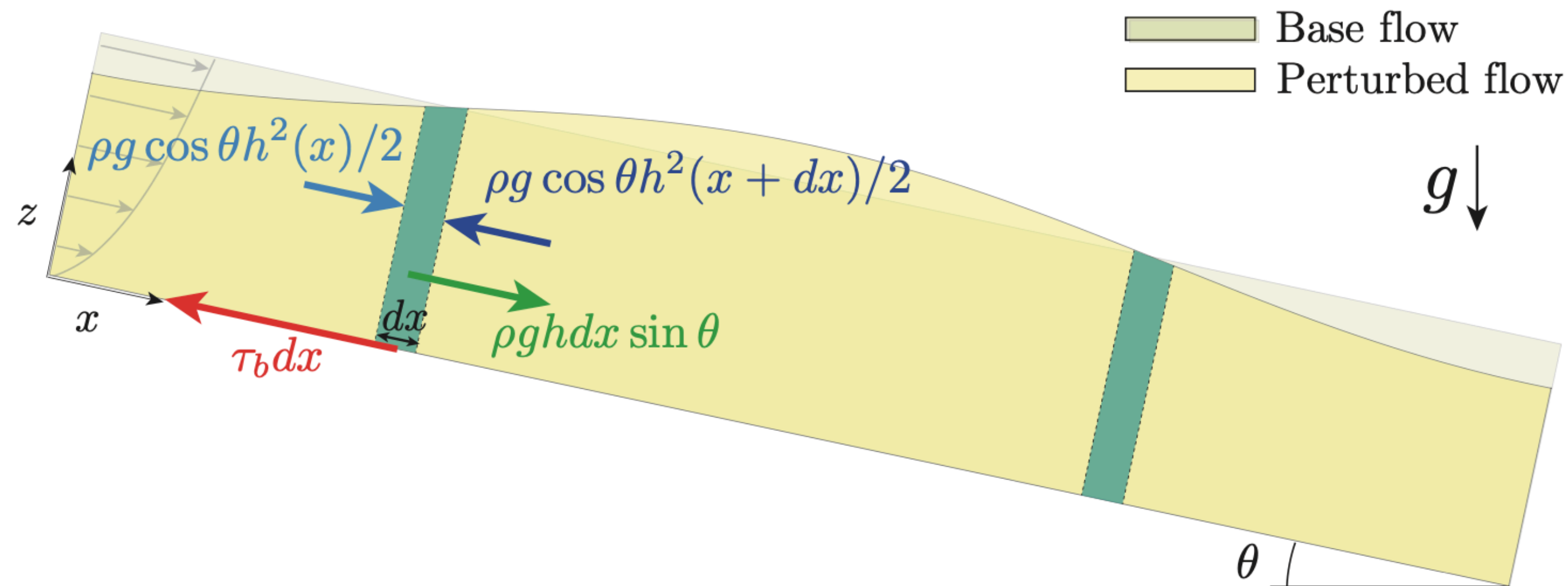
Basal stress Gravity

# Instability Mechanism without Inertia



● S-shaped  $A = \frac{d\dot{\gamma}}{d\tau} < 0$

● No inertia  $Re \ll 1$



Force balance (depth averaged):

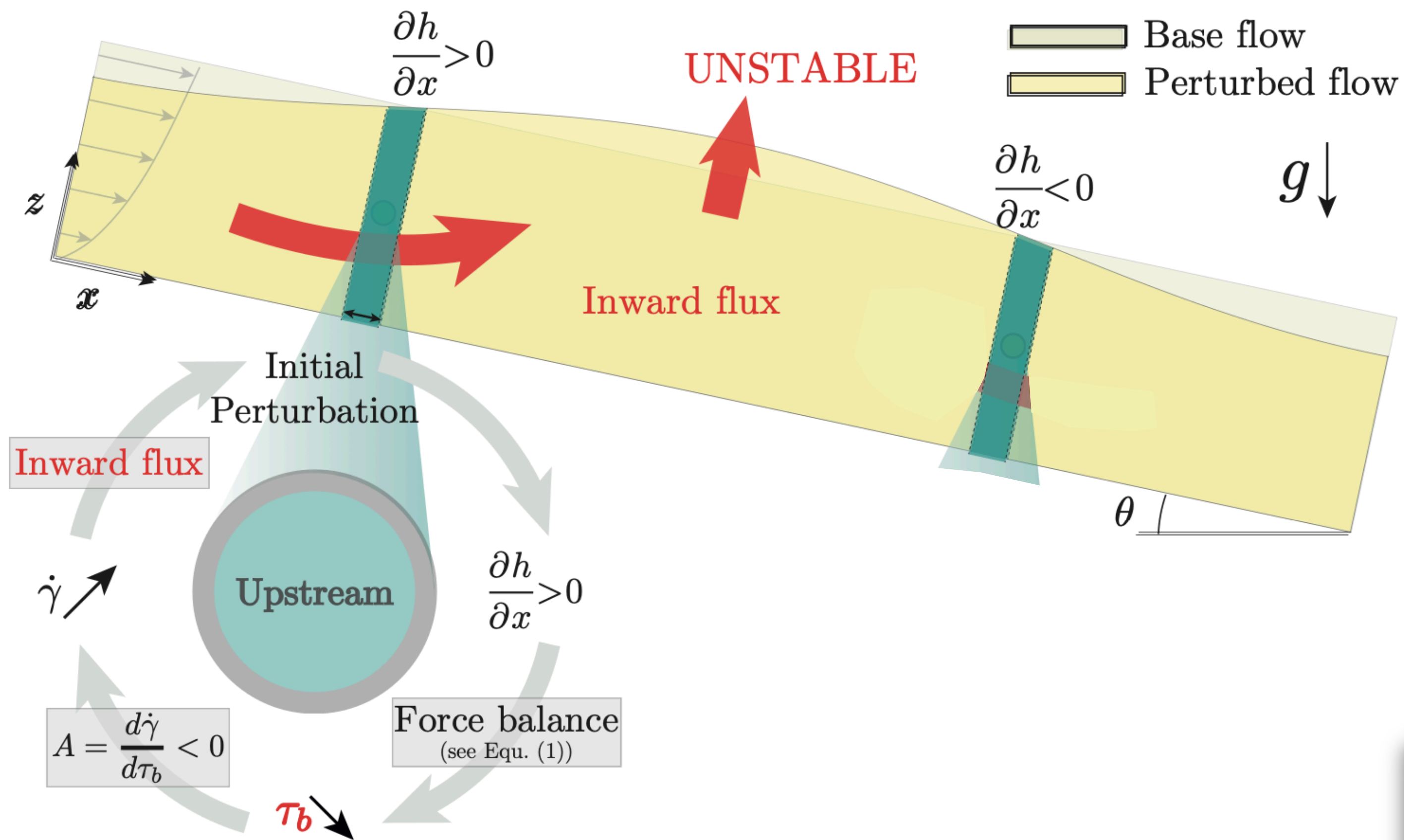
$$\tau_b = \rho g h \sin \theta - \rho g h \cos \theta \frac{\partial h}{\partial x}$$

Basal stress   Gravity   Hydrostatic pressure

# Instability Mechanism *without* Inertia

- S-shaped  $A = \frac{d\dot{\gamma}}{d\tau} < 0$

- No inertia  $Re \ll 1$



Force balance (depth averaged):

$$\tau_b = \rho g h \sin \theta - \rho g h \cos \theta \frac{\partial h}{\partial x}$$

Basal stress

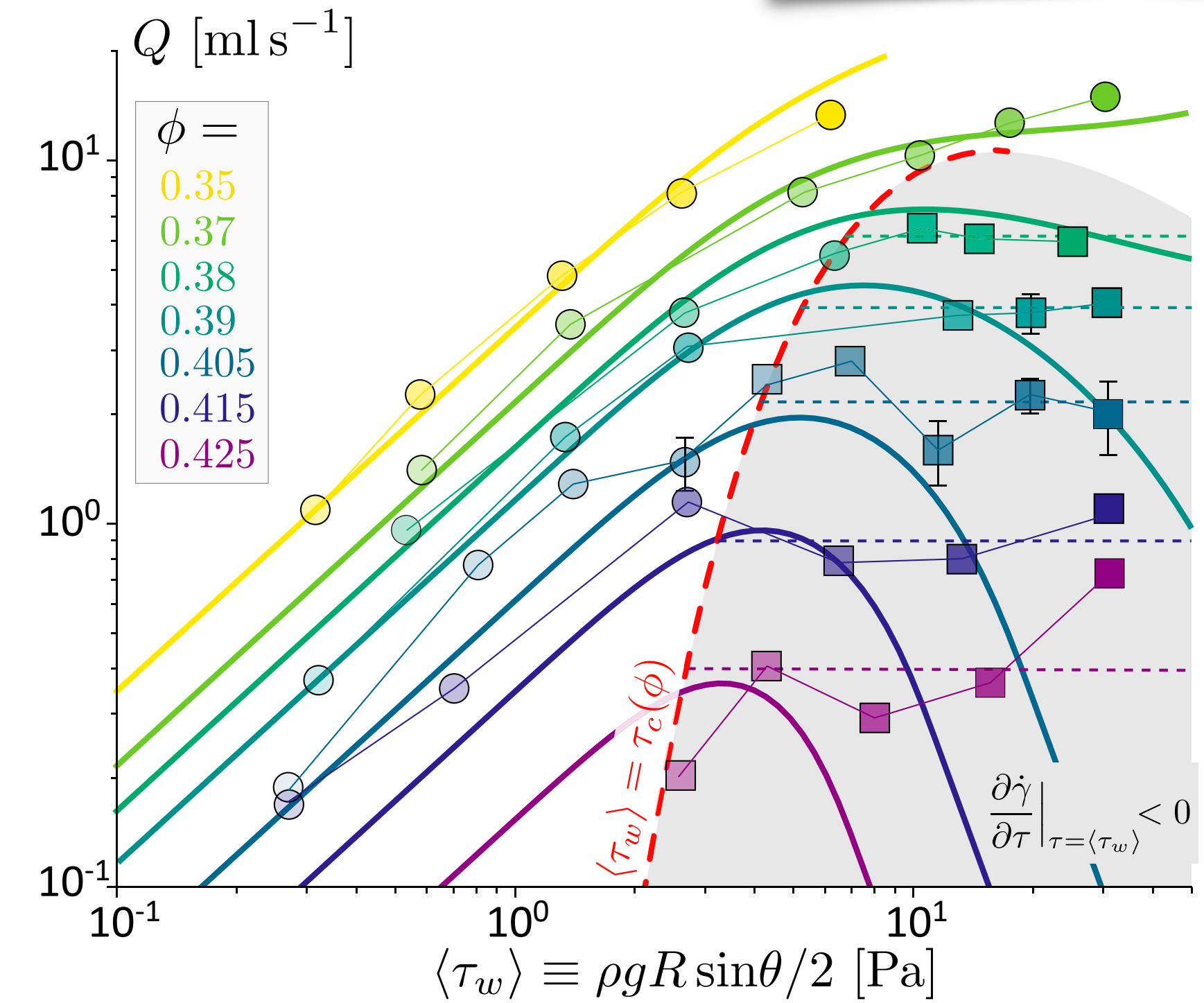
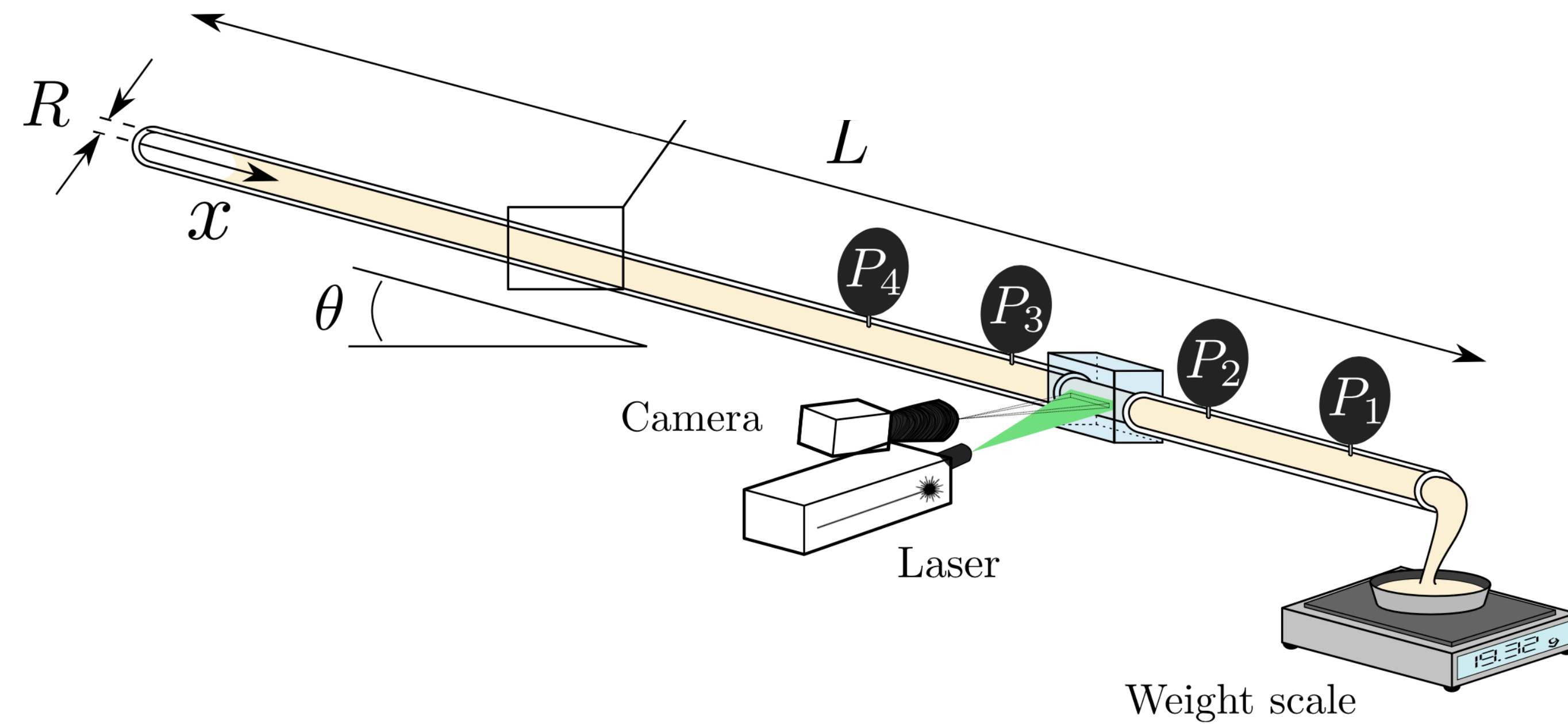
Gravity

Hydrostatic  
pressure

→ Unstable if  $A = \frac{d\dot{\gamma}}{d\tau} < 0$

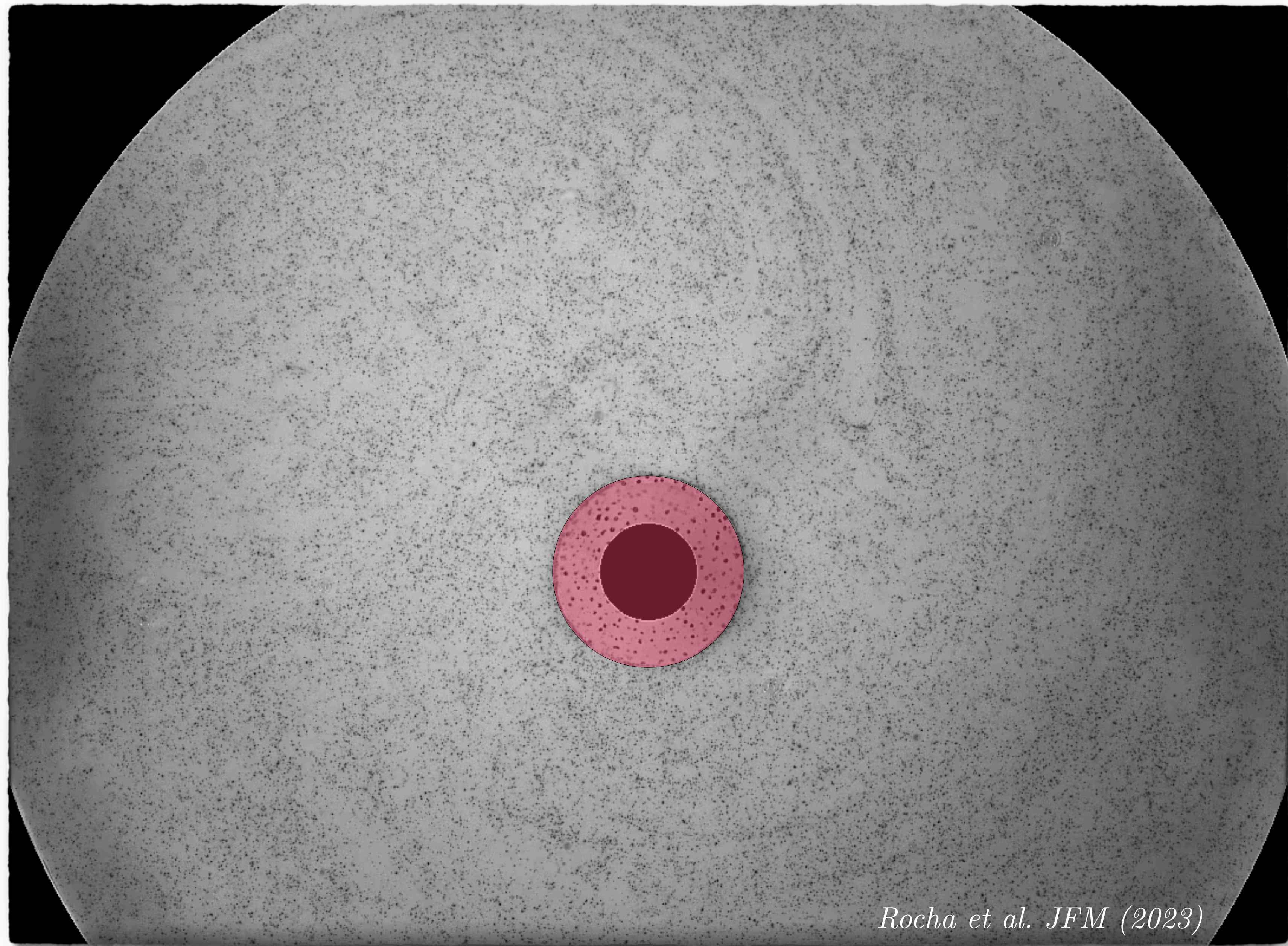
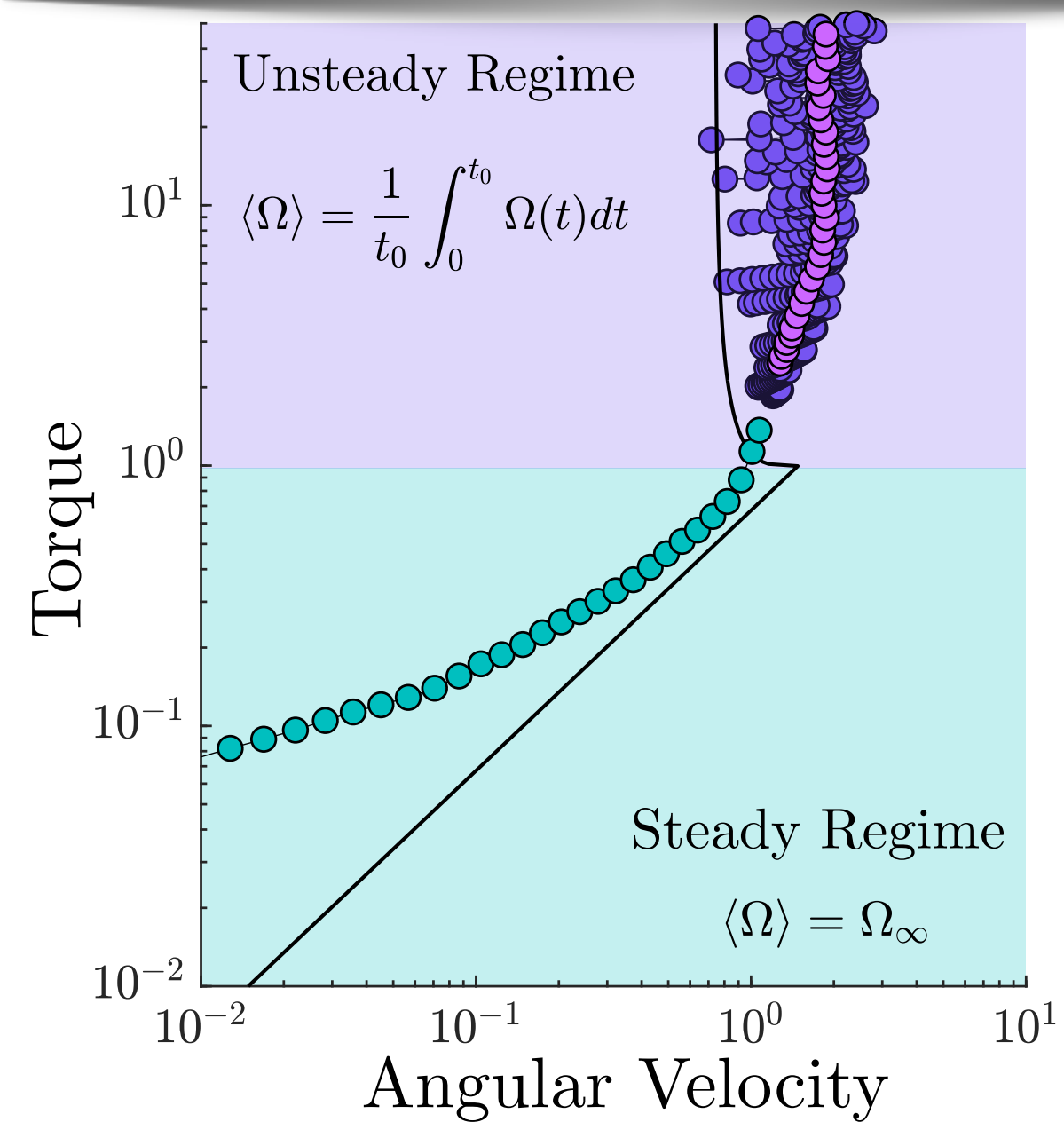
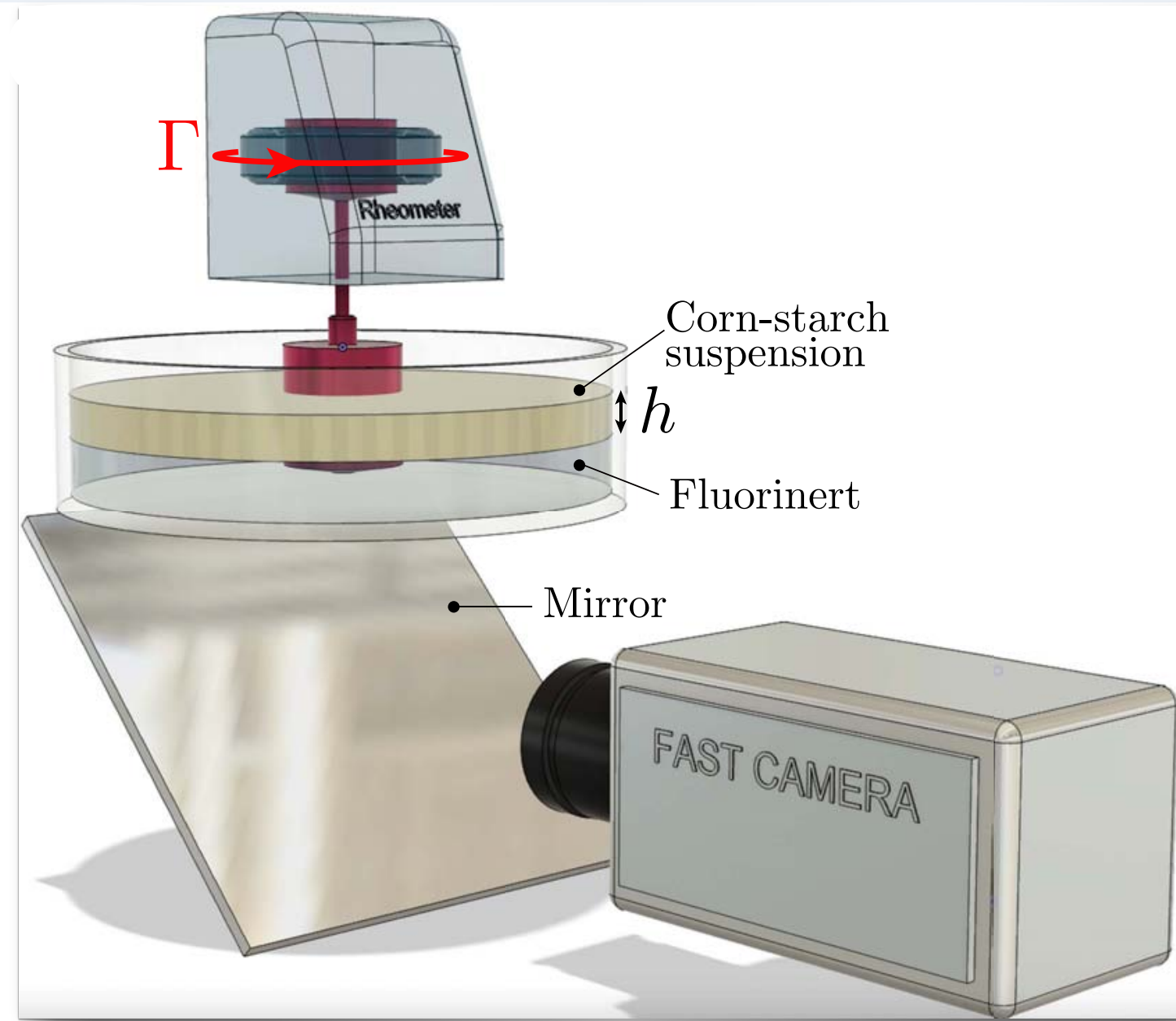
# Pipe flow of Shear—thickening Suspensions

Talk:  
Alexis Bougouin  
*S2 on Friday*

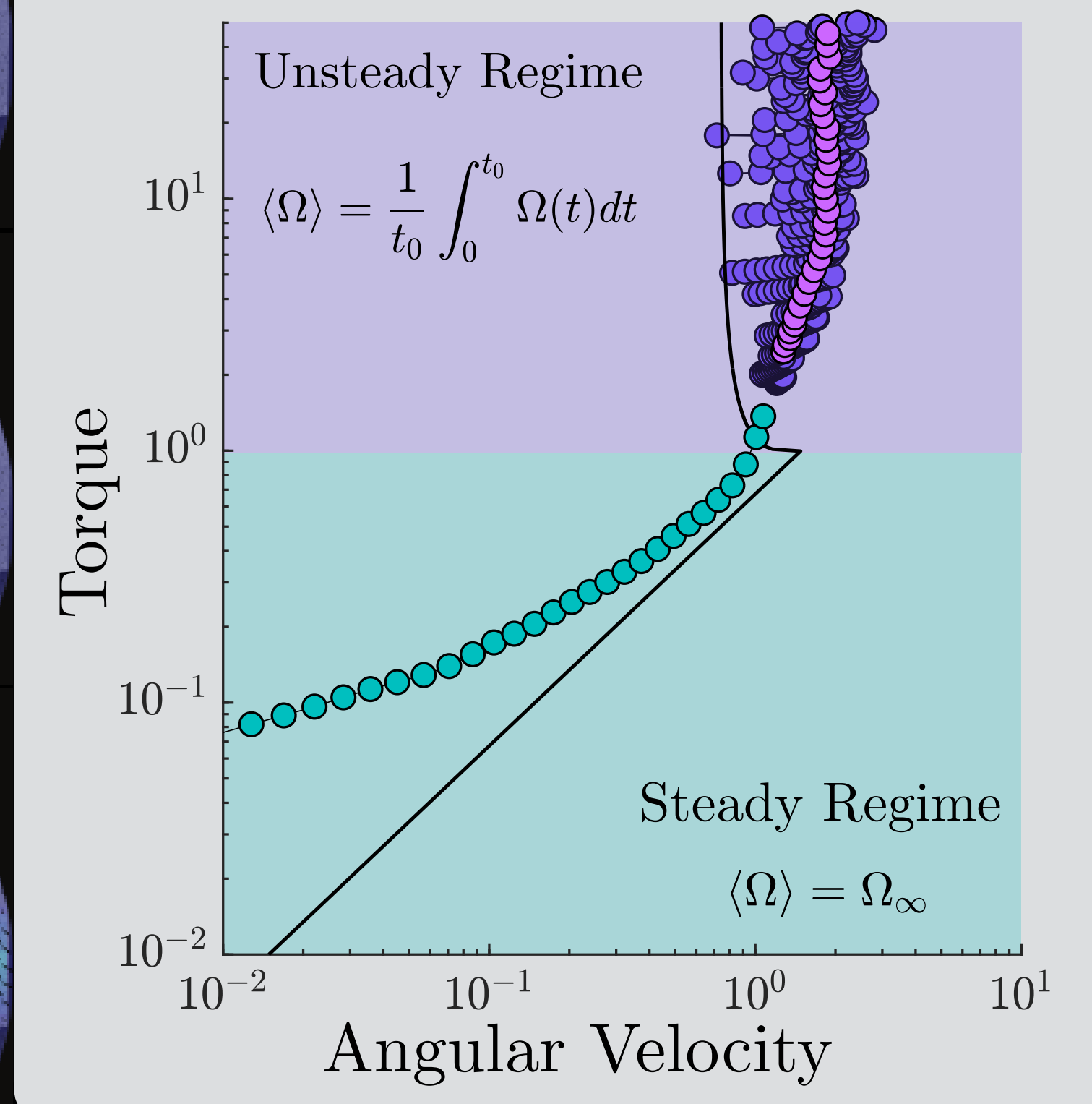
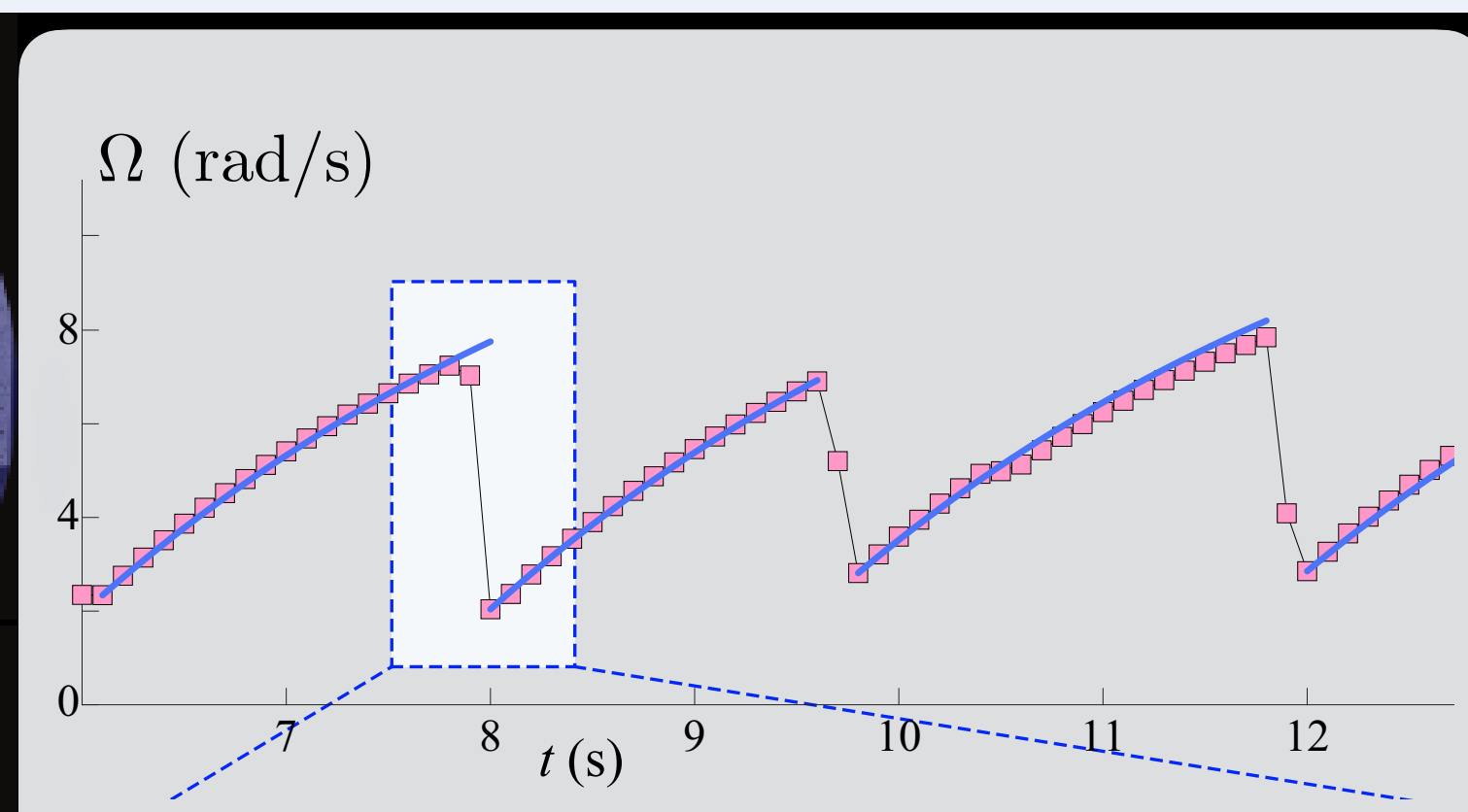
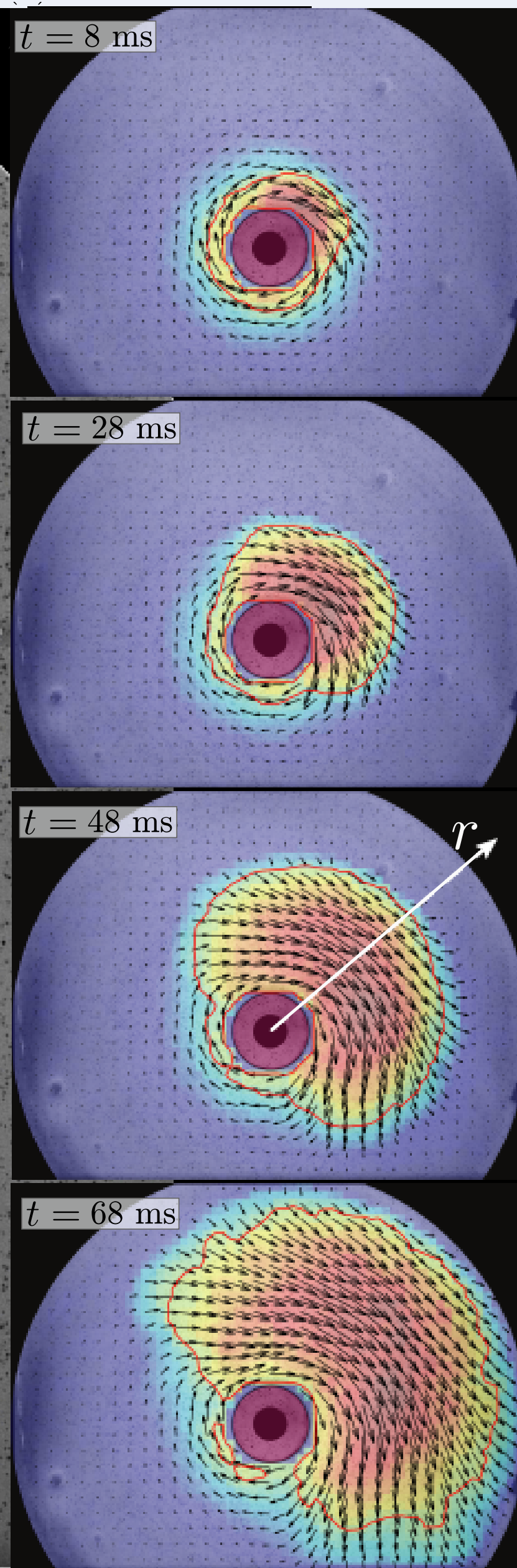
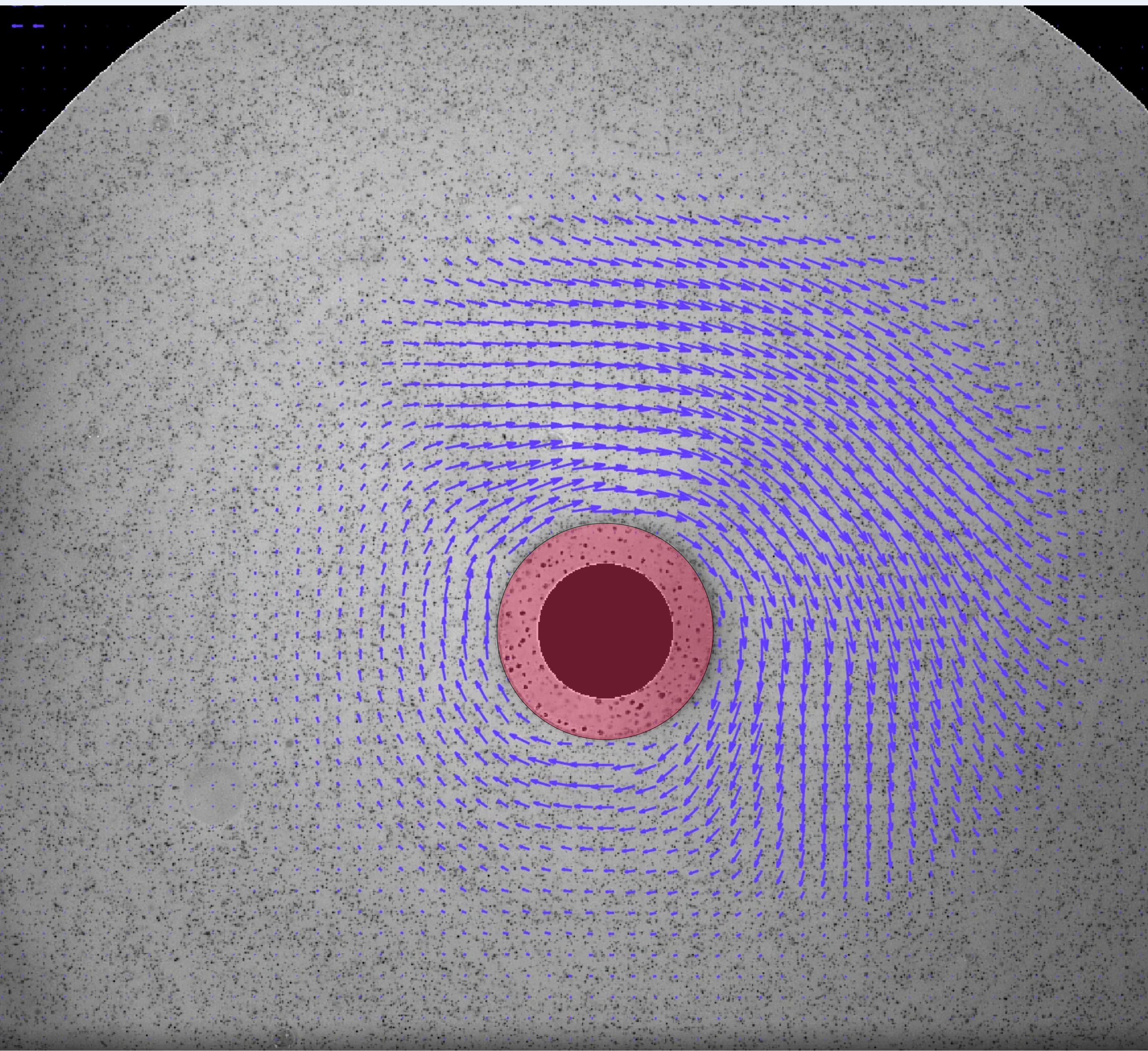


A retrogressive FRictional Solitary Wave controls the flow rate!

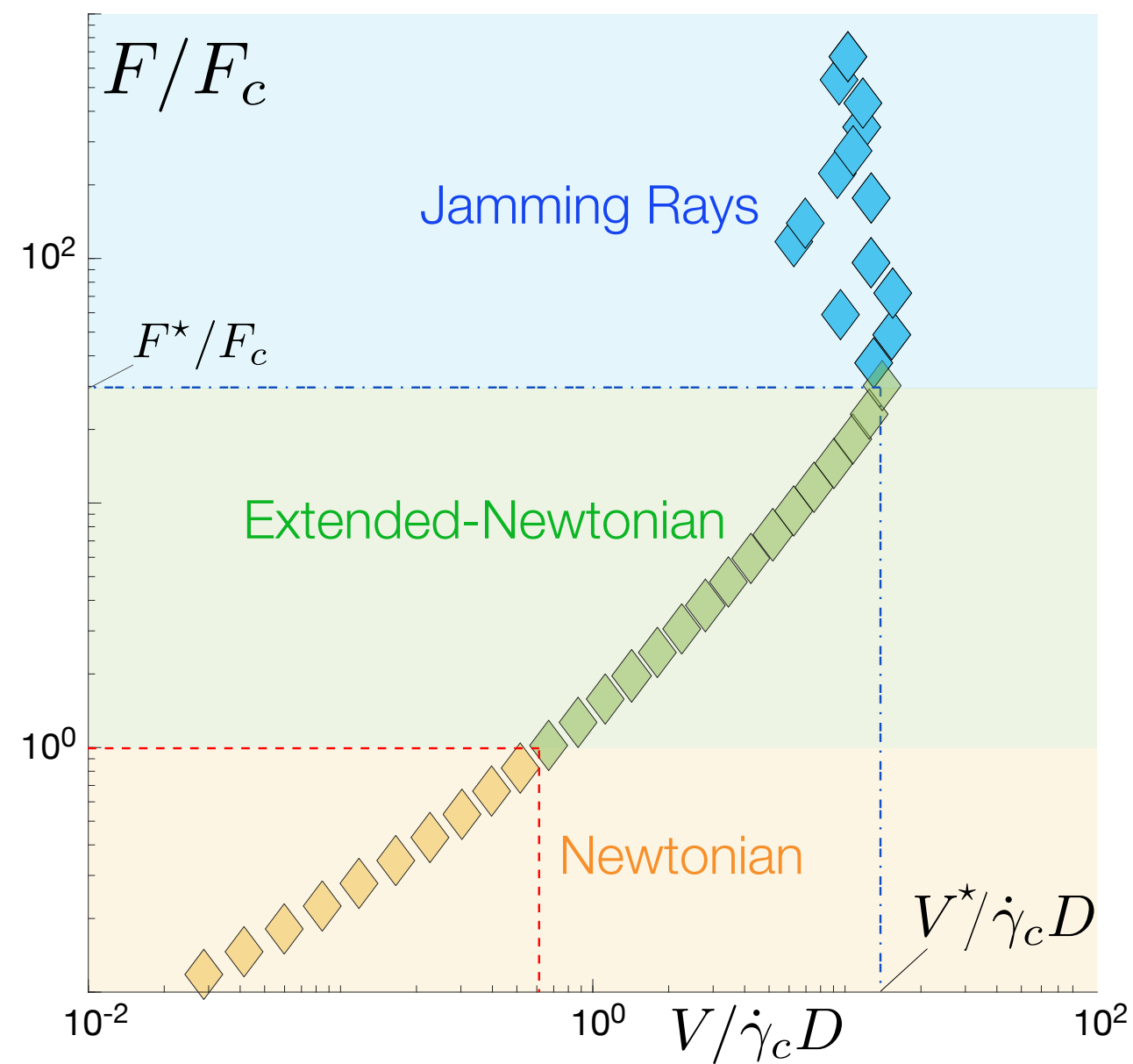
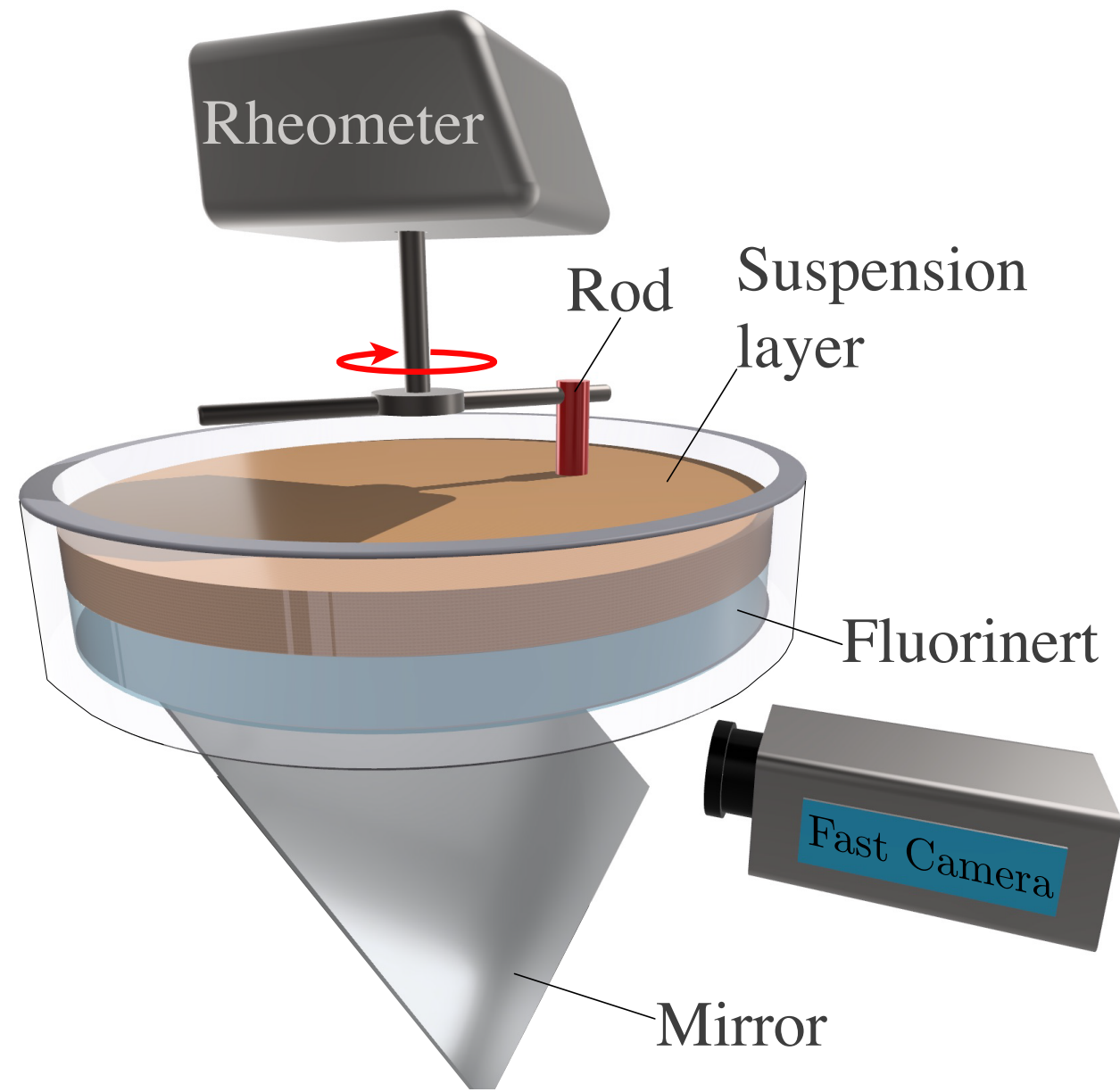
# Drag Forces in Shear—thickening Suspensions



# Drag Forces in Shear—thickening Suspensions



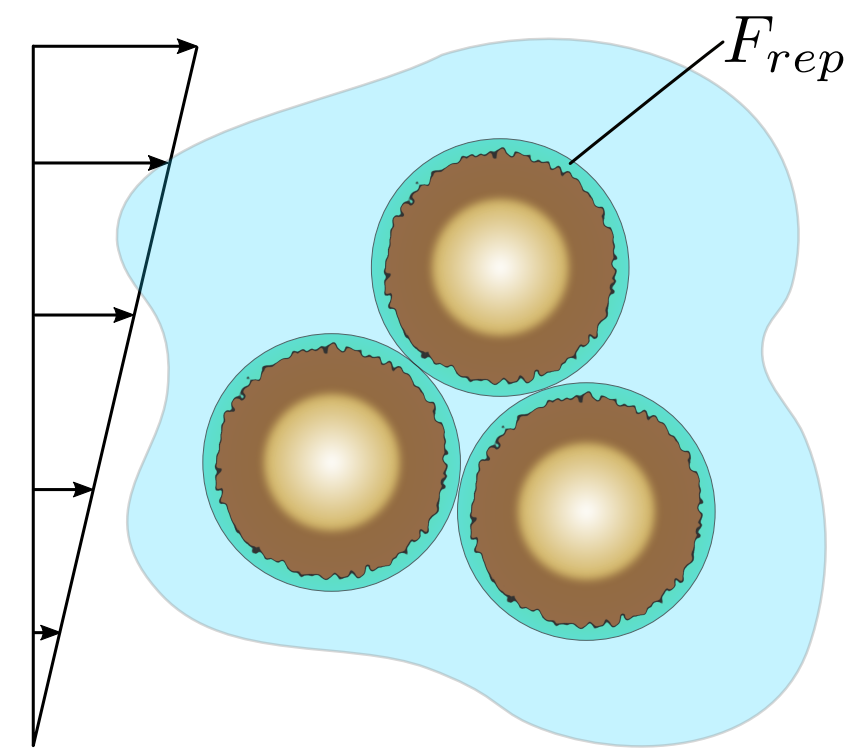
# Flow of a Shear—thickening Suspensions around a Cylinder



(Rocha et al. to be submitted)

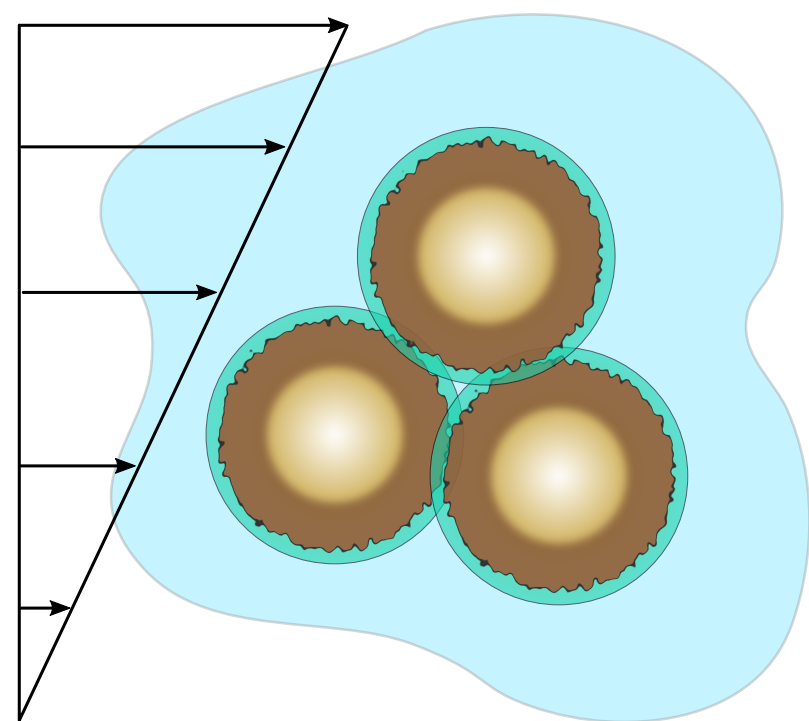
# To Conclude...

## Frictional Transition at the particle scale



Low Stress  $P < P_{rep}$

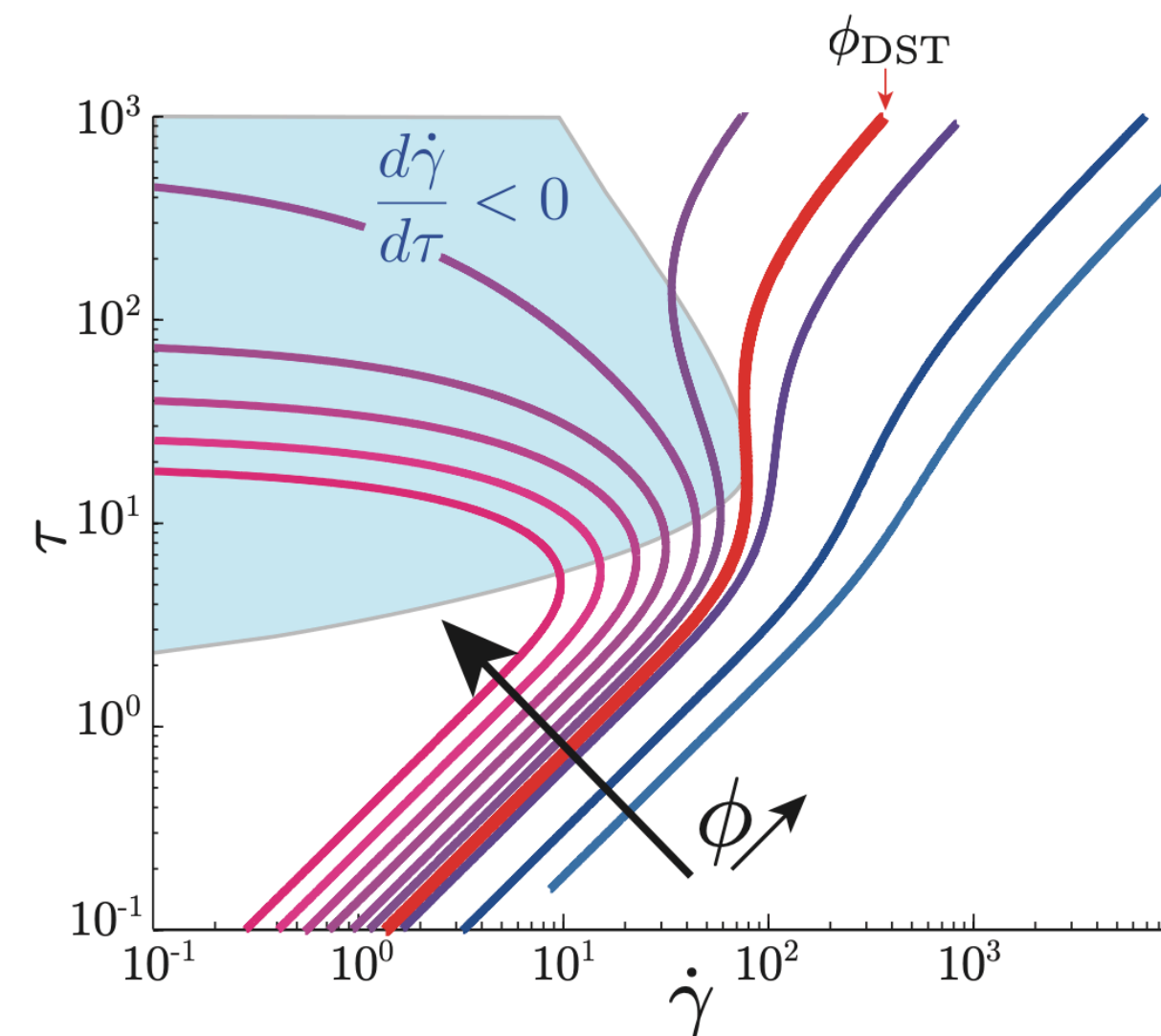
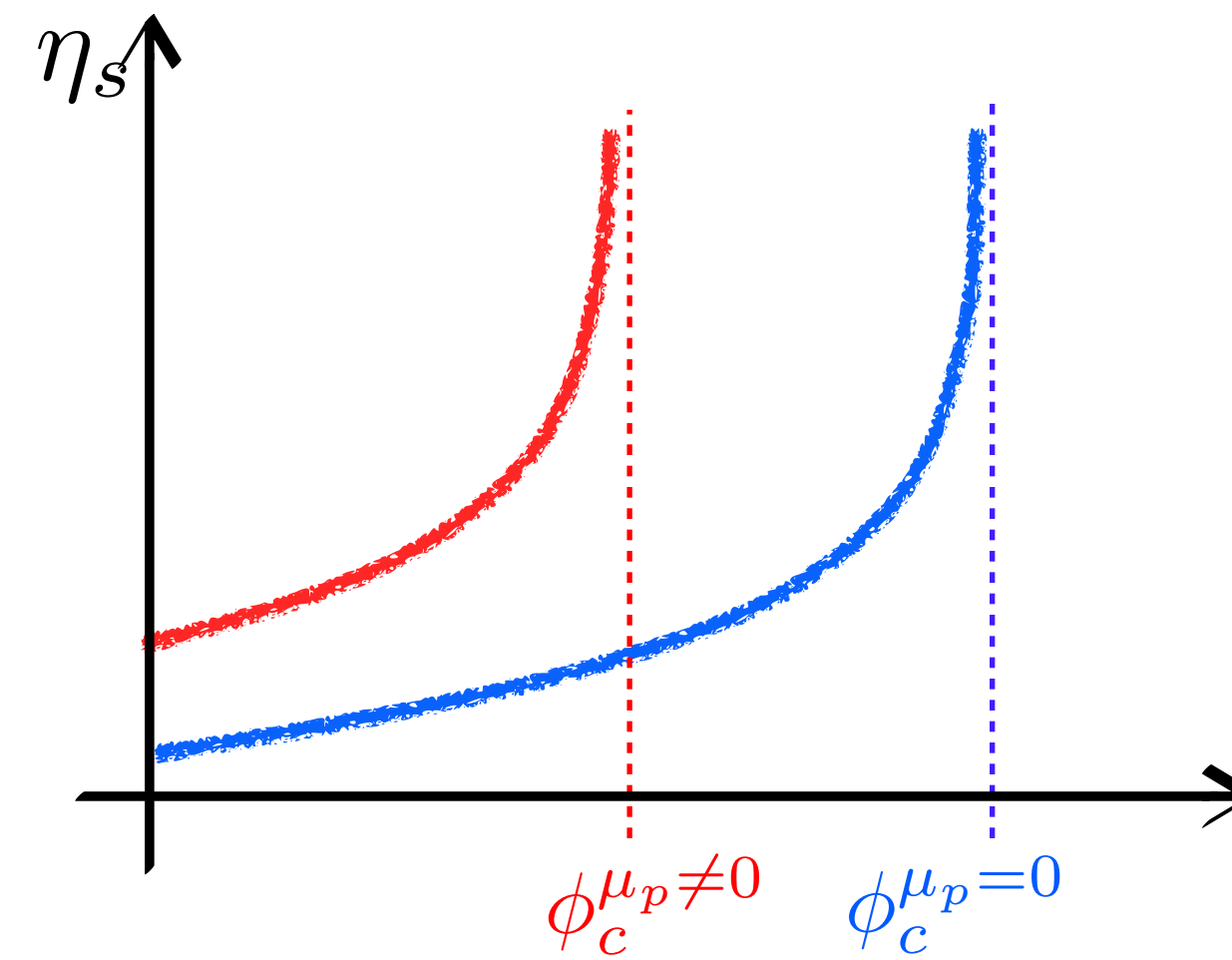
**Frictionless**



High Stress  $P > P_{rep}$

**Frictional**

## Peculiar Rheology [Flow Rules]



## Flow Properties

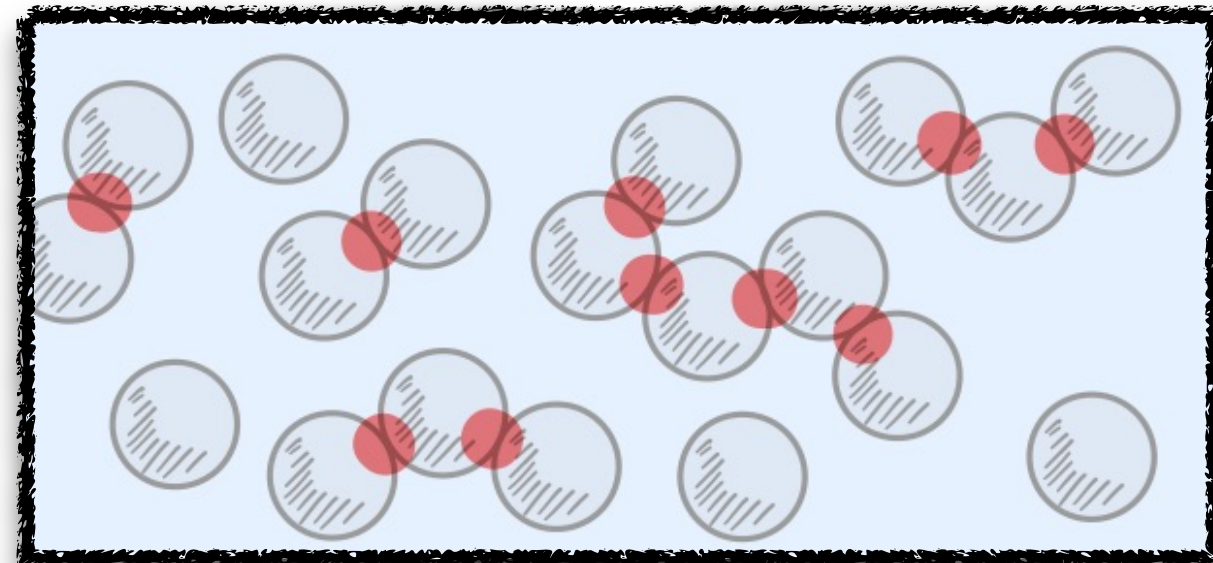




# To Conclude...

Dilute

Dense



long-range hydrodynamics

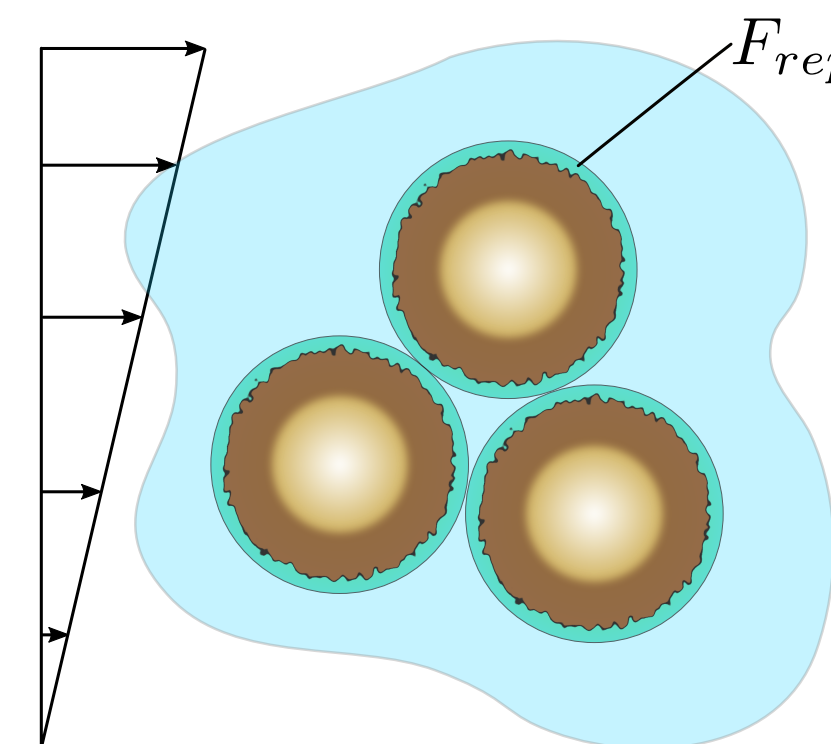
contact dynamics

If  $\phi_c$  changes dynamically



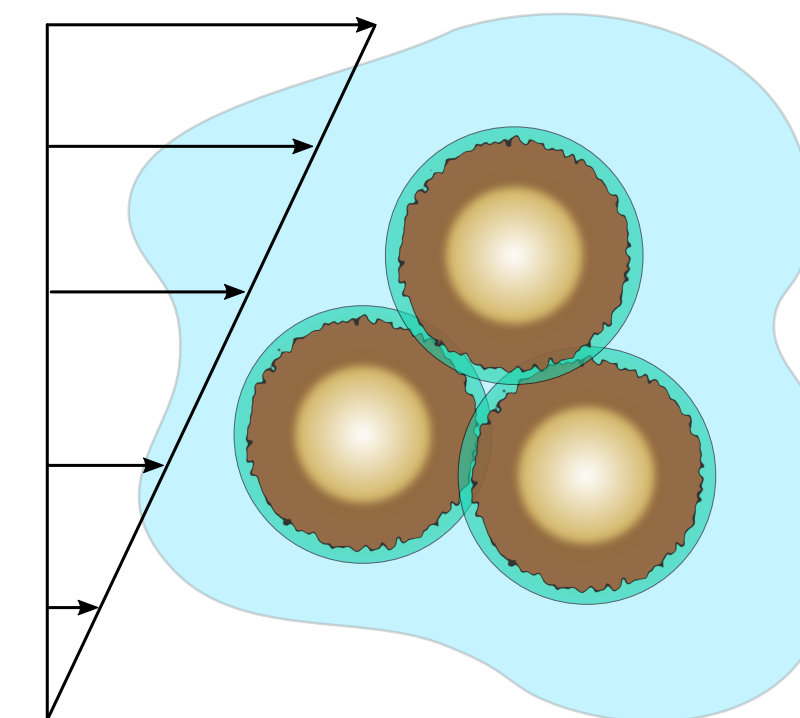
non-Newtonian Behaviours

e.g. Shear thickening



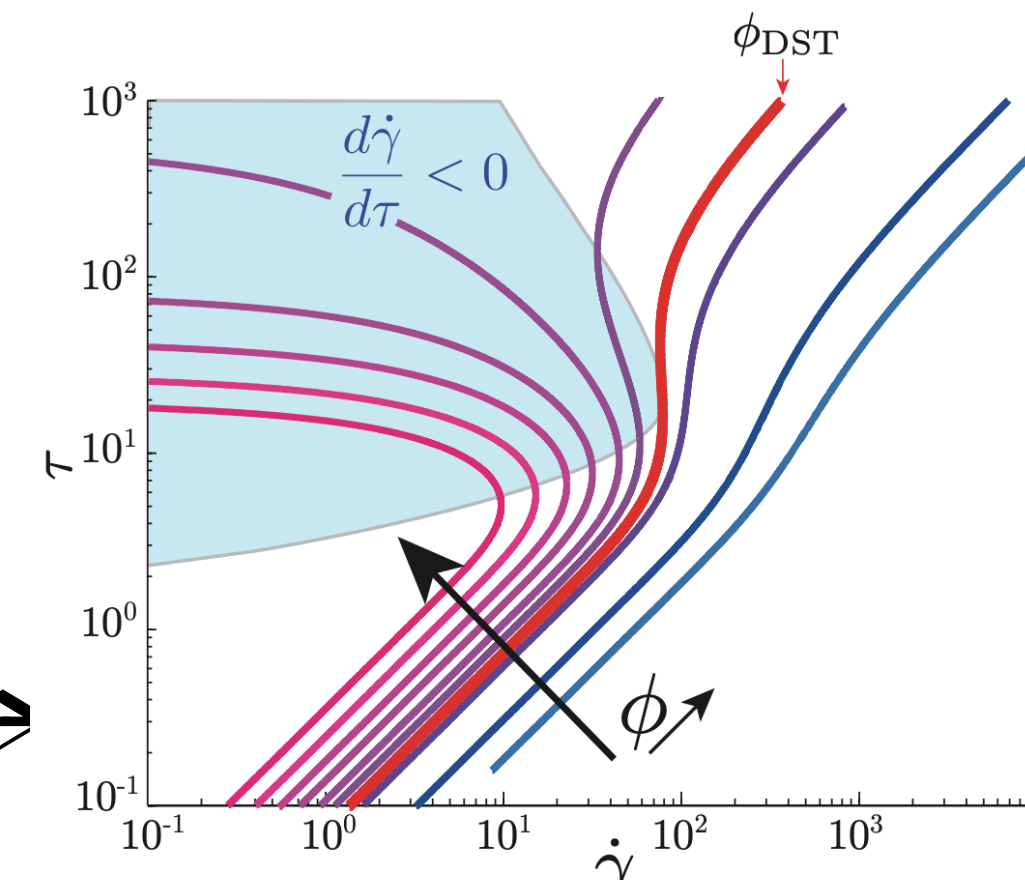
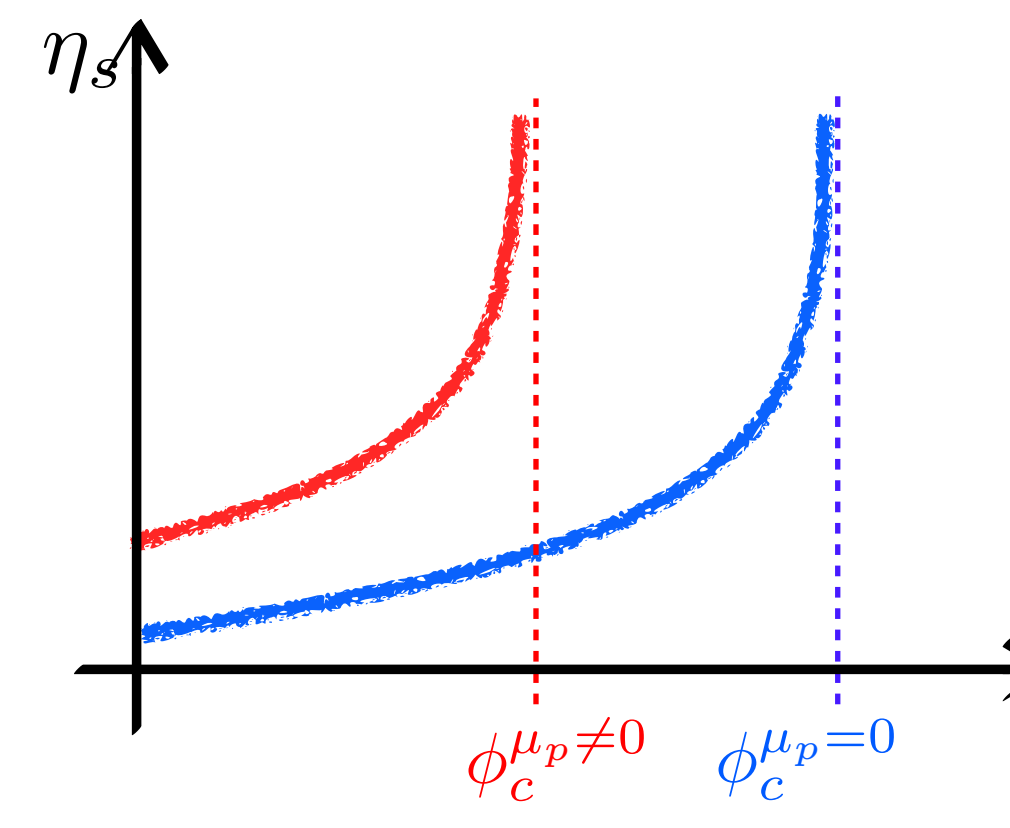
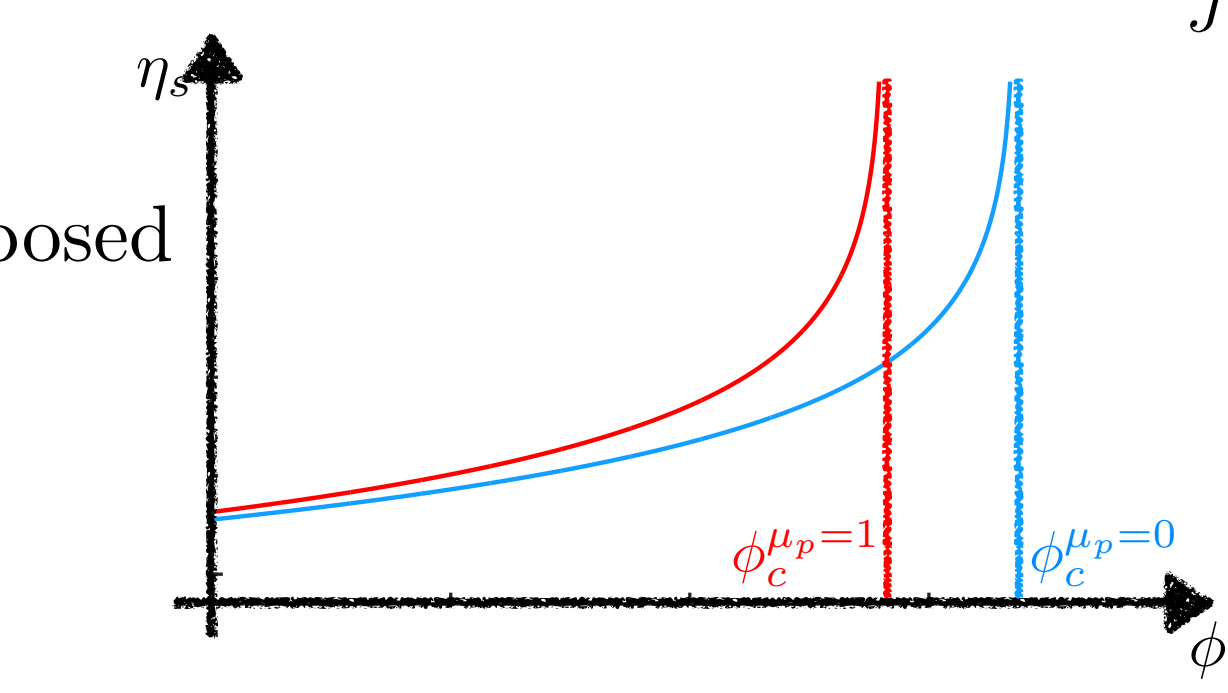
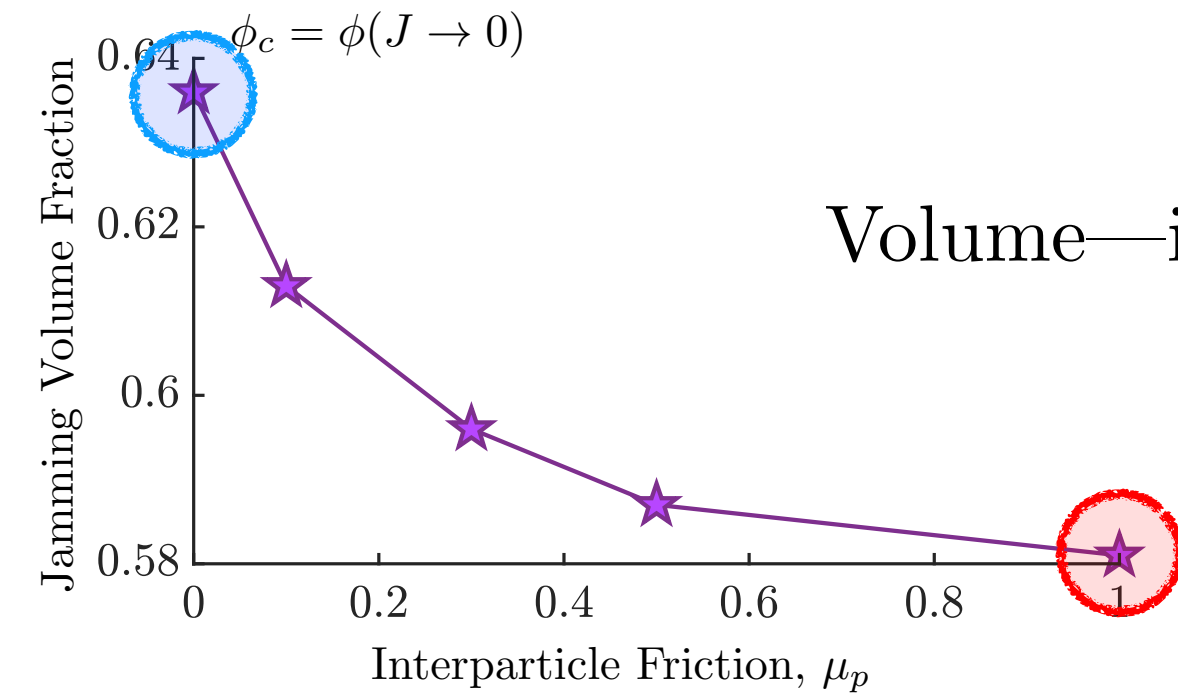
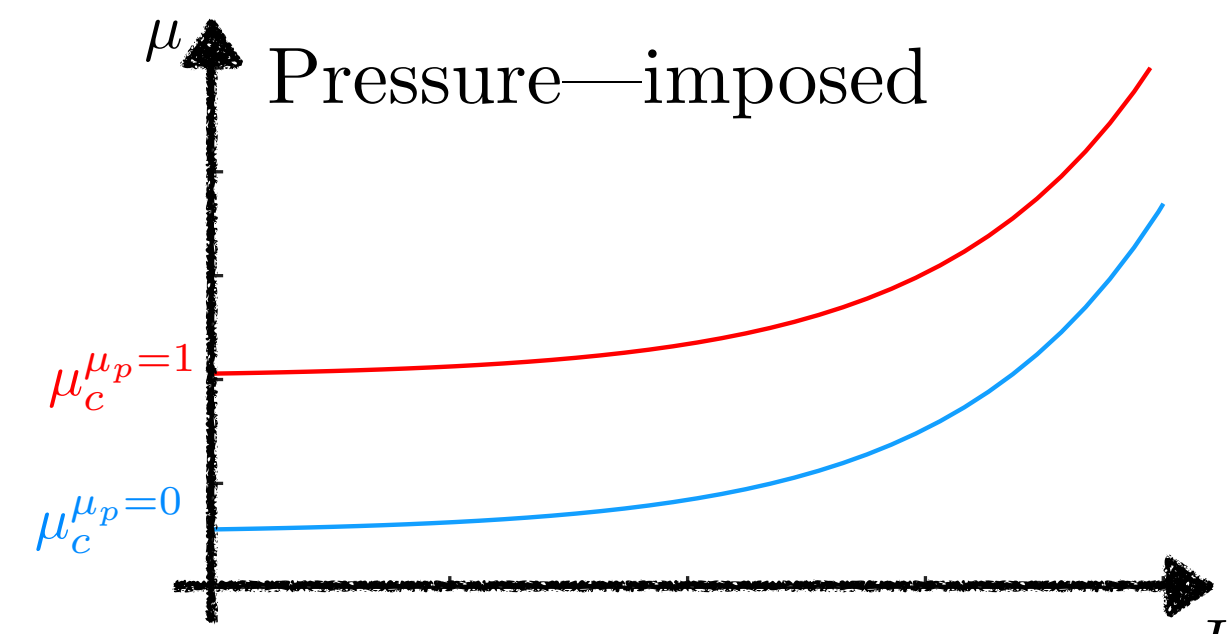
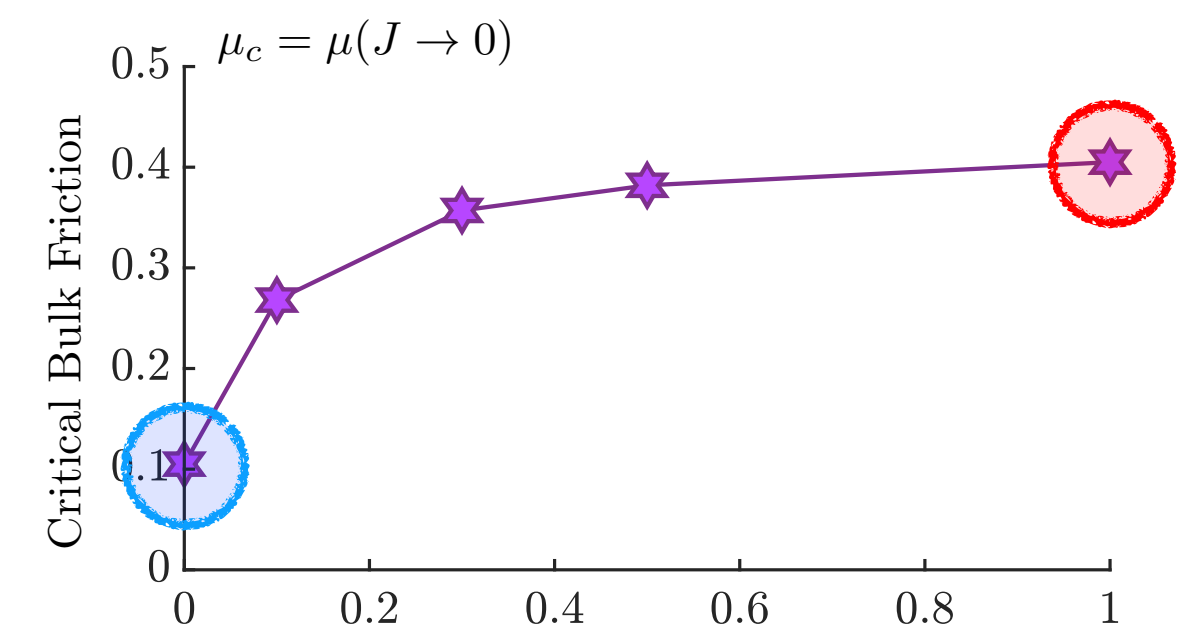
Low Stress  $P < P_{rep}$

Frictionless



High Stress  $P > P_{rep}$

Frictional



**\*\* A couple of Reviews, *Books* & *Nice Lectures* \*\***

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1. *E. Guazzelli & O. Pouliquen, JFM Perspectives (2018)*
2. *C. Ness, R. Seto & R. Mari, Annu. Rev. Condens. Matter Phys. (2022)*
3. *E. Guazzelli, Physical Review Fluids (2024)*
4. *J. Morris, Annu. Rev. Fluid Mech. (2020)*
5. *E. Guazzelli & J. Morris, Cambridge Press (2012)*
6. *B. Andreotti, Y. Forterre & O. Pouliquen, Cambridge Press (2004)*
7. *Elisabeth Lemaire — The Hitchhikers' of Rheology {Youtube}*
8. *Mike Cates — Trinity College Science Society {Youtube}*
9. *Wilson Poon — KITP Program: Physics of Dense Suspensions {KITP website}*
10. *Yoel Forterre — Département de Physique de l'ENS {Youtube}*
11. *Elisabeth Guazzelli — Australasian Fluid Mechanics Society {Youtube}*

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